
Modelling of Microporous Layers

ModVal 6, Bad Herrenalb, 25.03.2009

Jürgen Becker

Fraunhofer ITWM, Fraunhofer-Platz 1, 67663 Kaiserslautern

Christian Wieser

Adam Opel GmbH, IPC MK-01, 65423 Rüsselsheim

Retrospection: Modelling of Gas Diffusion Layers without MPL

First step: Structure Model

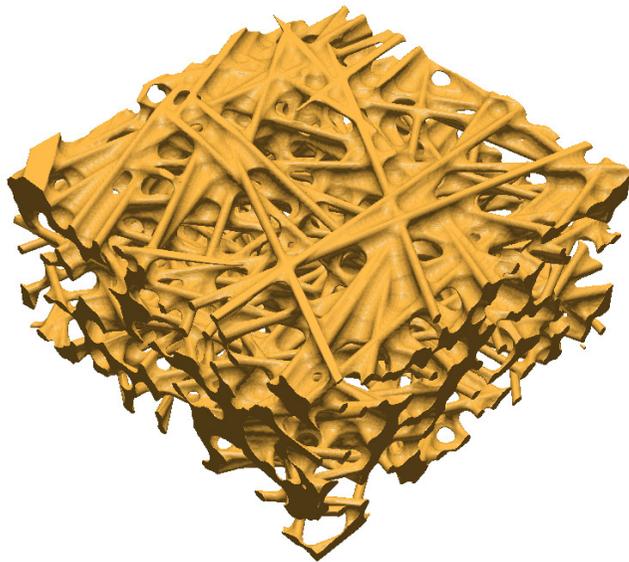
- virtually created
- tomography image

Second step: Solve PDE

- Flow (Stokes Equation)
- Diffusion (Laplace Eq.)
- Conduction (Poisson Eq.)

Third step: Upscaling

- Permeability
- Diffusivity
- Conductivity



MPL Modelling - What is the Problem?

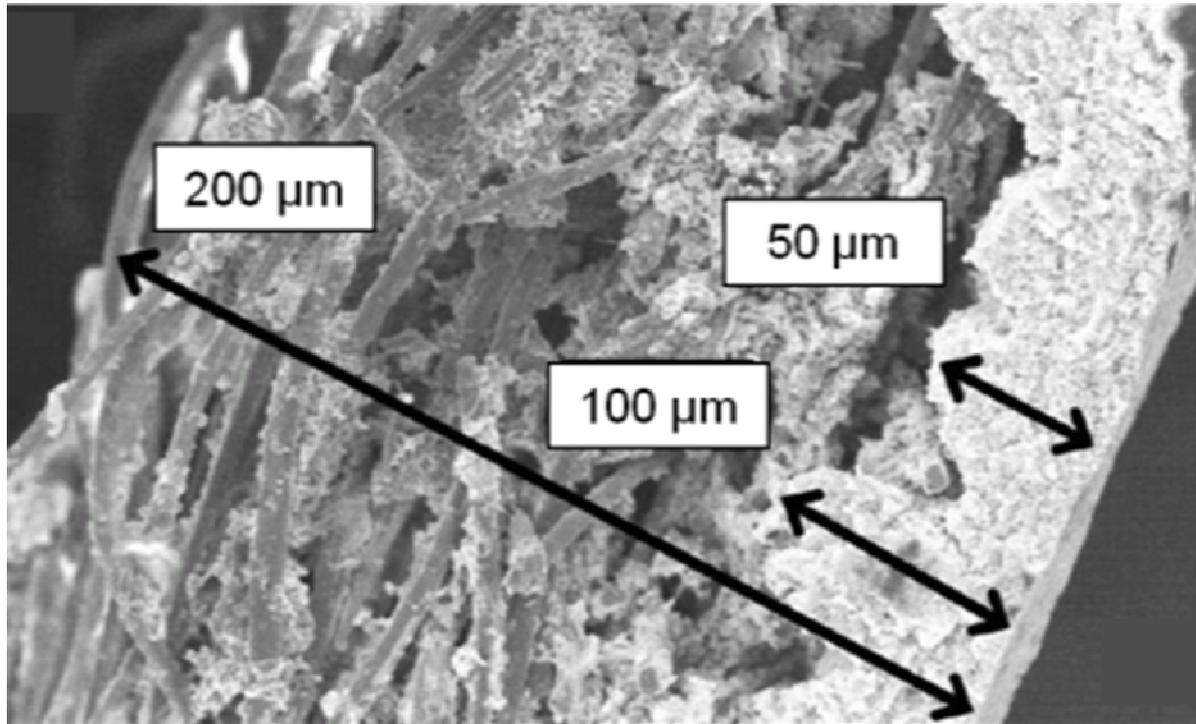
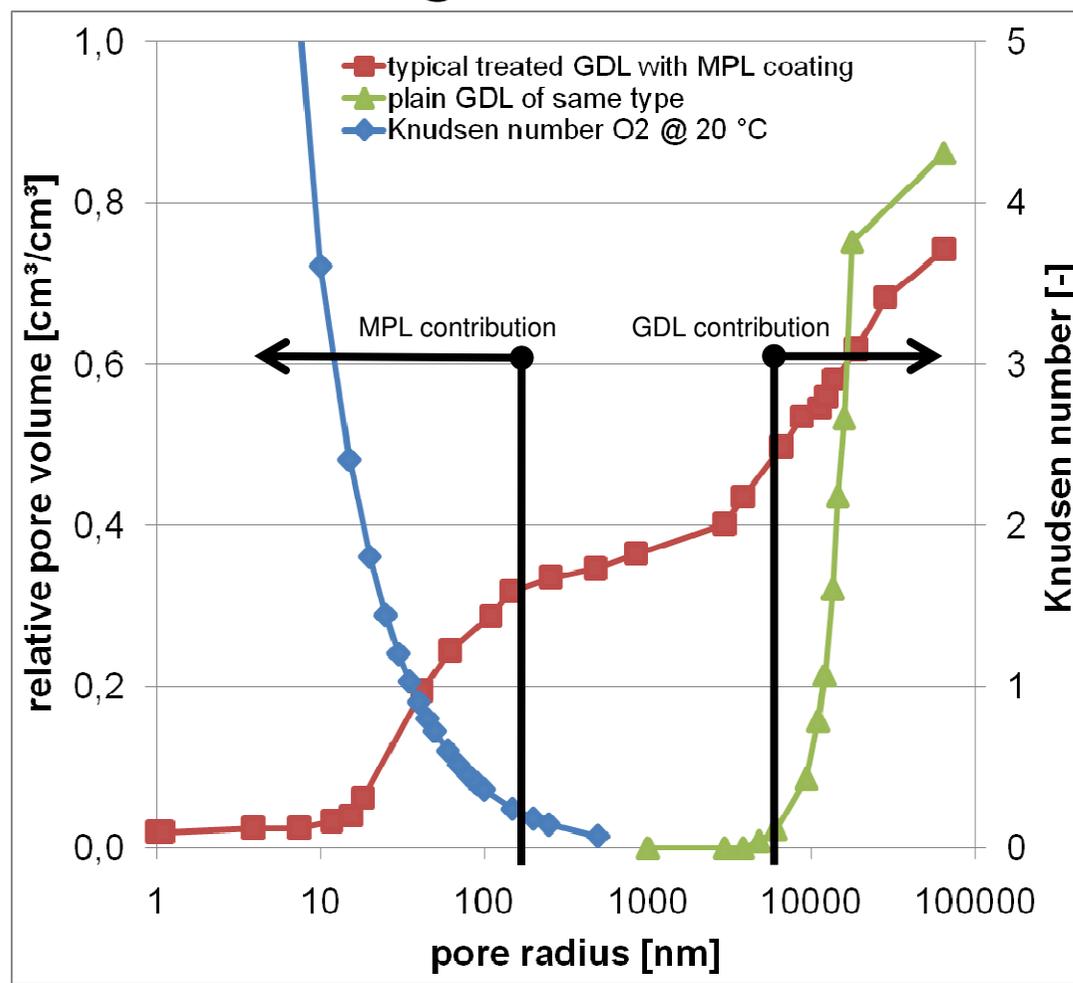


image source: Gostick et al., Journal of Power Sources 156 (2006), p. 375-387

Gas diffusion layers (GDL) in technical applications (e.g. automotive) are typically coated with a microporous layer (MPL) to

- improve electrical and thermal contact to catalyst layer.
- protect membrane electrode assembly (MEA) from mechanical stress.
- enhance fuel cell performance and robustness under humid and wet operating conditions by improving water management.

MPL Modelling - What is the Problem?



Pore size distribution of GDL w/ MPL and GDL

Mean pore radii:

- MPL 10..100 nm
- GDL 10..100 μm

→ three orders of magnitude difference

Implications:

- GDL and MPL pores cannot be resolved in the same computational grid to numerically determine effective properties of assembly
- There are different transport mechanisms in GDL and MPL
 - GDL: bulk diffusion (particle-particle collisions dominate)
 - MPL: contribution of Knudsen diffusion (significant particle-wall collisions)



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Outline / Approach

A) Modelling of the MPL (stand-alone)

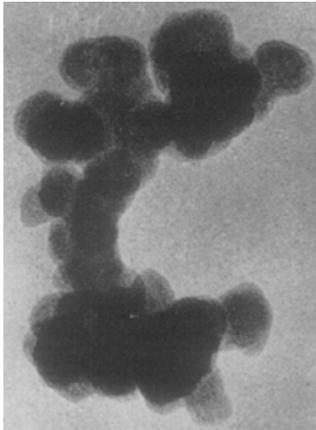
1. Structure model (resolution ~ 5 nm)
2. Determination of MPL diffusivity

B) Modelling of GDL plus MPL

1. Structure model (resolution $\sim 1\mu\text{m}$) with homogenised MPL
2. Determination of diffusivity of GDL plus MPL

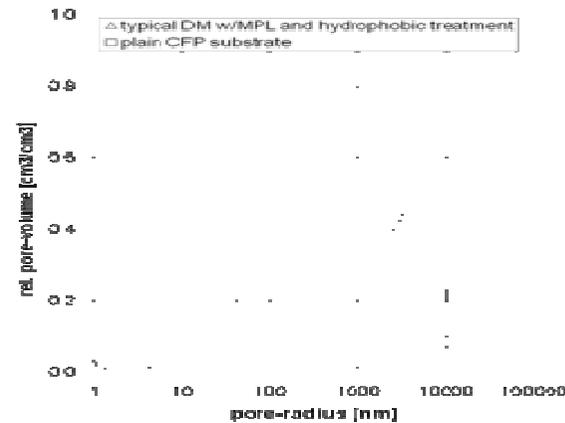
A) Modelling of the MPL

MPL Structure Model: Material Parameters



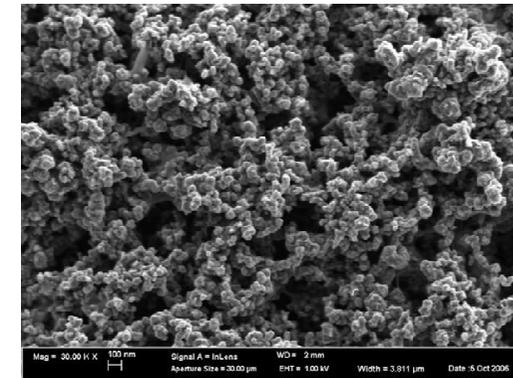
Primary particle and particle aggregate data, e.g. acetylene black:

- Particle size 42 nm
- Aggregate size 200 particles
- Surface area 51 m²/g
- Shape parameters



Pore size distribution:

- Shape of pore size distribution
- MPL porosity 55%



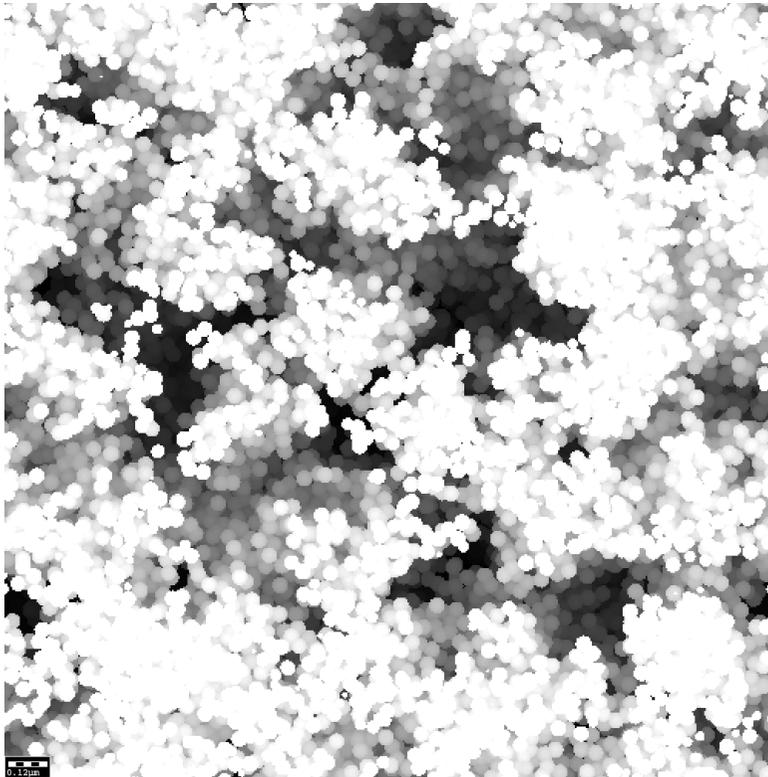
SEM images of MPL surface and cross-section
→ visual plausibility check



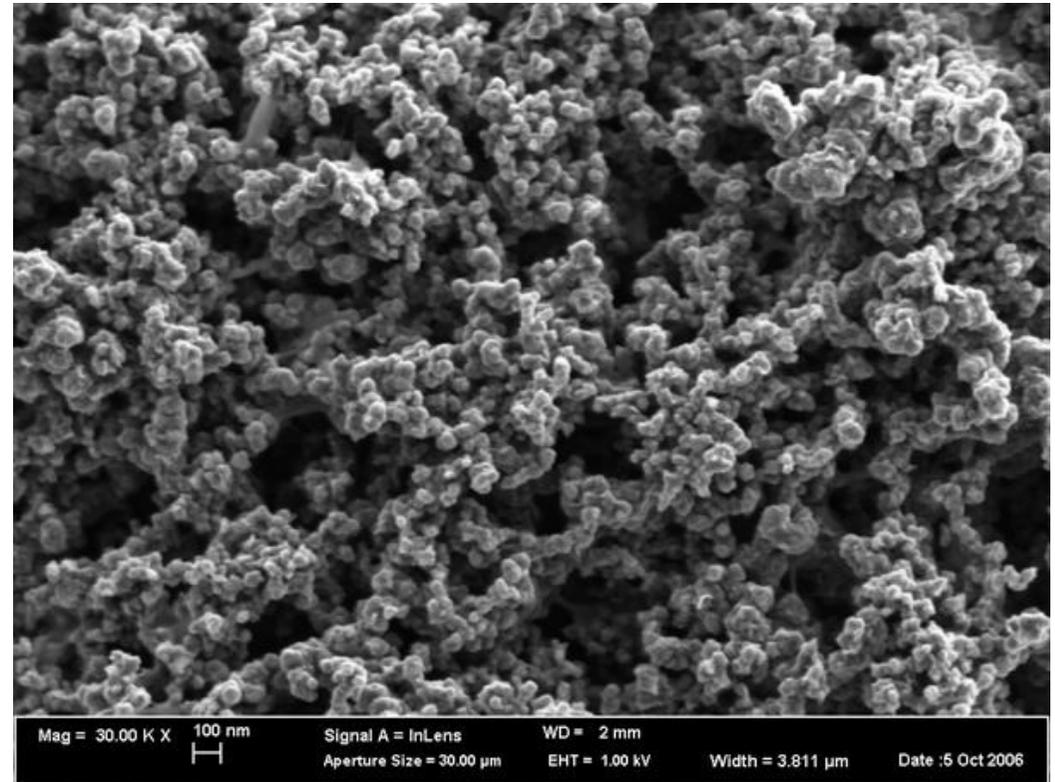
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MPL Model and SEM Picture



Virtually created model



SEM picture

Diffusion

Macroscopic description (homogenized porous media model)

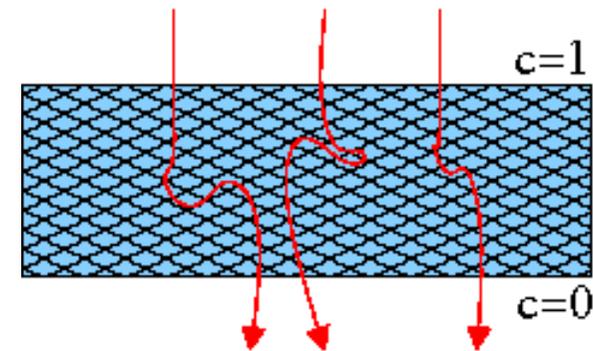
Fick's first law:

$$j = -D^* \nabla c$$

D^* : anisotropic effective diffusivity [m^2/s]

j : diffusion flux [$\text{mol}/\text{m}^2/\text{s}$]

∇c : concentration gradient [$\text{mol}/\text{m}^3/\text{m}$]



Microscopic description (pore structure model)

- j and D^* can be calculated

- Depending on the Knudsen number $Kn = \frac{\text{mean free path}}{\text{characteristic length}}$ the diffusion mechanisms in the pores change.



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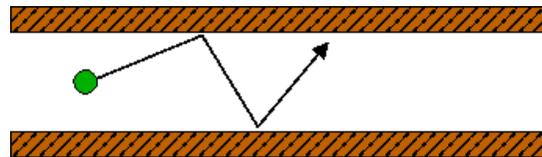


Diffusion Mechanisms

1) $Kn \gg 1$ (Knudsen diffusion)

Diffusion by particle-wall collisions

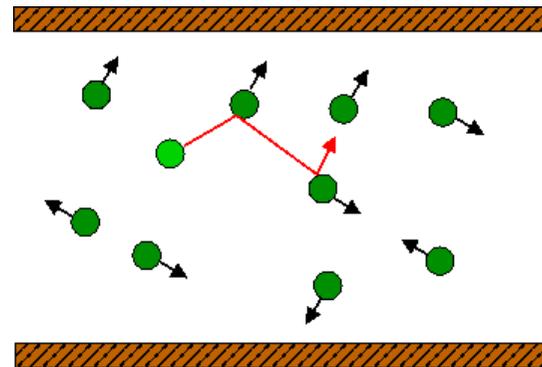
Mathematical model: random walk methods



2) $Kn \ll 1$ (bulk diffusion)

Diffusion by particle-particle collisions

Mathematical model: Laplace equation



3) $Kn \sim 1$ (transition regime diffusion)

Both mechanisms are present

Diffusion at $Kn \sim 1$: Bosanquet's Formula

Bosanquet's formula: $D = \left(D_{bulk}^{-1} + D_{Kn}^{-1} \right)^{-1}$

Coefficient D_{bulk}

- describes diffusion by particle - particle collisions
- scales with $D_{bulk} = \frac{1}{3} \lambda \bar{v} D_1$
- determined by solving Laplace equation

Coefficient D_{Kn}

- describes diffusion by particle - wall collisions
- scales with $D_{Kn} = \frac{1}{3} l \bar{v} D_2$
- determined by random walk methods

Definitions:

- ε porosity
- v mean thermal velocity
- λ mean free path
- l char length

Remarks:

- D_1 and D_2 are dimensionless and independent from λ, l, v
- Tortuosity $\eta_1 = \varepsilon / D_1$
- Knudsen tortuosity: $\eta_2 = \varepsilon / D_2$



Determination of D_{Kn}

The diffusivity matrix can be calculated from the displacement of a set of gas molecules, where for each molecule we

- start at a random position x^0
- find the end position at time t by a random walk: x^t
- calculate the displacement vector: $\xi = x^t - x^0$

Diffusivity matrix: $D_{Kn} = \frac{\epsilon}{2t} E [\xi \xi^T]$

($E[\dots]$ expectation value, ϵ porosity)

Random walk (for a single molecule):

- if molecule hits a wall, choose new velocities (v, w_1, w_2) , v orthogonal to wall, w_1, w_2 parallel to wall with probability density (Maxwell):

$$p(v, w_1, w_2) = 2\alpha v e^{-\alpha v^2} \sqrt{\frac{\alpha}{\pi}} e^{-\alpha w_1^2} \sqrt{\frac{\alpha}{\pi}} e^{-\alpha w_2^2}$$

- molecule moves with this velocity until it hits a wall.

- speed determined by $\alpha = \frac{4}{\pi \bar{v}^2}$

H. Babovsky, On Knudsen Flows within Thin Tubes, J. Stat. Physics 44, pp 865--878, 1986.



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Results: Diffusivity of O₂ in N₂ in the MPL

Gas species parameters for diffusion of O₂ in N₂ (Input):

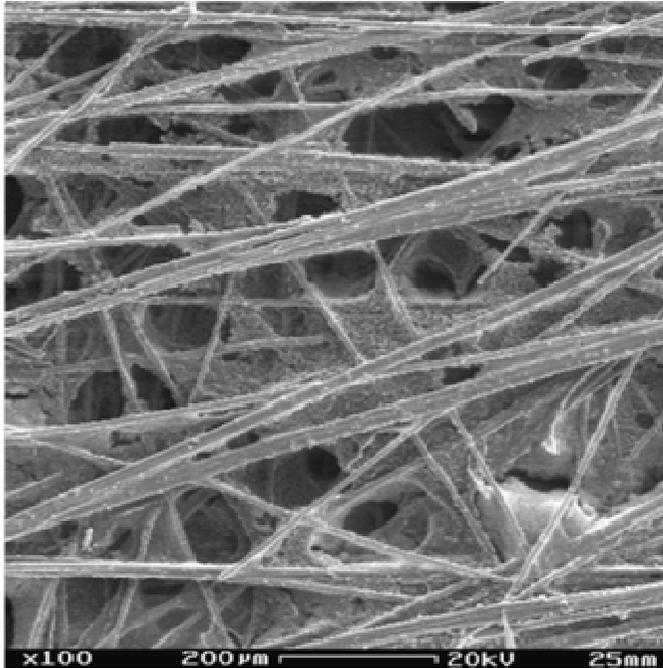
- mean thermal velocity: 444.1 m/s
- absolute diffusivity (no obstacles): 20.86 mm²/s
- mean free path: $\lambda = 140.9$ nm

These parameters lead to the following diffusivity values (isotropic) for the MPL:

- Knudsen diffusion: $D_{Kn} 3.12$ mm²/s
- Bulk diffusion: $D_{bulk} 6.40$ mm²/s
- Bosanquet formula gives: $D = 2.10$ mm²/s

B) Modelling of GDL plus MPL

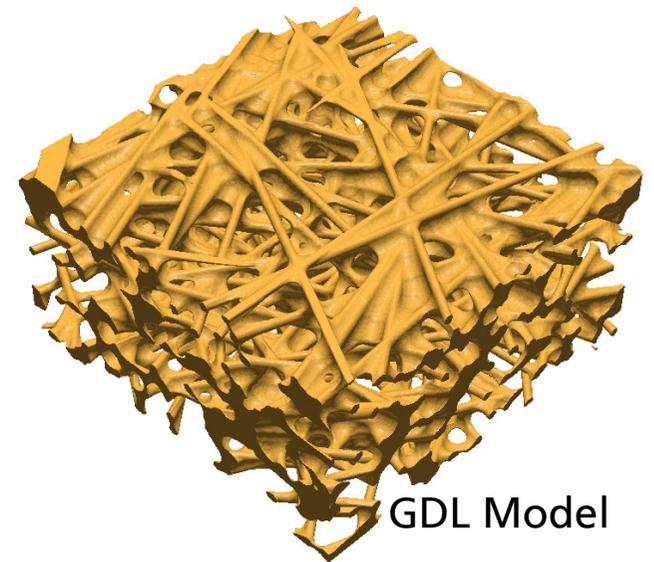
GDL Model: Material Parameters



SEM Picture

GDL:

- Fibre diameter $7 \mu\text{m}$
- Fibre density 1.9 g/cm^3
- Binder density 1.7 g/cm^3
- GDL thickness $180 \mu\text{m}$
- Assumptions:
 - Fibre content 11 vol%
 - Binder content 50 wt%

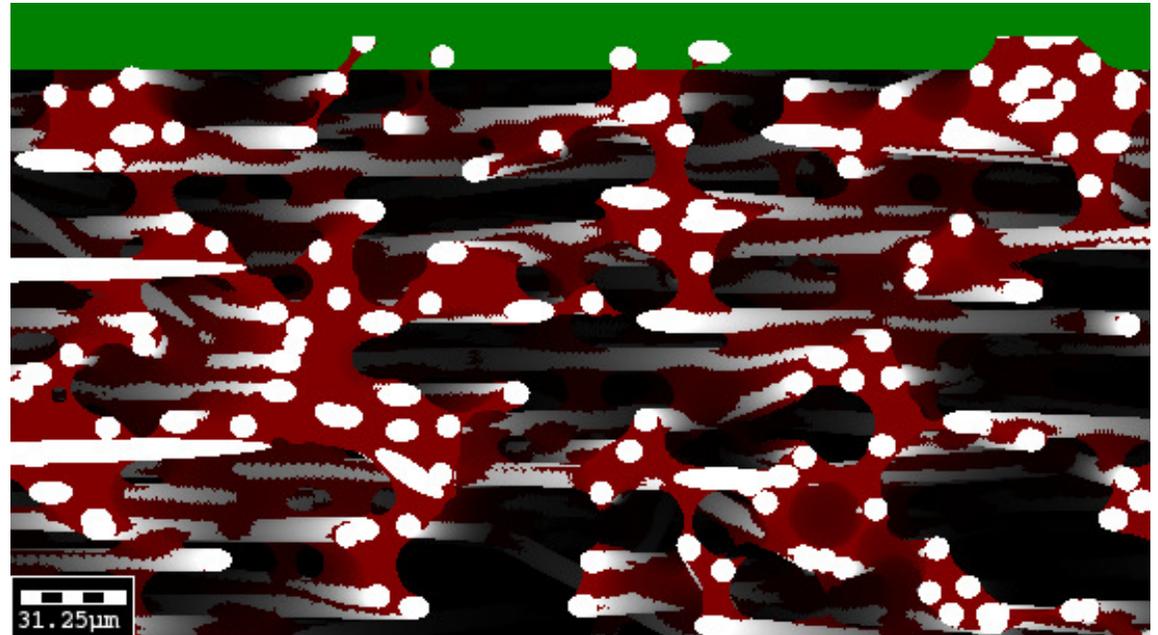


GDL Model

GDL Model with Homogenised MPL

GDL+MPL model parameters:

- Voxel length $0.625 \mu\text{m}$
- Geometry size: $550 \times 550 \times 304$ voxels
- GDL thickness: $180 \mu\text{m}$
- MPL thickness: $10 \mu\text{m} + 10 \mu\text{m}$
- Overall thickness: $190 \mu\text{m}$



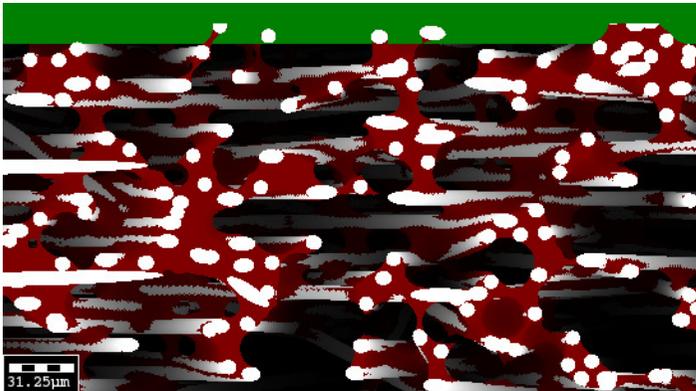
Substrate with MPL layer

Results: Diffusivity of GDL/MPL Assembly

Input: (Diffusivities of O₂ in N₂) :

- Pore space (black): 20.86 mm²/s
- MPL (green): 2.10 mm²/s
- Fibres (white): 0
- Binder (red): 0

Solve equation: $\text{div}(d(x)\nabla u) = 0$



	D _x [mm ² /s]	D _y [mm ² /s]	D _z [mm ² /s]
without MPL	11.54	11.73	9.71
MPL	10.30	10.36	5.98

Conclusions

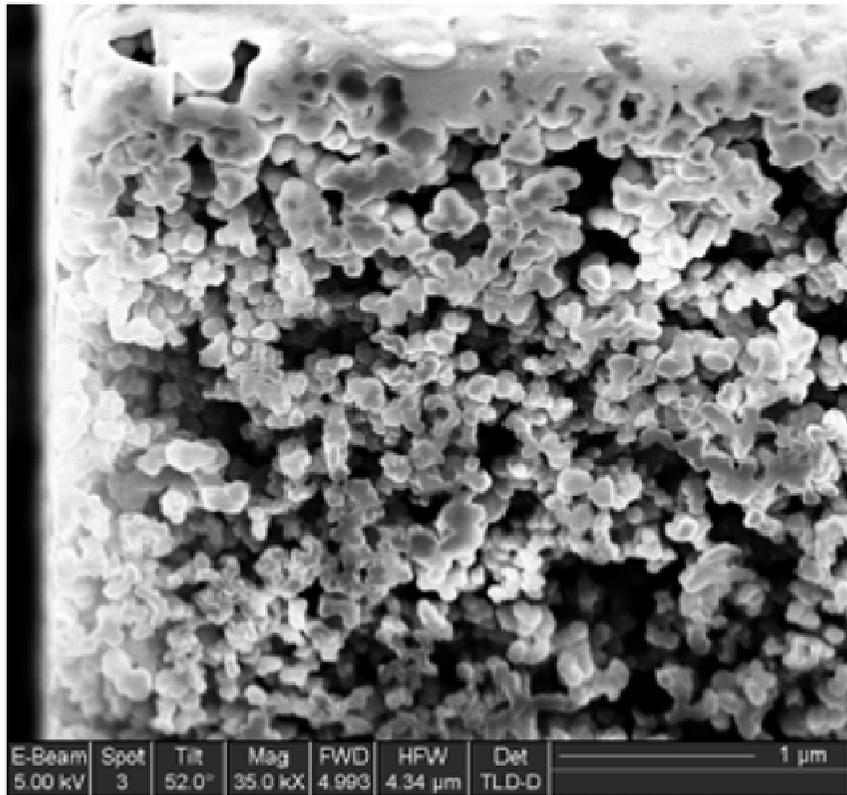
Summary

- Method to determine diffusivity of MPL and MPL+GDL developed
- Approach can now be used to study different geometrical setups

Challenges / Open Problems

- No tomographical 3D images available for MPL
- Generating realistic MPL models requires MPL-only material data:
 - porosity, pore size distribution...
- Generating realistic MPL+GDL models requires
 - penetration depth, cracks etc.
- Experimental validation of simulated MPL+GDL diffusivities
 - MPL-only, MPL+GDL

Outlook: Pore Scale Material Visualization



Exemplary method:
Dual-beam focused ion beam/scanning electron microscopy nanotomography (FIB/SEM) w/ serial slicing

Major challenges:

- Resolution in slicing direction
- Image processing/segmentation (visibility of pore background)

single FIB/SEM image of typical MPL from image stack obtained by serial slicing



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