Design of filter media via simulation

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Symposium >> Textile Filters <<

Chemnitz, March 7th, 2006.



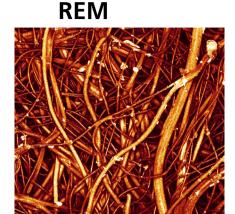
- I. Virtual Material Design Cycle
- II. Filter Media
- III. Fluid & Electric Field
- IV. Dirt model & dirt motion
- V. Deposition
- VI. Life time
- VII. Nano model
- **VIII. Summary**

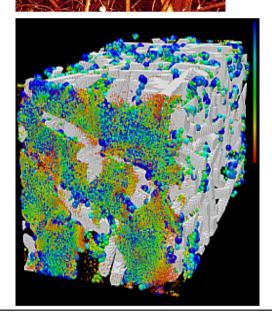




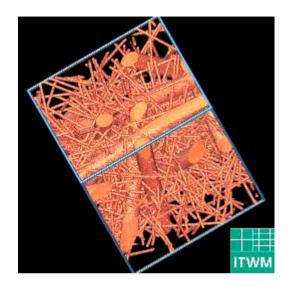
I. The Virtual Filter Material Design Cycle

- Identify parameters for real, existing material
- 2. Generate volume image for parameters
- 3. Solve Stokes(-Brinkmann)equations
- 4. Solve electric potential
- 5. Solve particle motion & deposition
- 6. Compute filter efficiency, pressure drop/ filter life time
- 7. Modify material parameters





Generated



Clogged nonwoven





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II. What constitutes ITWMs designable Virtual Materials?

The real media, porous or composite [e.g. nonwoven vs. carbon fiber-enforcement]

The mathematical model with (few) parameters [e.g. fiber diameter, etc.]

The Realizations in volume images, independent of the model

The Validation

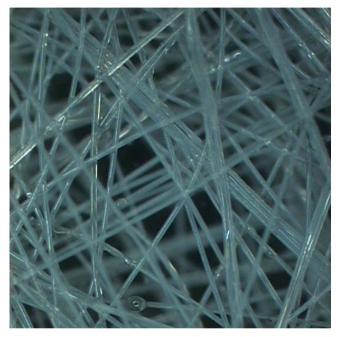
- inspection [2d & 3d visualization, comparison with microscopy & tomography]
- geometric analysis [e.g. porosity, pore size distribution, etc.]
- agreement of computed properties for existing media

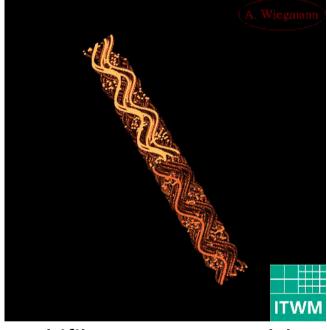
The **Design**; based on model parameters, not the volume images





II. Material Models for Nonwoven, Woven & Layers





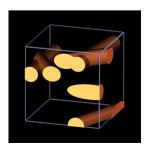
Microscopy

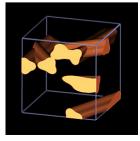
Nonwoven model

Multifilament woven model

Possible variations: for example

Cross sections





Layers





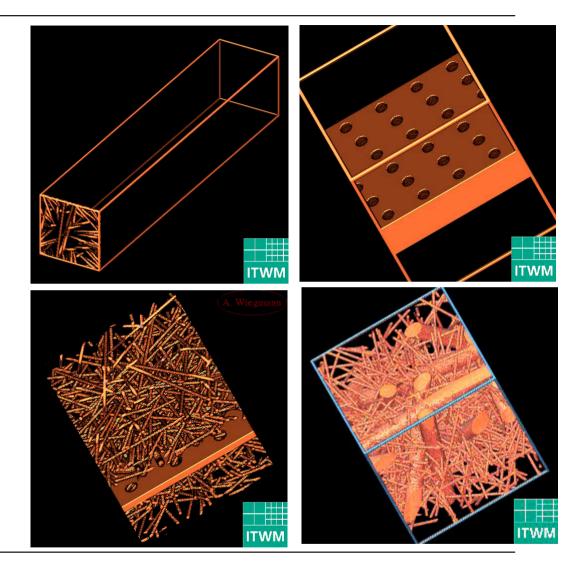
Anisotropy





II. Simulation and Design Parameters for Filter Media

- 1. Nonwoven model
- 2. Sinter model
- 3. Layers
- 4. Layer thicknesses
- 5. Porosity
- 6. Fiber diameters
- 7. Fiber anisotropy
- 8. Fiber shapes
- 9. Fiber overlap
- 10. Fiber crimp
- 11. Fiber length
- 12. ...







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III. Fluid & Electric Field:

For very sparse particles, the influence of the particles on the flow field and on the electrical field can be neglected.

The fluid enters the model through its viscosity μ . For example,

Oil at -25°C : $\mu = 1.50e + 0 \text{ kg/(m s)}$

Blood at 22°C : $\mu = 2.00e-2 \text{ kg/(m s)}$

Air at 20°C : $\mu = 1.84e-5 \text{ kg/(m s)}$

Mean flow velocity is an output of the model. It is controlled by the pressure drop, which enters the model as a volume force, e.g. for 200 Pa, sample thickness L:

$$f = \frac{200Pa}{L}$$

Electric field enters the model as charges on fiber surfaces





III. Flow: Navier-Stokes-Brinkmann equations

$$-\mu\Delta\vec{u}+\nabla\vec{u}\cdot\vec{u}+\kappa^{-1}\vec{u}+\nabla p=\vec{\mathbf{f}}$$
 (momentum balance)
$$\nabla\cdot\vec{u}=0 \text{ (mass conservation)}$$
 $\vec{u}=0 \text{ on } \Gamma \text{ (no-slip on fiber surfaces)}$

 $\vec{\mathbf{f}} = (0, 0, f)$: force in flow(z)-direction,

 κ : porous voxel permeability,

 $ec{u}$: velocity,

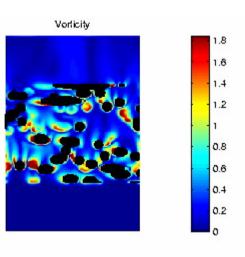
 μ : fluid viscosity,

p: pressure and

 Γ : fiber or deposited particle surfaces.

The flow can be solved with periodic boundary conditions if the cutout is large enough and empty space is added in front.





Cross section views of vorticity





III. Electric field: Poisson equation for the potential

 $\Delta u = \rho \chi (\delta \Omega)$: Poisson equation

 $\vec{\mathbf{E}} = \nabla u$: Field equation

 $\delta\Omega$: boundary of domain occupied by fibers (surface),

 ρ : source strength,

 χ : surface Dirac delta function,

u: the electric potential,

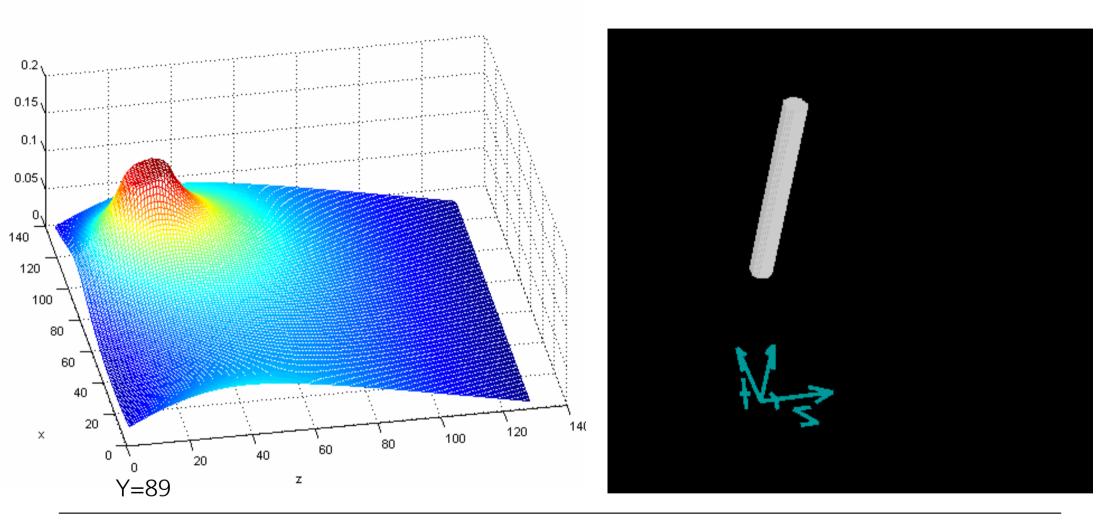
 $ec{\mathbf{E}}$: the electric field (the gradient of the potential).

The field can be solved with periodic boundary conditions in the lateral direction and zero potential at appropriately chosen distances outside the media.





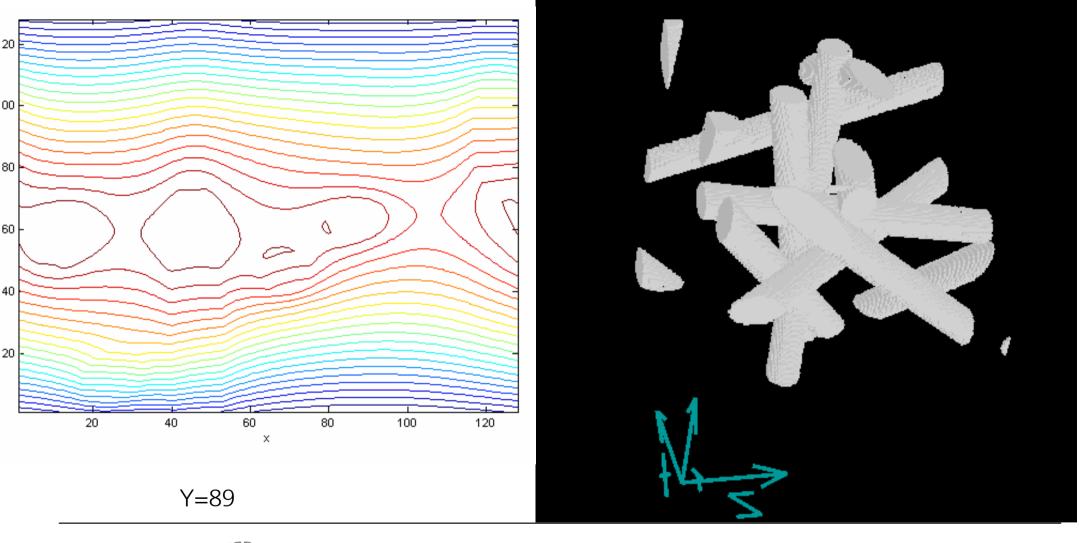
III. Electric potential (cross section Y=89) for a single fiber







III. Electric potential (contour Y=89) for random fibers







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IV. Dirt Model

- probability distribution of diameters of spherical particles of given material
- Size and material determine the particle mass
- Particles move with fluid via friction
- Particles move diffusively in fluid dependent on size and temperature
- Particles move electrostatically based on their own charge and the electric field





IV. Lagrangian description of particle motion





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V. Mechanisms of filtration

Particle impact by:

A: direct interception

B: inertial impaction

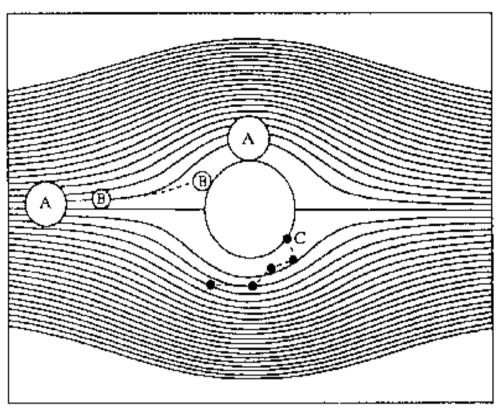
C: diffusional deposition

D: electrostatic attraction

E: sieving

F: clogging

G: other effects (gravity,...)



Detect collisions of particles with fibers and previously deposited particles!





V. Filter Efficiency Model

B) Fluid: A) Testdust: C) Nonwoven geometry:

Electrostatic charges Sphere radii Viscosity Specific weight

No-slip boundary conditions Density

Electrostatic charges Temperature

Mean flow velocity

D) Efficiency:

Flow & pressure drop: B & C

Electrostatic field:

Friction: A & B

Diffusion: A & B

Collision: A & C

Adhesion: A & C

Electrostatic attraction: A & C

Particle Paths: A, B & C E) Deposition due to:

Adhesion

- Inertial impact
- Diffusion
- **Electrostatic attraction**

Sieving

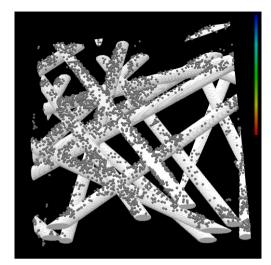




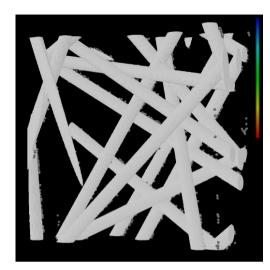
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V. Simulation results with(out) electric surface charge

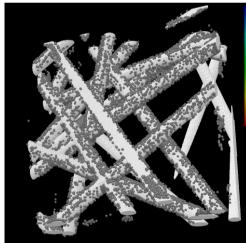


Simulation result without the influence of electric surface charges on the fibers.



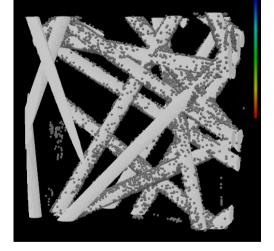
Front view

back view



Simulation result under the influence of electric surface charges on the fibers.

Retention rate increased by about 50%!



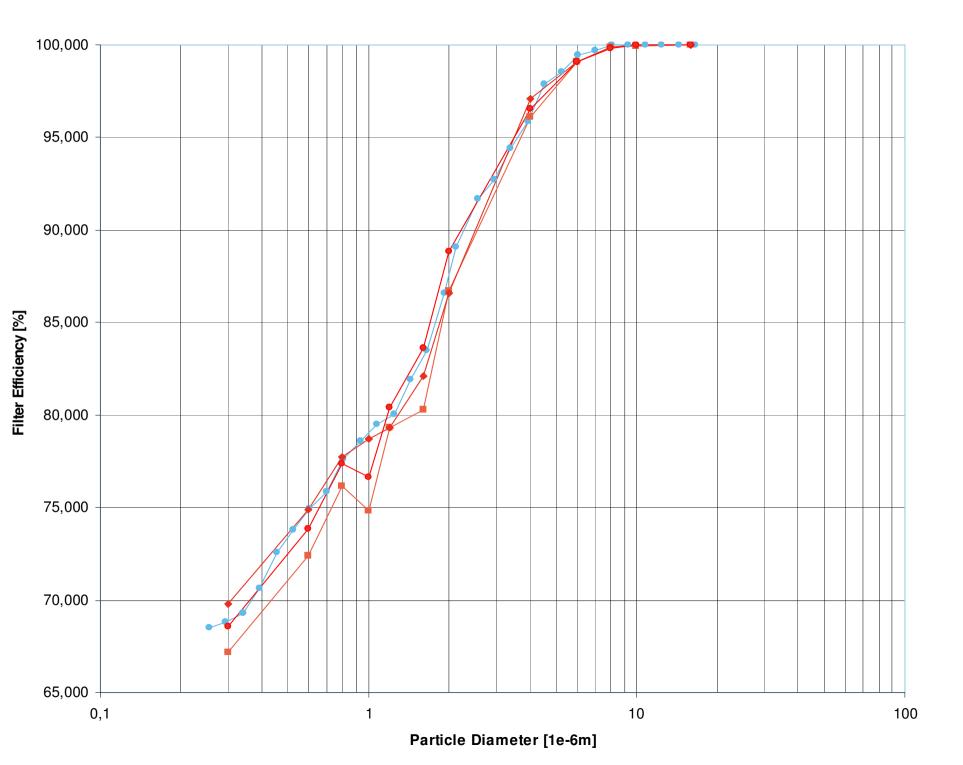
Front view

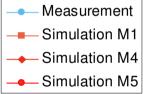
back view





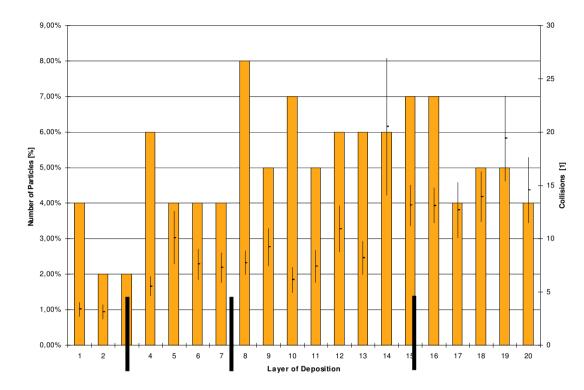
Filter Efficiency





V. Deposition Diagram

- Deposition locations are 20 64µm layers.
- Orange: particle numbers
- Lines: mean value and standard deviation of number of collisions
- Example: Layer 15 contains 7% of the filtered particles. Those had on average 13.15 collisions with standard deviation 1.9
- 4 layers of gradient material indicated by thick black lines:







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VI. Decoupling of fluid flow and particle motion simulations

Assume particle density is very low, then:

- Particles move and deposit independently, they do not collide in the air.
- When many particles have deposited, the fluid flow is significantly altered.
- So, for clogging, the volume image is periodically updated by deposited particles and the flow field in this volume image is recomputed.
- Subsequent particle motion is computed based on the updated flow field, particle deposition is based on the updated volume image.





VI. Filter Life Time Model

G) Multipass:

Unfiltered particles change particle size distribution



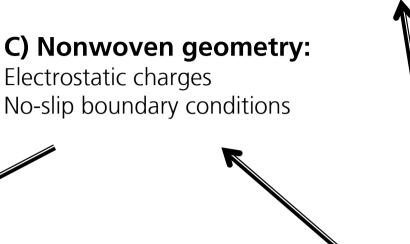
Sphere radii Specific weight Electrostatic charges

B) Fluid:

Viscosity Density

Temperature

Mean flow velocity



D) Efficiency:

Flow & pressure drop: B & C

Electrostatic field: (

Friction: A & B

Diffusion: A & B

Collision: A & C

Adhesion: A & C

Electrostatic attraction: A & C

Particle Paths: A, B & C

E) Deposition due to: Adhesion

- Inertial impact
- Diffusion
- Electrostatic attraction

Sieving

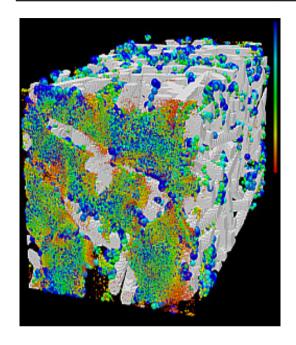
F) Clogging:

Deposited particles determine new geometry model, including **permeable** voxels

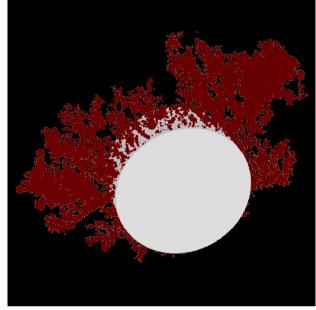




VI. Clogging of nonwoven & ceramic; dendrites on single fiber



Clogged nonwoven

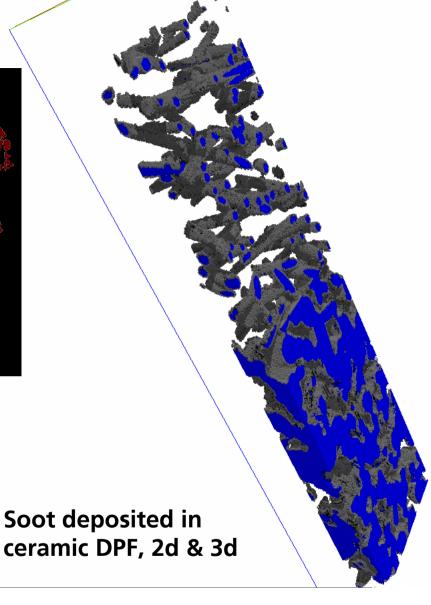


Soot deposition on a single fiber

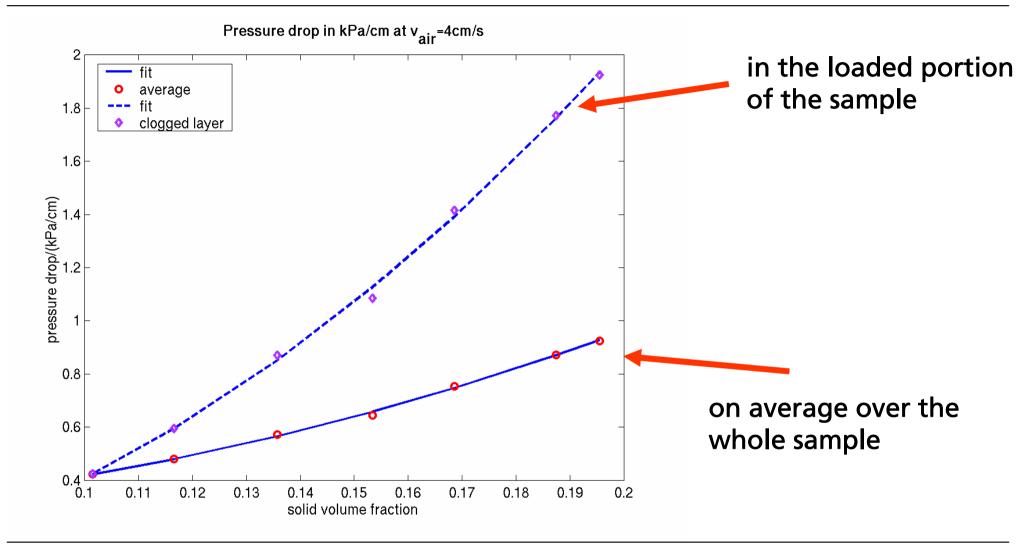
Deposition occurs on fibers and on previously deposited particles







VI. Time Dependent Pressure Drop







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VIII. Summary

Complex geometry of real textiles _______ high resolution volume image

"Slow" flow Stokes equations

Highly diluted Particles do not modify fields

Material & Dirt models

Fluid & electric models

Deposition & Clogging models

Output are models, predicted filter properties, and optimized material geometries

Models & equations are fairly standard. Completeness of approach is new.

Difficulties: knowledge of parameter settings, high resolution for large cutouts.

Goals: "generic agreement with reality", little need for recalibration for new application areas. New material must be manufactured and predictions must be verified.





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