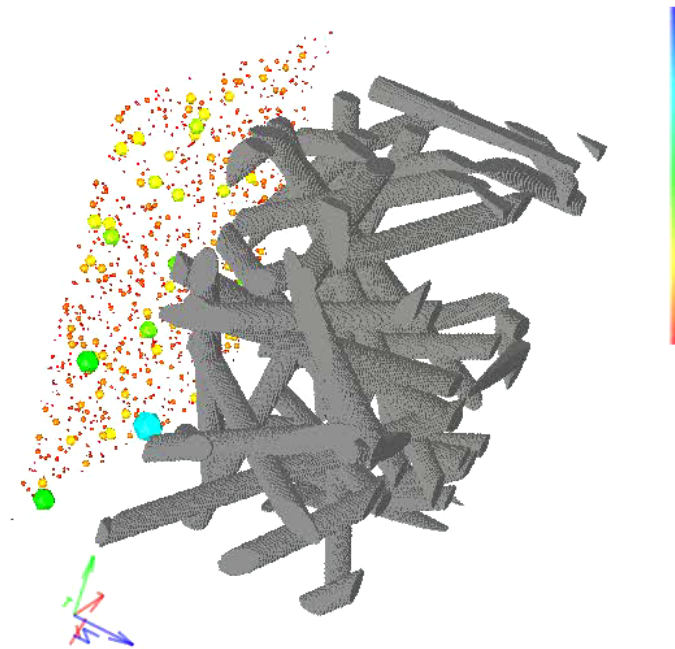

Toward predicting Filtration and Separation: Challenges & Progress

Andreas Wiegmann

Filtech 2009

13th October, 2009



Thanks to collaborators at Fraunhofer ITWM

Currently at ITWM:

- Heiko Andrä, Jürgen Becker, Peter Klein, Arnulf Latz, Sven Linden, Barbara Planas, Stefan Rief, Katja Schladitz, Konrad Steiner, Aivars Zemitis.
- Presenters at Filtech 2009:
 - Liping Cheng, Erik Glatt, Oleg Iliev, Mathias Kabel, Zarah Lakdawala, Kilian Schmidt.

Formerly at ITWM:

- *Donatas Elvikis, Irina Ginzburg, Dirk Kehrwald, Joachim Ohser, Doris Reinel-Bitzer, Vita Rutka, Christian Wagner, Ashok Kumar Vaikuntam, Rolf Westerteiger, Qing Zhang.*

Filtration and simulation occur on multiple scales

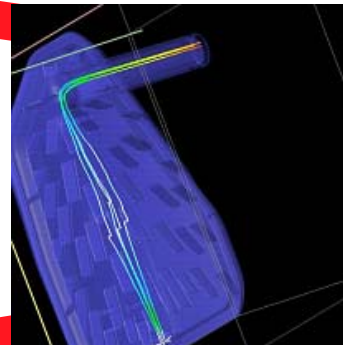
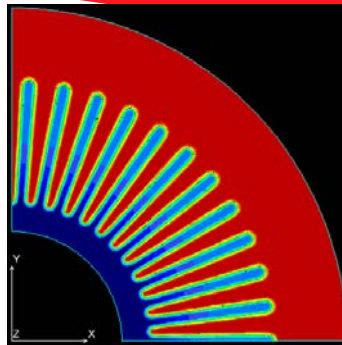
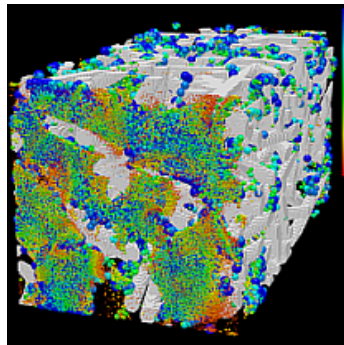
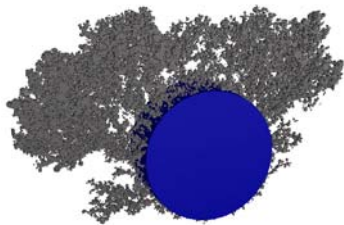
Single Fiber
Nanometer

Media
Micrometer

Cartridge
Millimeter

Element
Centimeter

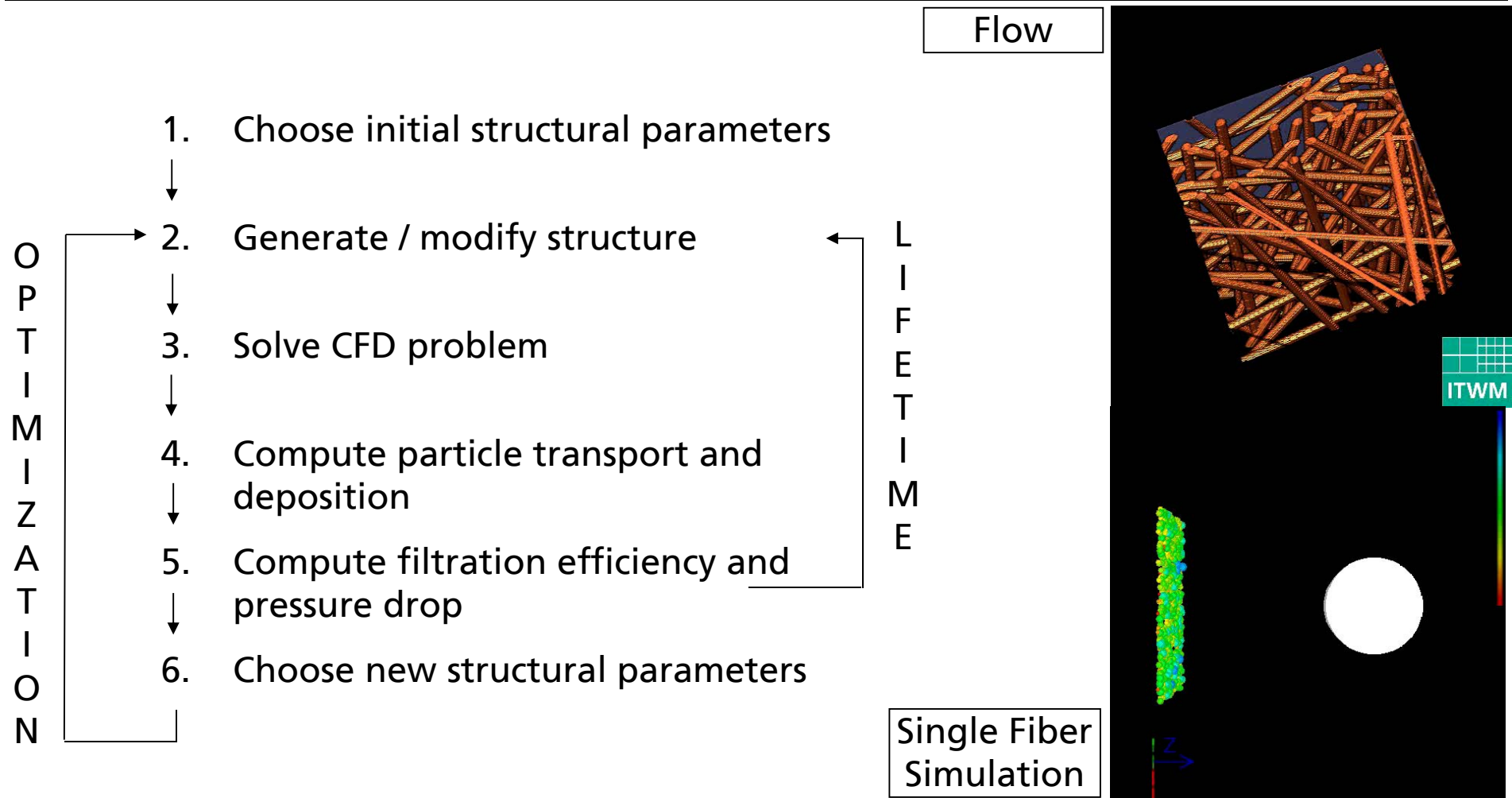
Exhaust system
Meter



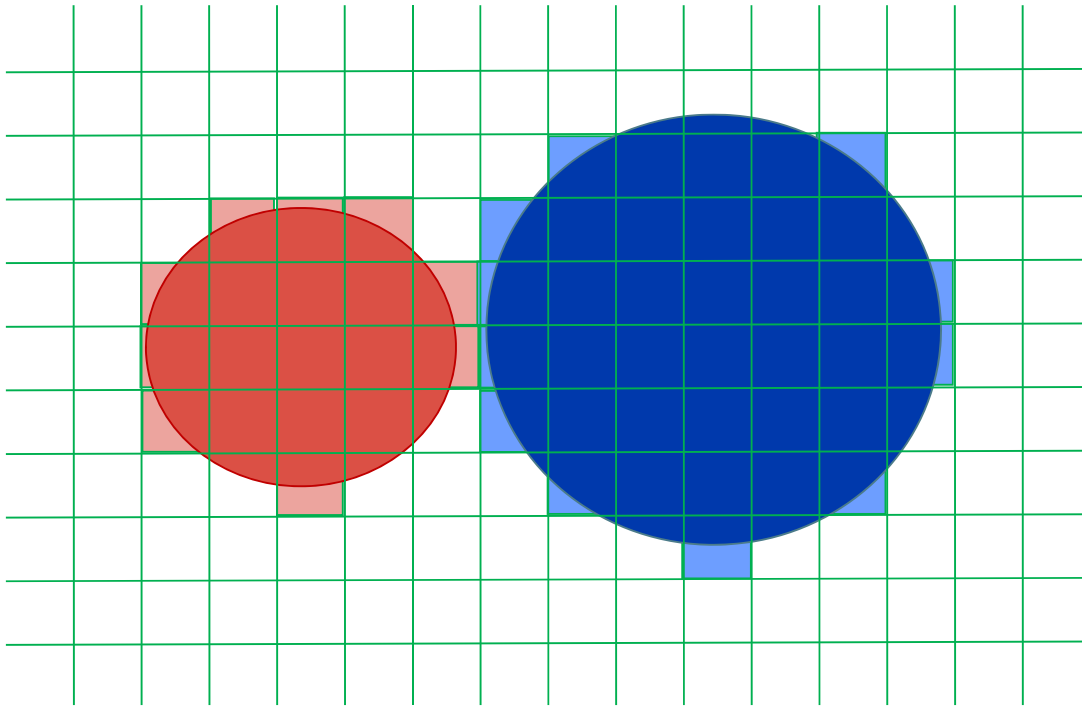
How does (direct numerical) filtration simulation work, anyway?

- 1. Have a geometric model of the filter media or filter element*
- 2. Have process conditions such as flow velocity, particle size and mass distributions, etc.*
- 3. Know chemistry such as adhesion between particles and obstacles*
4. Compute liquid or gas flow: **get initial pressure drop**
5. Compute motion and deposition of (first batch of) particles: **get initial filter efficiency**
6. Update geometric model by deposited particles
7. Update liquid or gas flow: **get pressure drop over deposited mass**
8. Compute motion and deposition of (next batch of) particles: **get clogging and life time**
9. Go back to 6

Virtual design cycle of filter media



All simulations done are based on structures of little cubes



Advantages

- Saves grid generation times
- Compatible with computer tomography
- Straight forward structure generation
- Straight forward solver implementation
- Straight forward parallel computations

Disadvantages

- Resolved features require many grid cells
- Leads to very large scale computations

Stationary Stokes flow with no slip vs fractional slip

$$-\mu\Delta\vec{u} + \nabla\vec{u} \cdot \vec{u} + \nabla p = 0 \text{ (momentum balance)}$$

$$\nabla \cdot \vec{u} = 0 \text{ (mass conservation)}$$

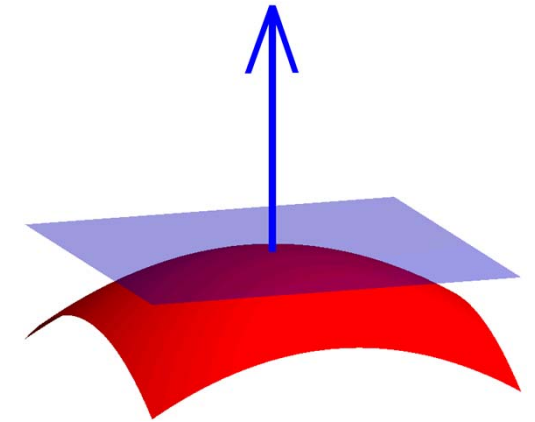
$$\vec{u} = 0 \text{ on } \Gamma \text{ (no-slip on fiber surfaces)}$$

$$P_{in} = P_{out} + c \text{ (pressure drop is given)}$$

μ : fluid viscosity,

\vec{u} : velocity, periodic,

p : pressure, periodic up to pressure drop in flow direction.



$$-\mu\Delta\vec{u} + \nabla p = 0 \text{ (momentum balance)}$$

$$\nabla \cdot \vec{u} = 0 \text{ (mass conservation)}$$

$$\vec{n} \cdot \vec{u} = 0 \text{ on } \Gamma \text{ (no flow into fibers)}$$

$$\vec{t} \cdot \vec{u} = -\lambda \vec{n} \cdot \nabla (\vec{u} \cdot \vec{t}) \text{ on } \Gamma \text{ (slip flow along fibers)}$$

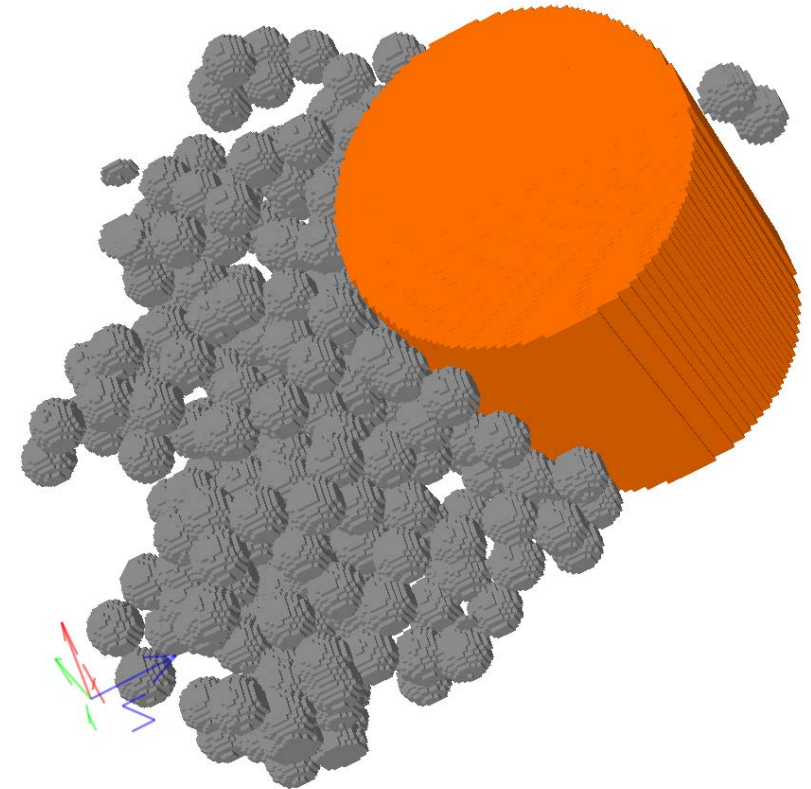
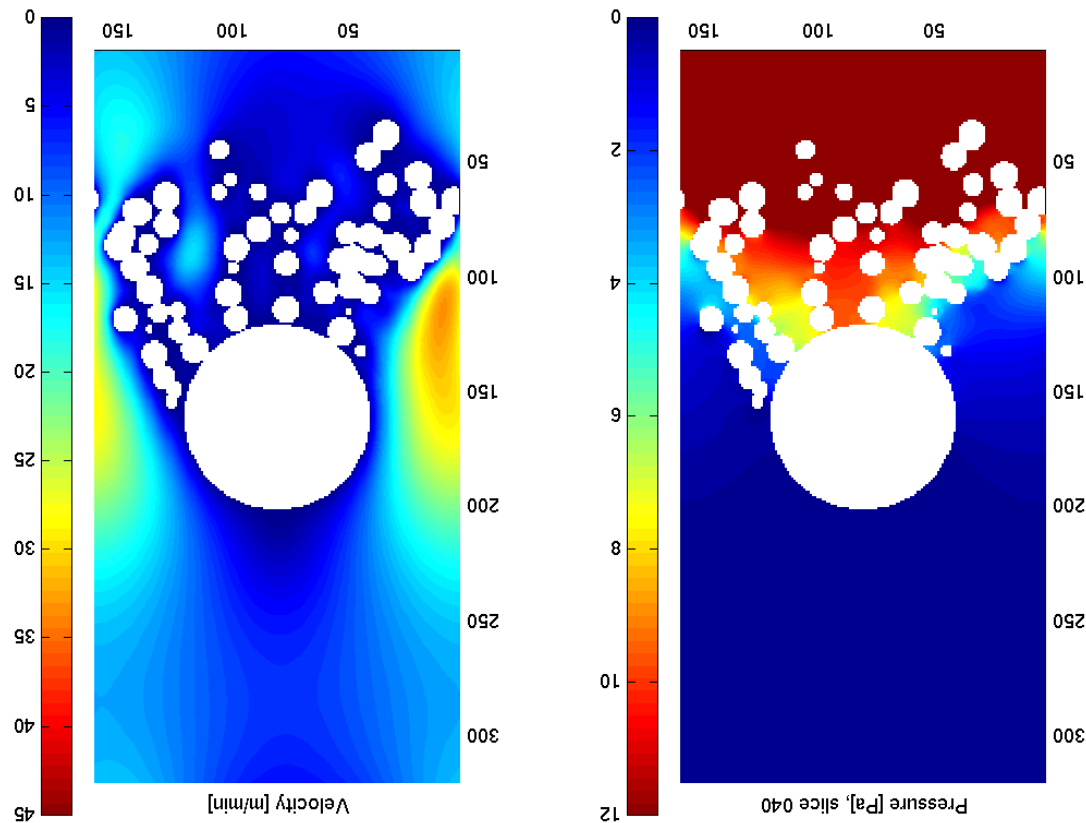
$$P_{in} = P_{out} + c \text{ (pressure drop is given)}$$

\vec{n} : normal direction to the fiber surface,

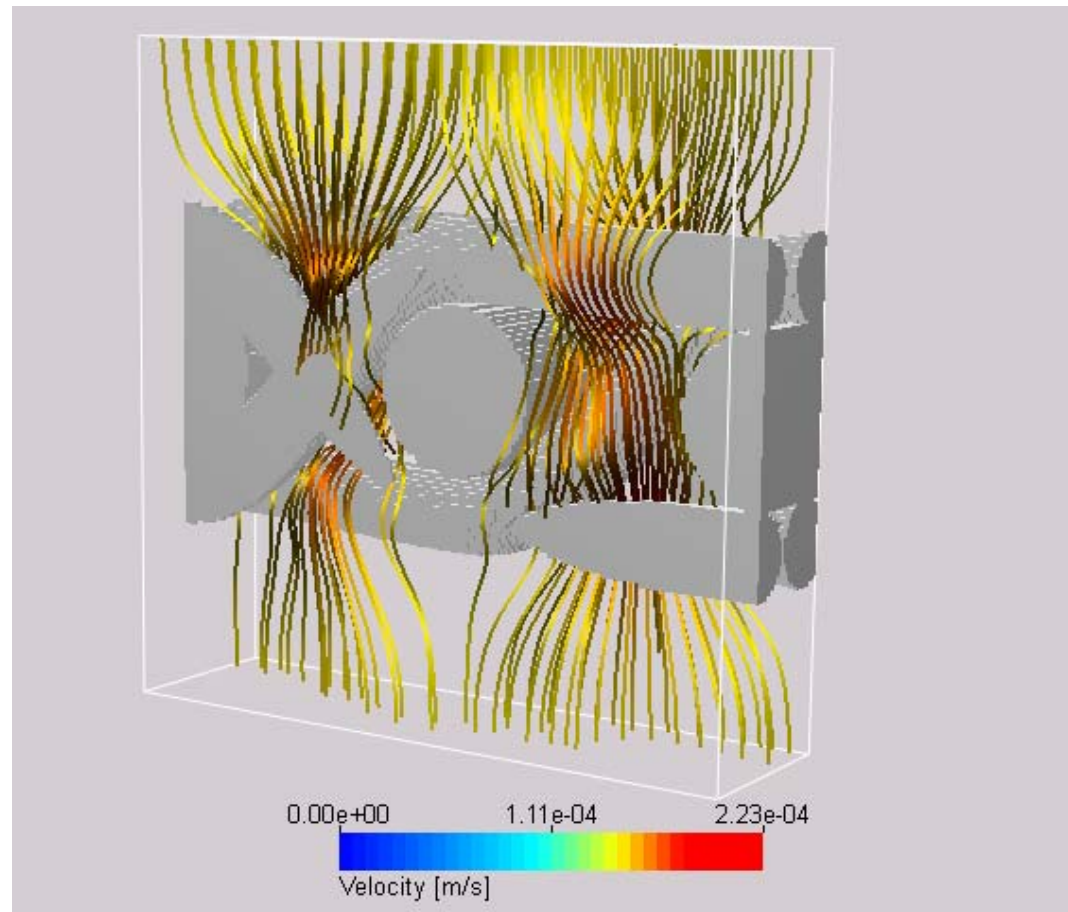
λ : slip length,

\vec{t} : any tangential direction with $\vec{t} \cdot \vec{n} = 0$.

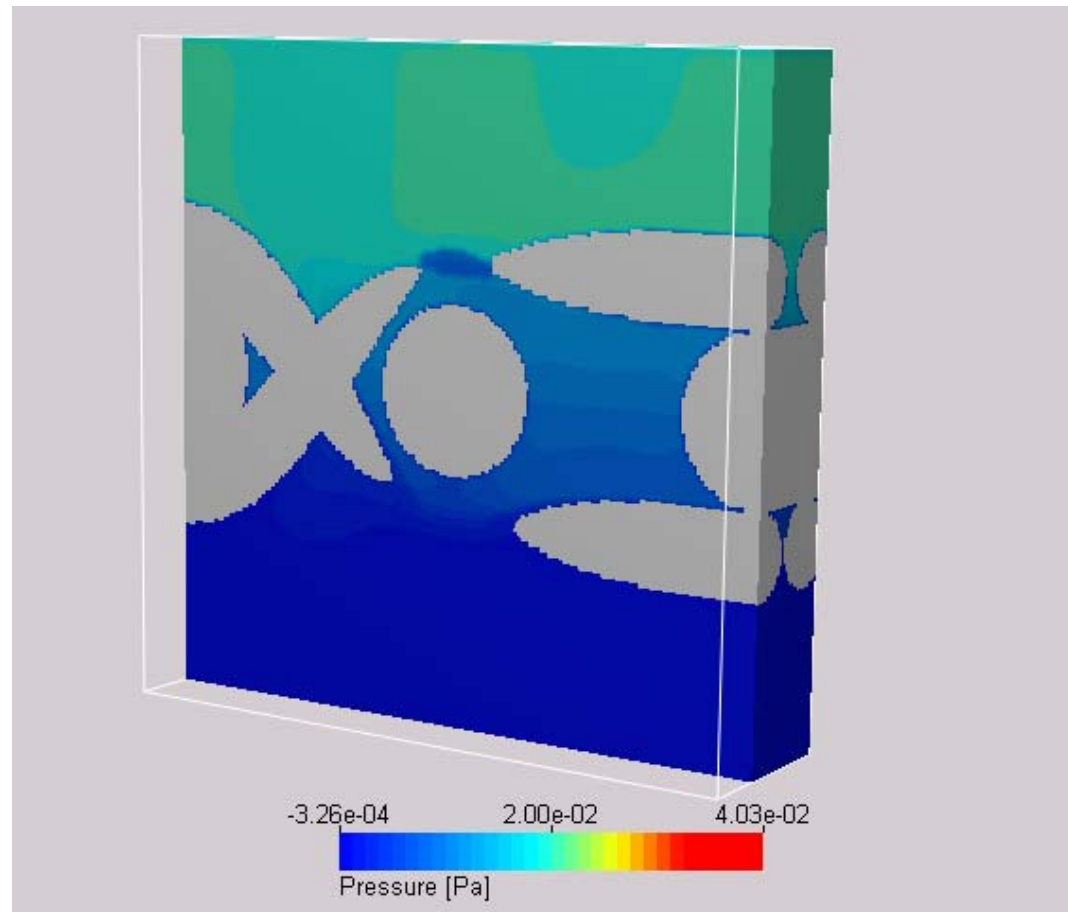
Pressure and Velocity in Clogging Simulation



Flow Field Visualization



Pressure Drop Visualization

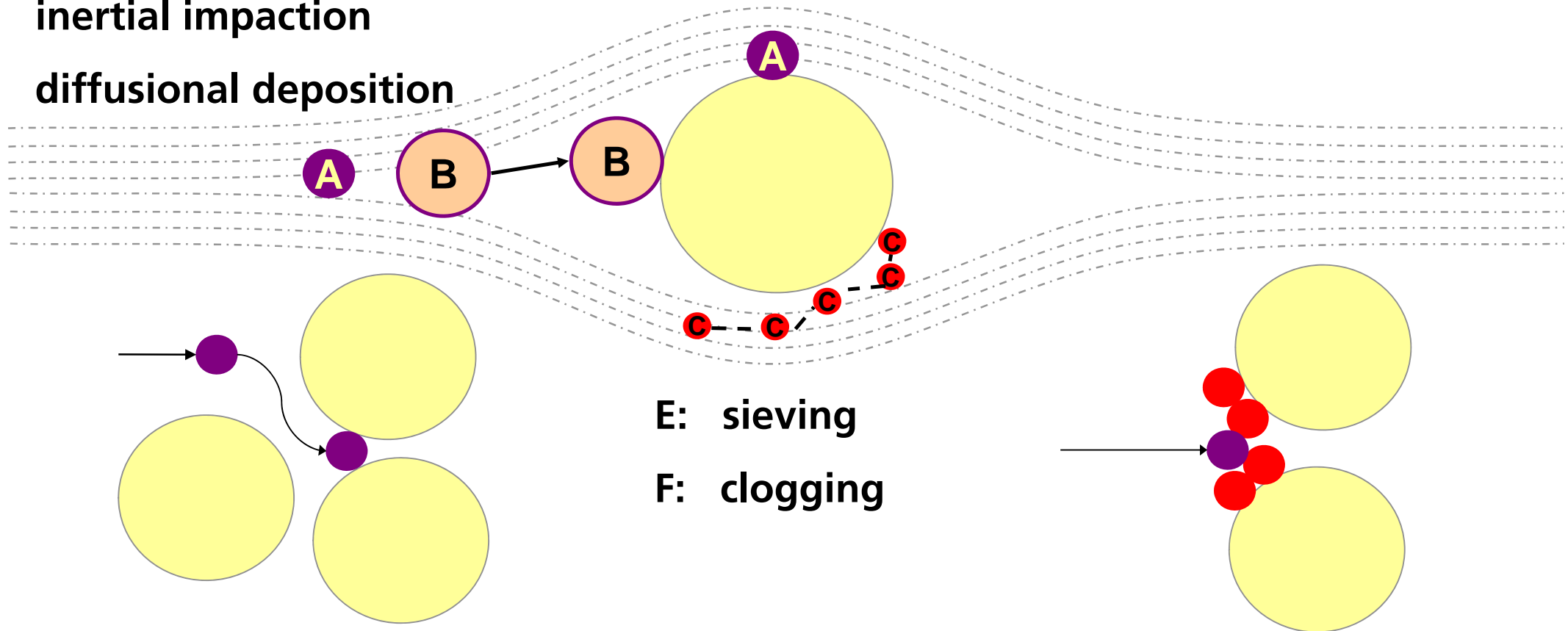


Filtration Effects I

A: direct interception

B: inertial impaction

C: diffusional deposition

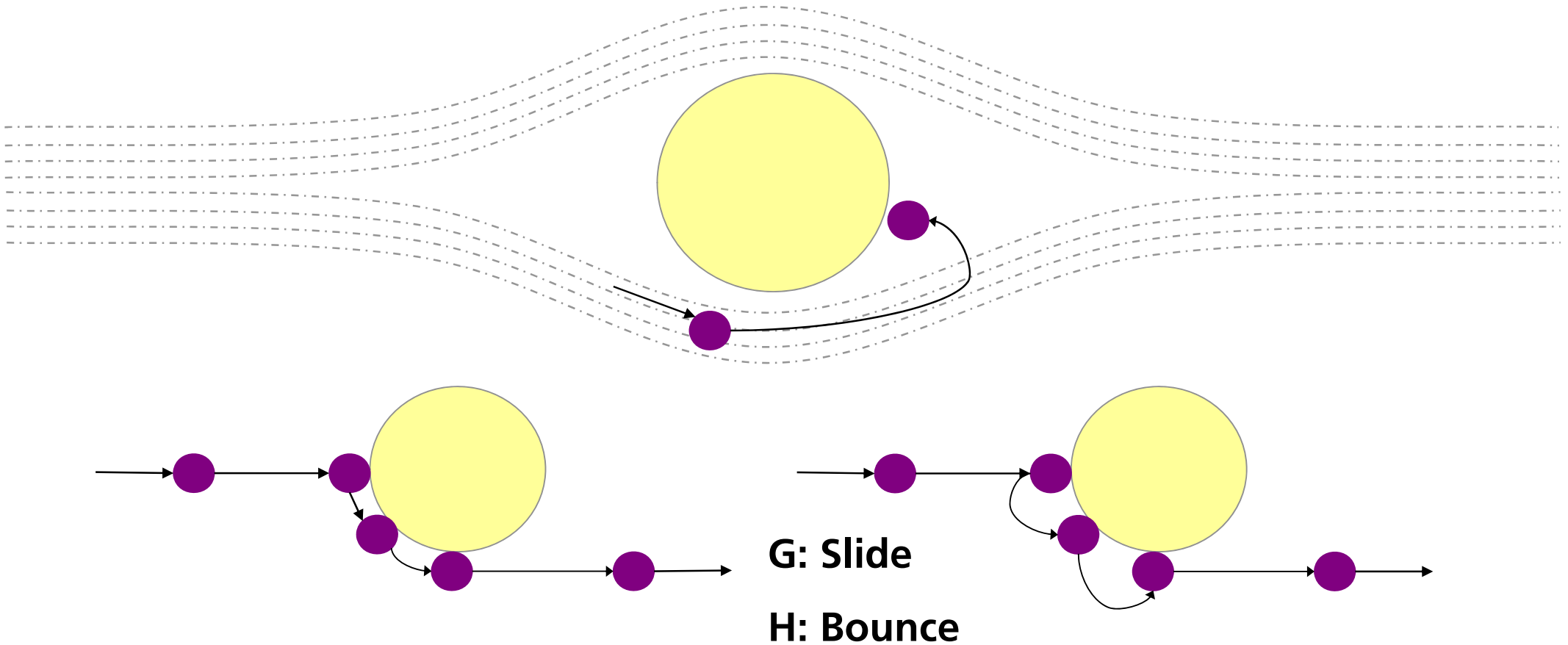


E: sieving

F: clogging

Filtration Effects II and modes of particle motion

D: electrostatic attraction



Description of particle motion

$$d\vec{x} = \vec{v} dt, \quad \text{Friction with fluid} \quad \text{Electric attraction} \quad \text{Diffusive motion}$$

$$d\vec{v} = -\gamma \times (\vec{v}(\vec{x}) - \vec{v}_o(\vec{x})) dt + \frac{Q\vec{E}_o(\vec{x})}{m} dt + \sigma \times d\vec{W}(t),$$

$$C_c = 1 + Kn \left(1.142 + 0.558 e^{-0.999/Kn} \right),$$

$$\gamma = 6\pi\rho\mu\frac{R}{C_cm},$$

$$\sigma^2 = \frac{2k_BT\gamma}{m},$$

$$\langle dW_i(t), dW_j(t) \rangle = \delta_{ij} dt,$$

$$Kn = \frac{\lambda}{R},$$

$$\lambda = \frac{k_BT}{\sqrt{32}\pi R^2 P}$$

t : time

\vec{x} : particle position

\vec{v} : particle velocity

R : particle radius

m : particle mass

q : particle charge

T : ambient temperature

P : total pressure

$d\vec{W}(t)$: 3d probability (Wiener) measure

γ : friction coefficient

k_B : Boltzmann constant

\vec{E}_o : electric field

\vec{v}_o : fluid velocity

ρ : fluid density

μ : fluid viscosity

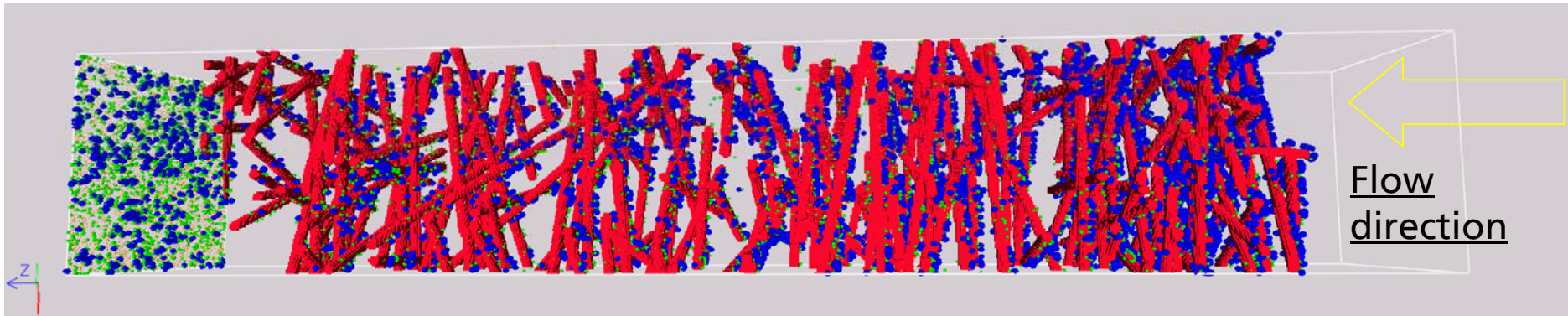
Deposition effects

$$\alpha = 0.05,$$

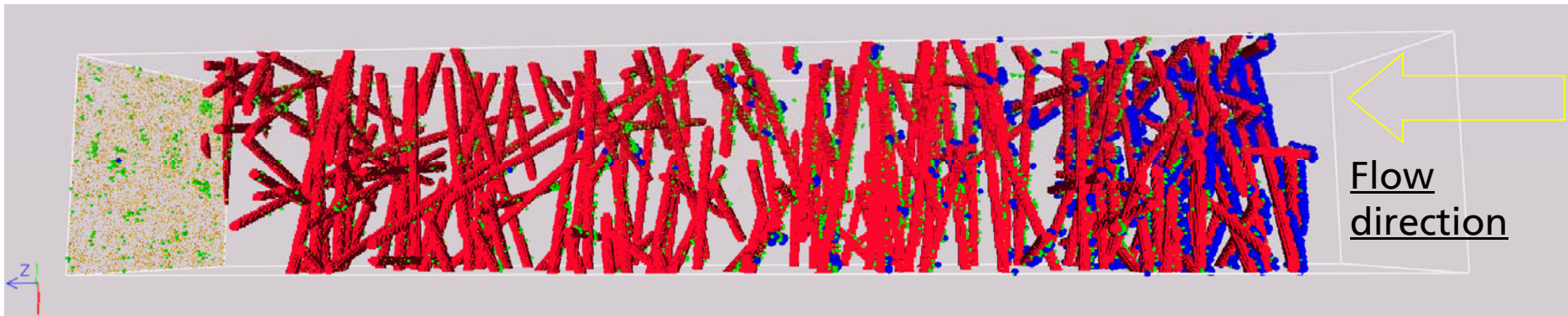
$$d_F = 14,$$

$$v = 0.1\text{m/s}$$

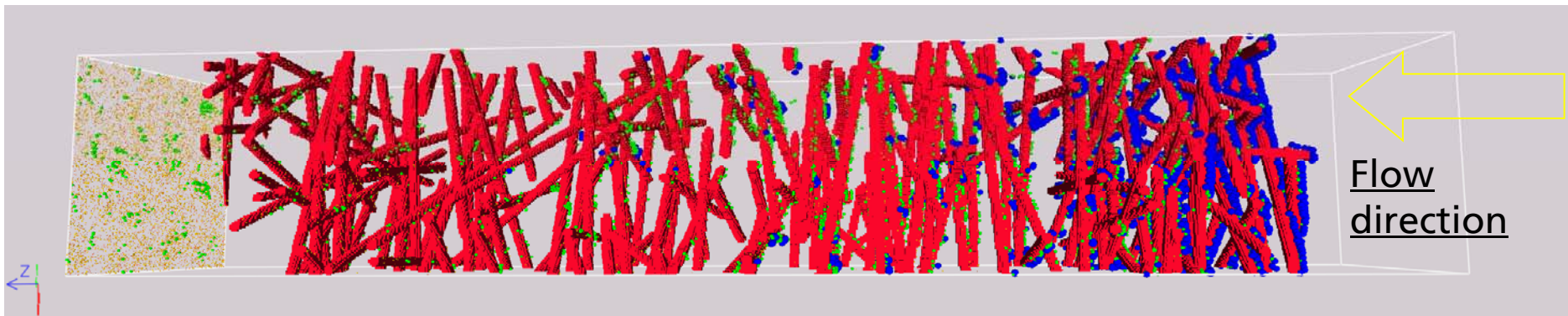
Interception



Interception
+ Impaction



Interception
+ Impaction
+ Diffusion



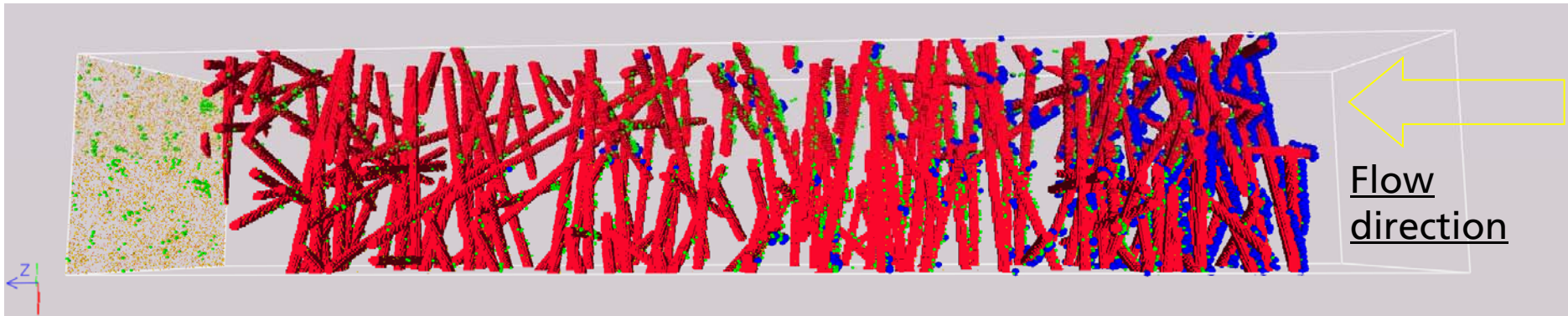
Velocity Effects

$$\alpha = 0.05,$$

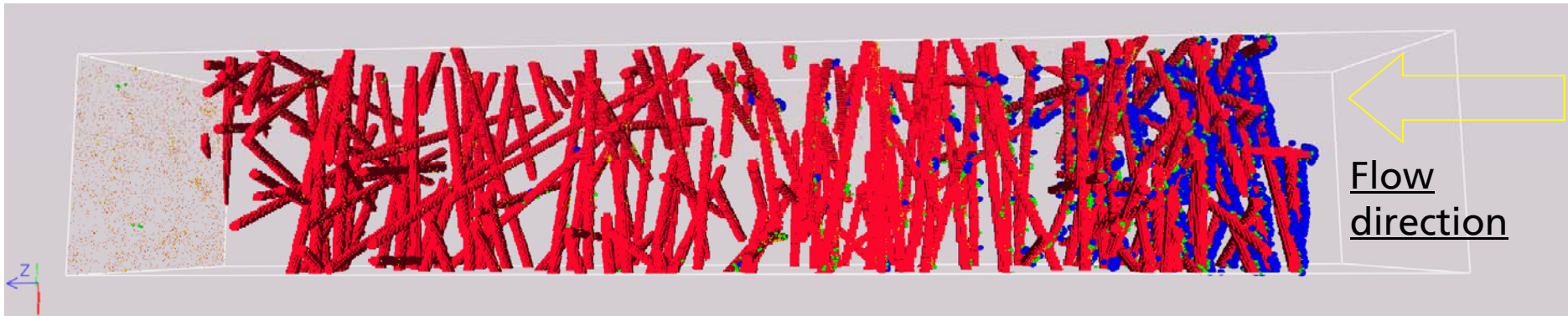
$$dF = 14,$$

Interception + Impaction + Diffusion

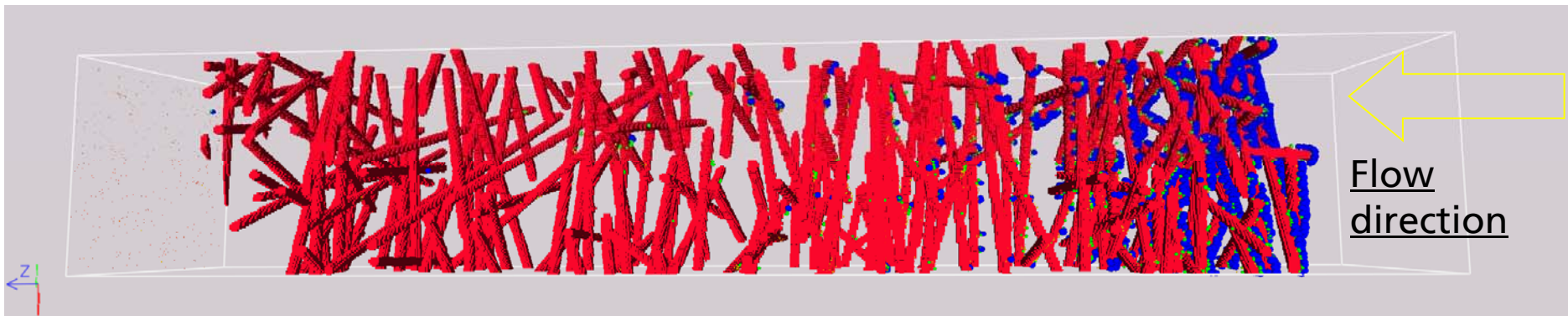
Velocity
 $v = 0.1 \text{ m/s}$



Velocity
 $v = 1 \text{ m/s}$



Velocity
 $v = 10 \text{ m/s}$



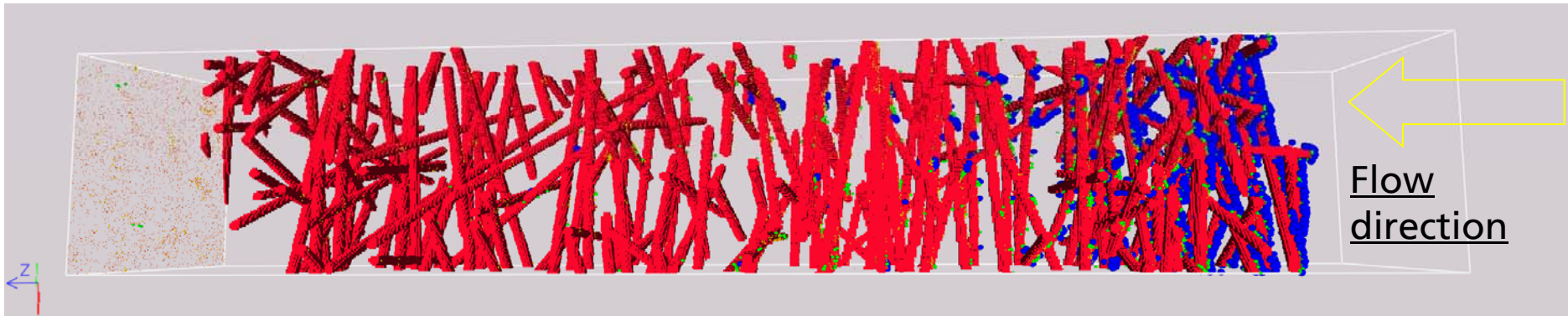
Effect of grammage (here: SVF)

$$dF = 14,$$

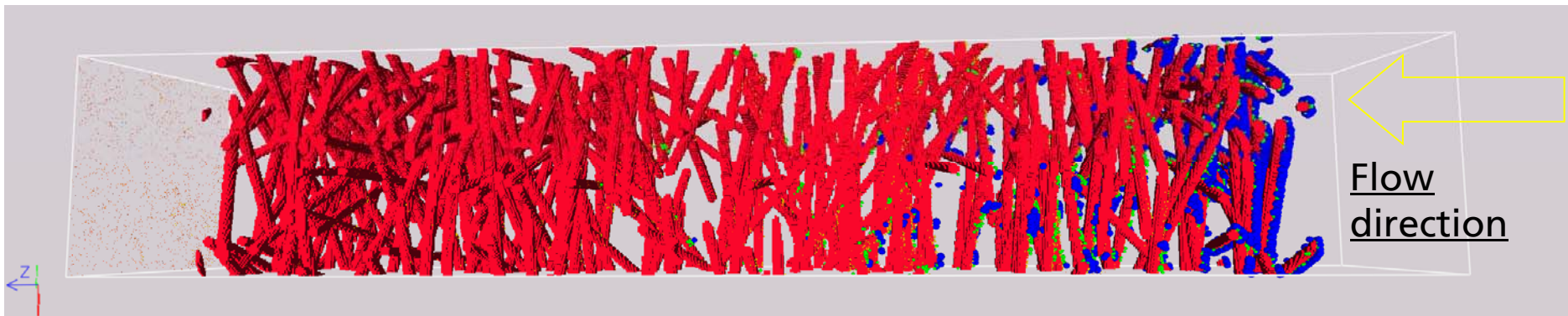
$$v = 1 \text{ m/s},$$

Interception + Impaction + Diffusion

SVF $\alpha=0.05$ _



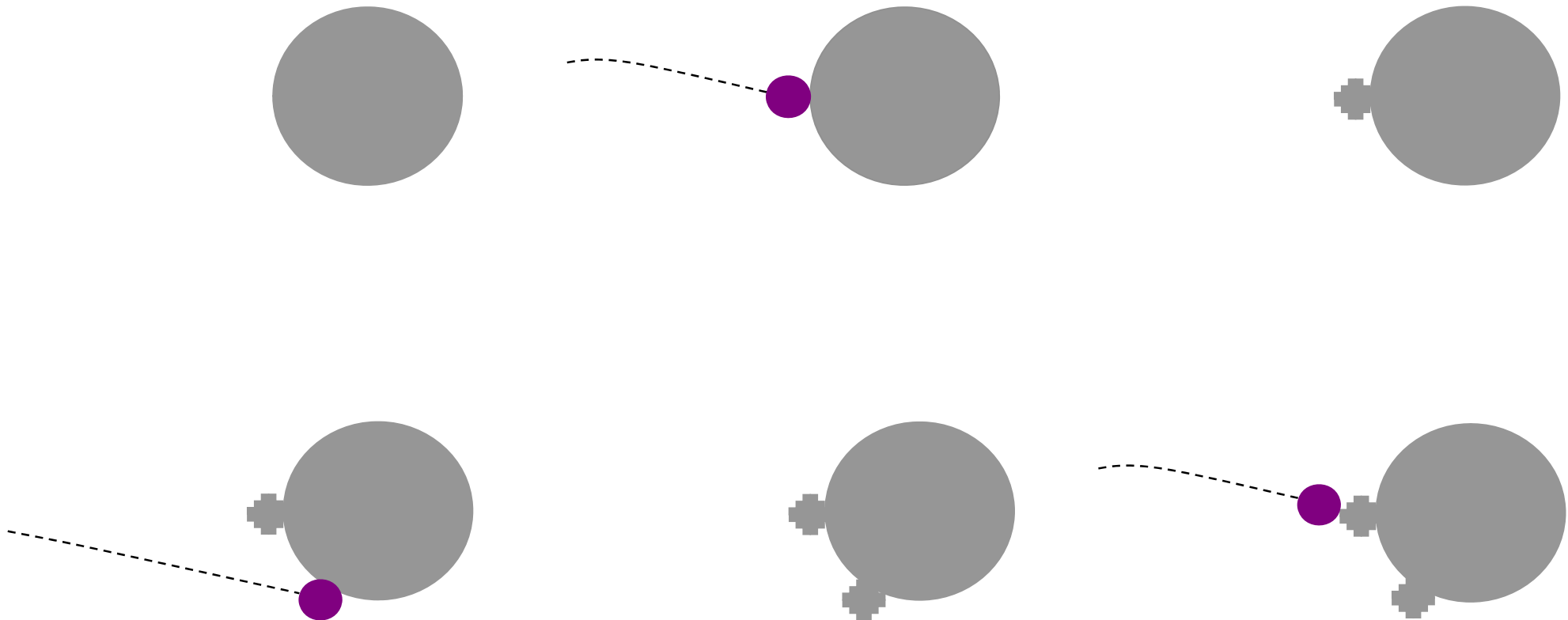
SVF $\alpha=0.07$ _



SVF $\alpha=0.1$



Nano-Modus

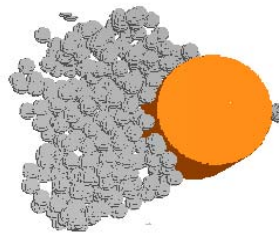


Influence of electric charge (air filtration)

No charges



Low charges

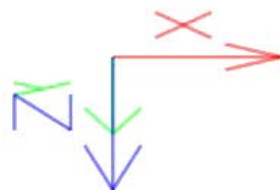


High charges



Deposition of resolved particles

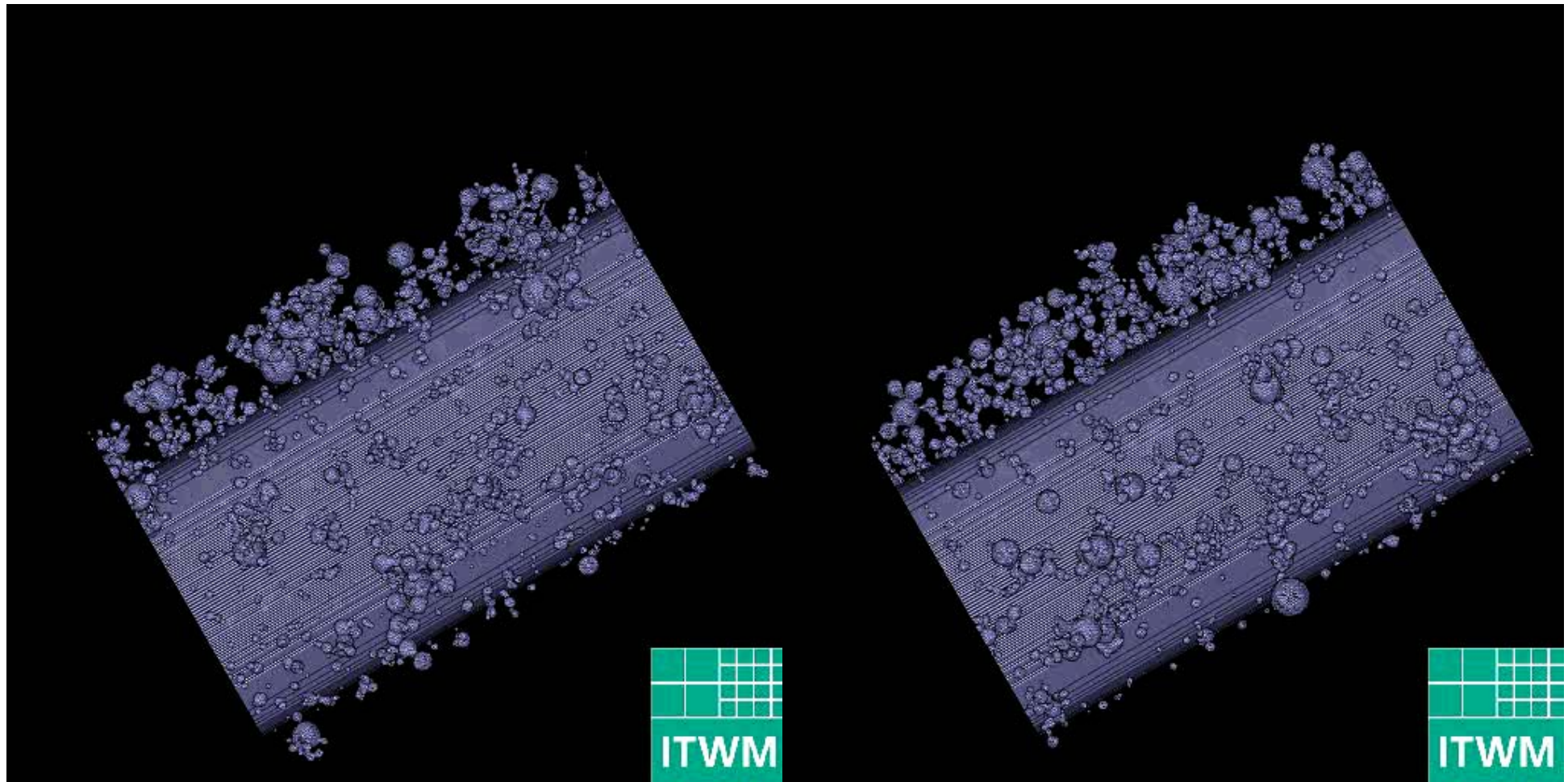
- Particles resolved by the cubes
- Filtration by “caught on first touch”
- Recompute flow after “batch” of particles
- Clogging in depth filtration



Nano Simulations

1.67cm/sec

10.0cm/sec



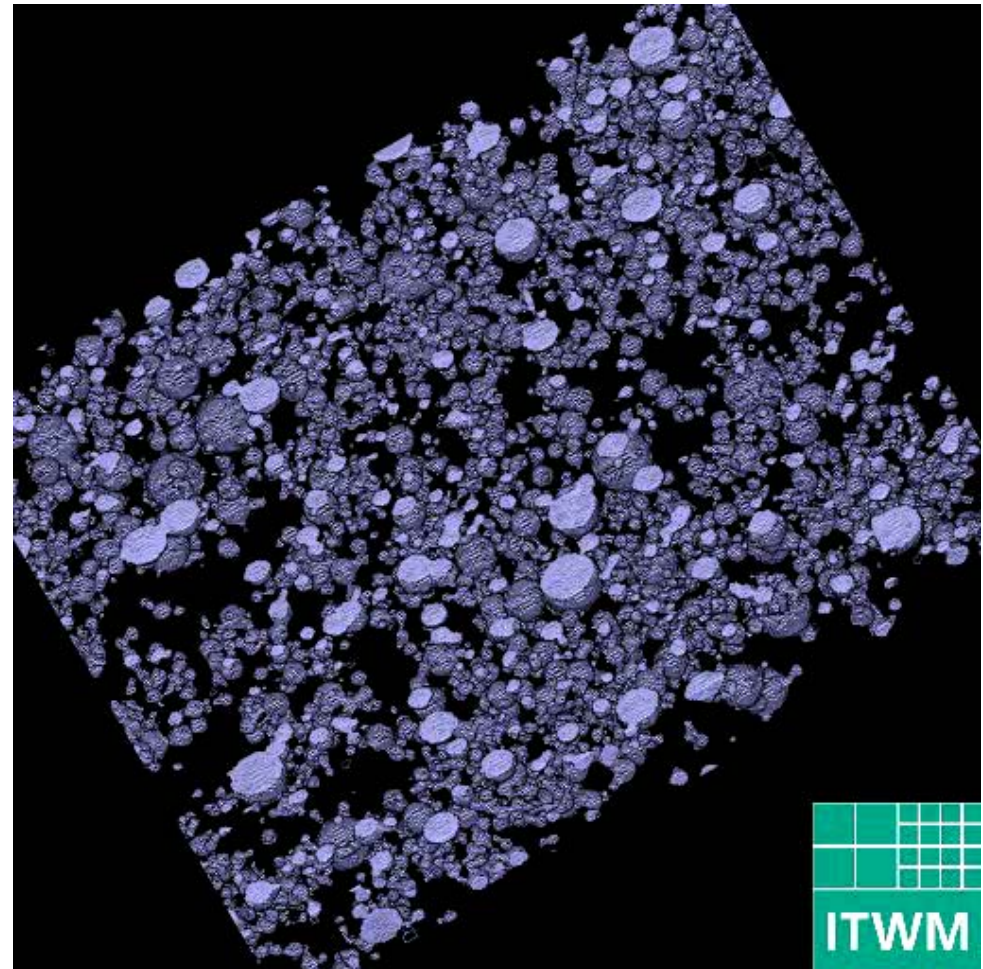
Nano Simulations

- Deposition patterns and porosity depend on far field velocity, particle size distribution, etc.

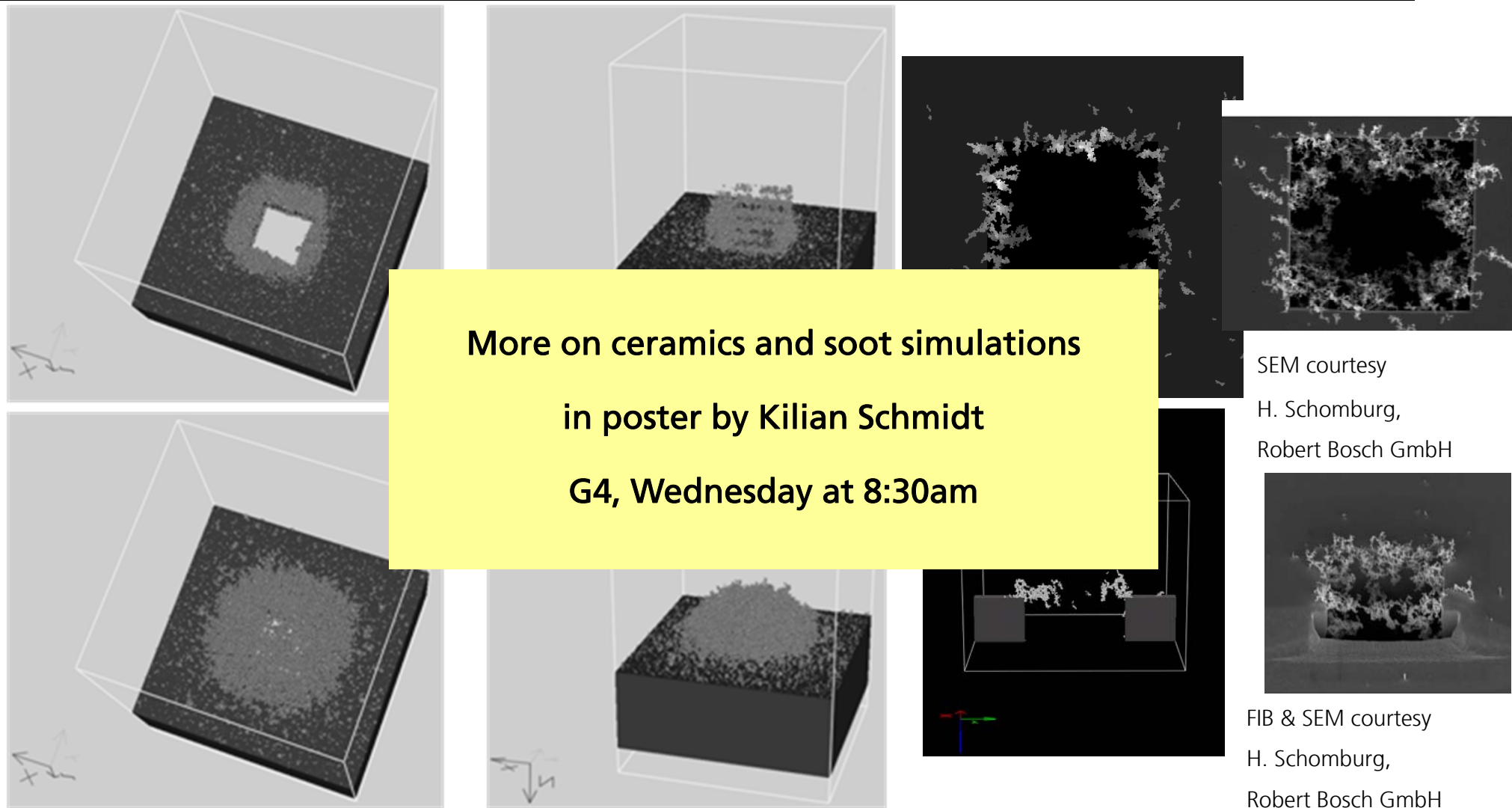
Result:

- Find minimal **porosity** and **permeability** of the soot layers, s_{\max} and κ_{\min}
- Derivation by layers from single fiber highly resolved simulations

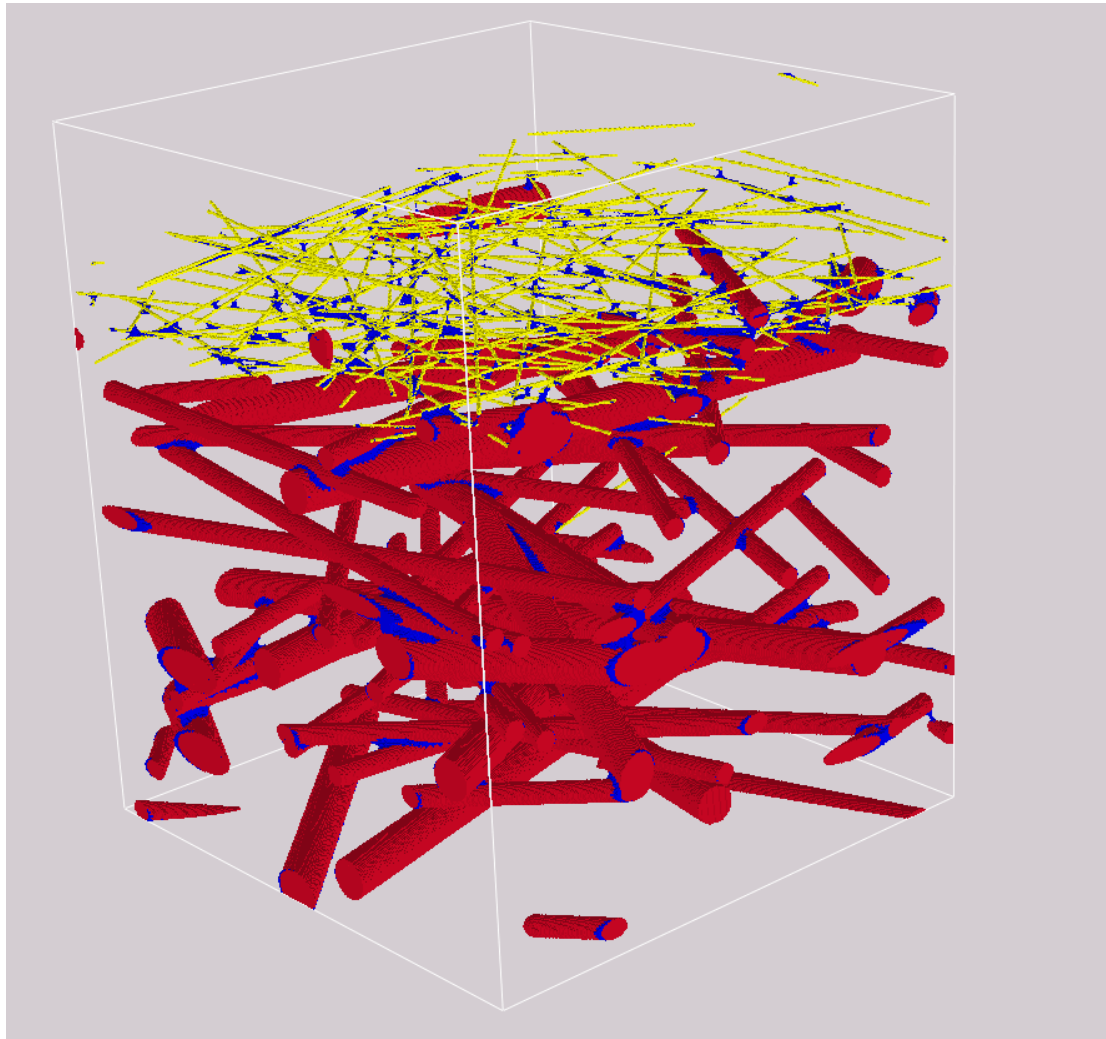
Soot Layer Cut-Out



3d view, virtual SEM and real SEM (with FIB) of soot on micro sieve



Nonwoven with binder and layer of nano fibers

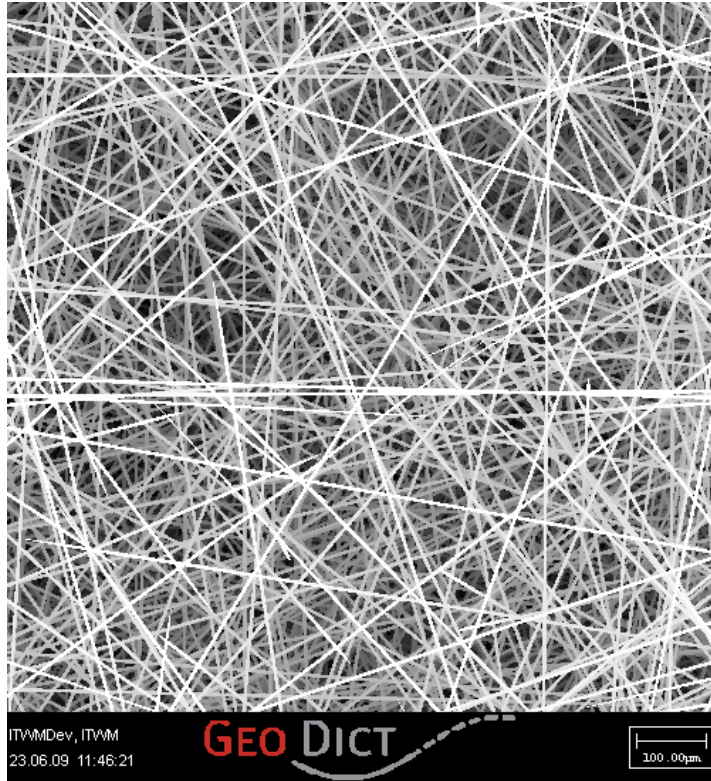


5.0 μm fibers (red)
2.5 μm fibers (red)
0.3 μm fibers (yellow)
2 vol % binder (blue)

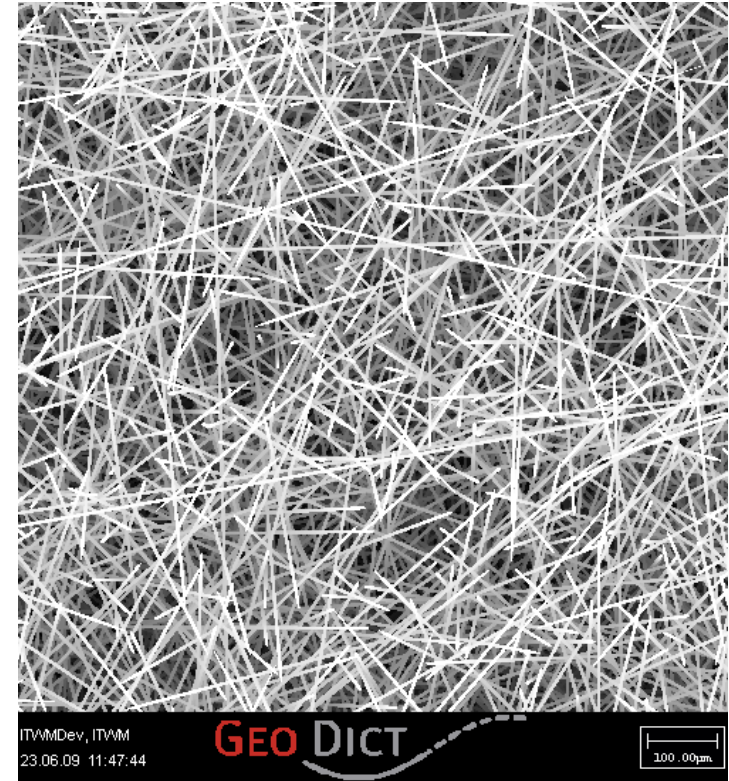
More on nano filtration media
in talk by Liping Cheng
G15, Thursday at 3:00pm

Nonwoven

SEM visualization of 8 volume percent 5 micron fibers

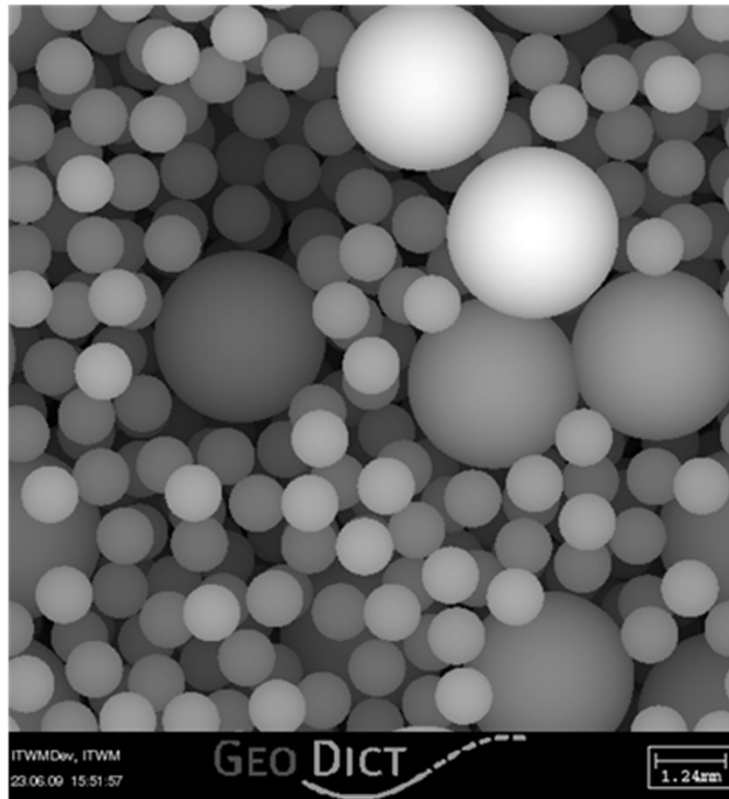


anisotropy 100

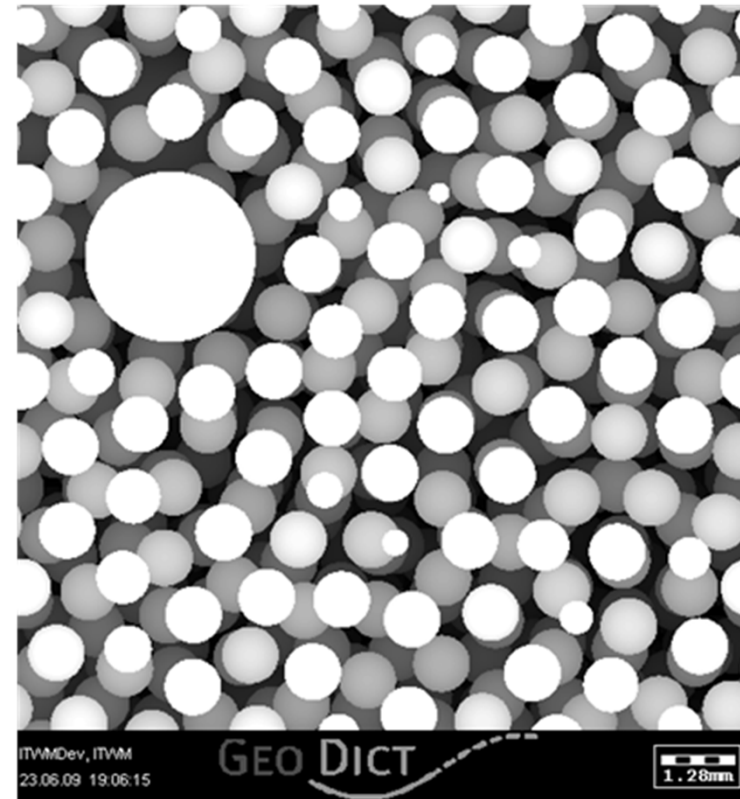


anisotropy 7

Packed bed of spheres and floating spheres

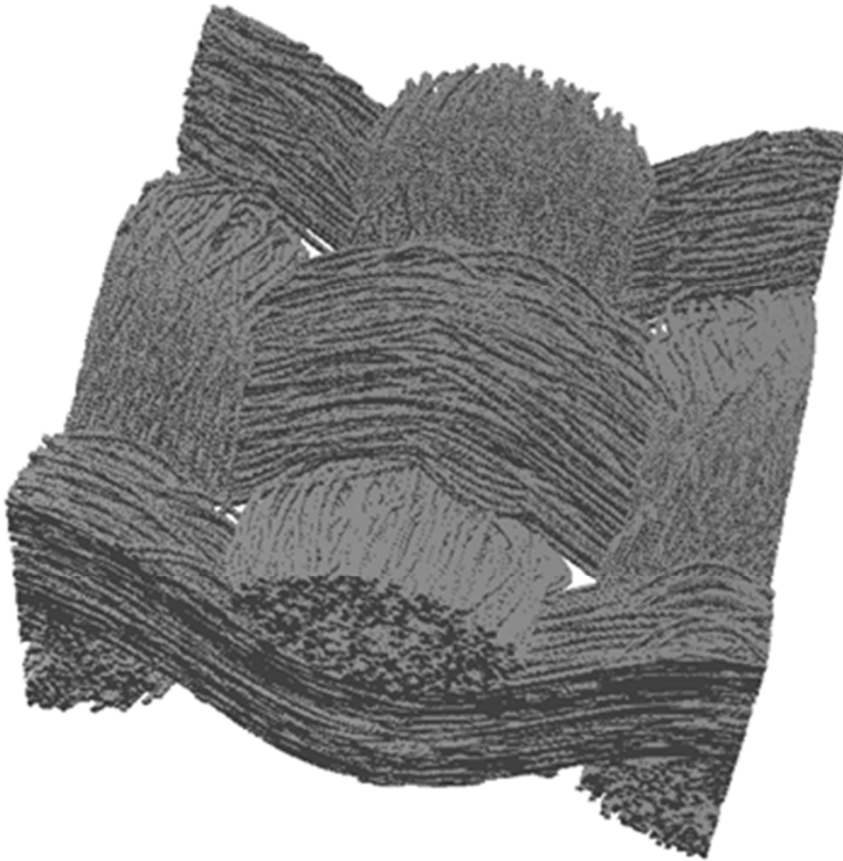


svf 0.64



svf 0.30

Carbon fiber multi-filament woven



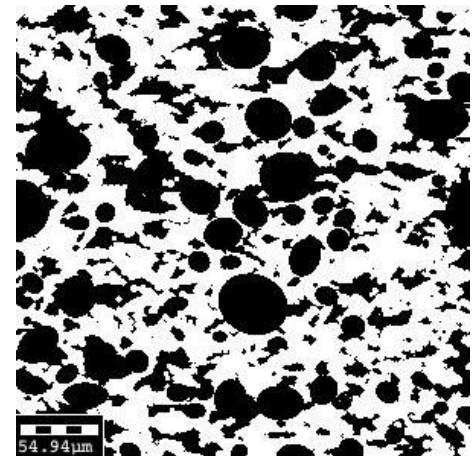
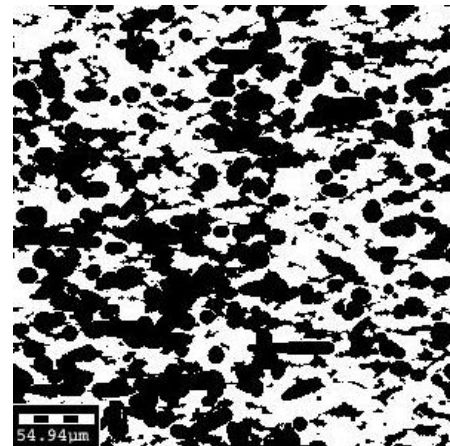
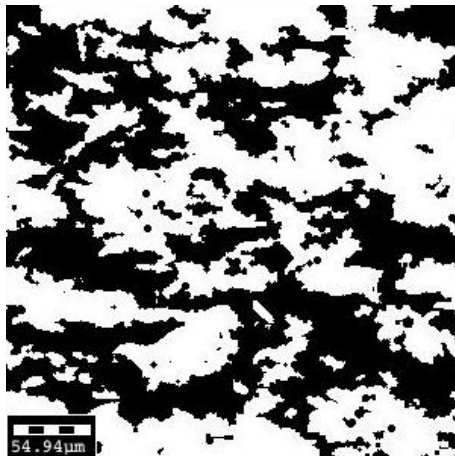
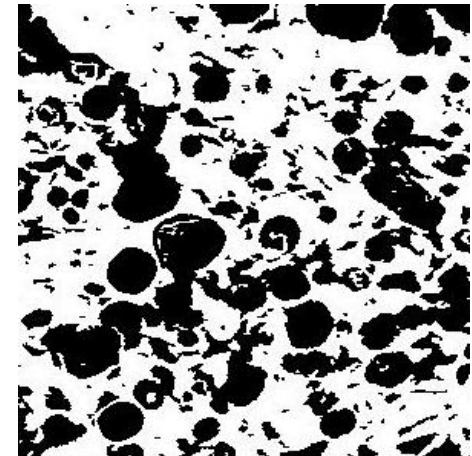
3D Visualization (generated)



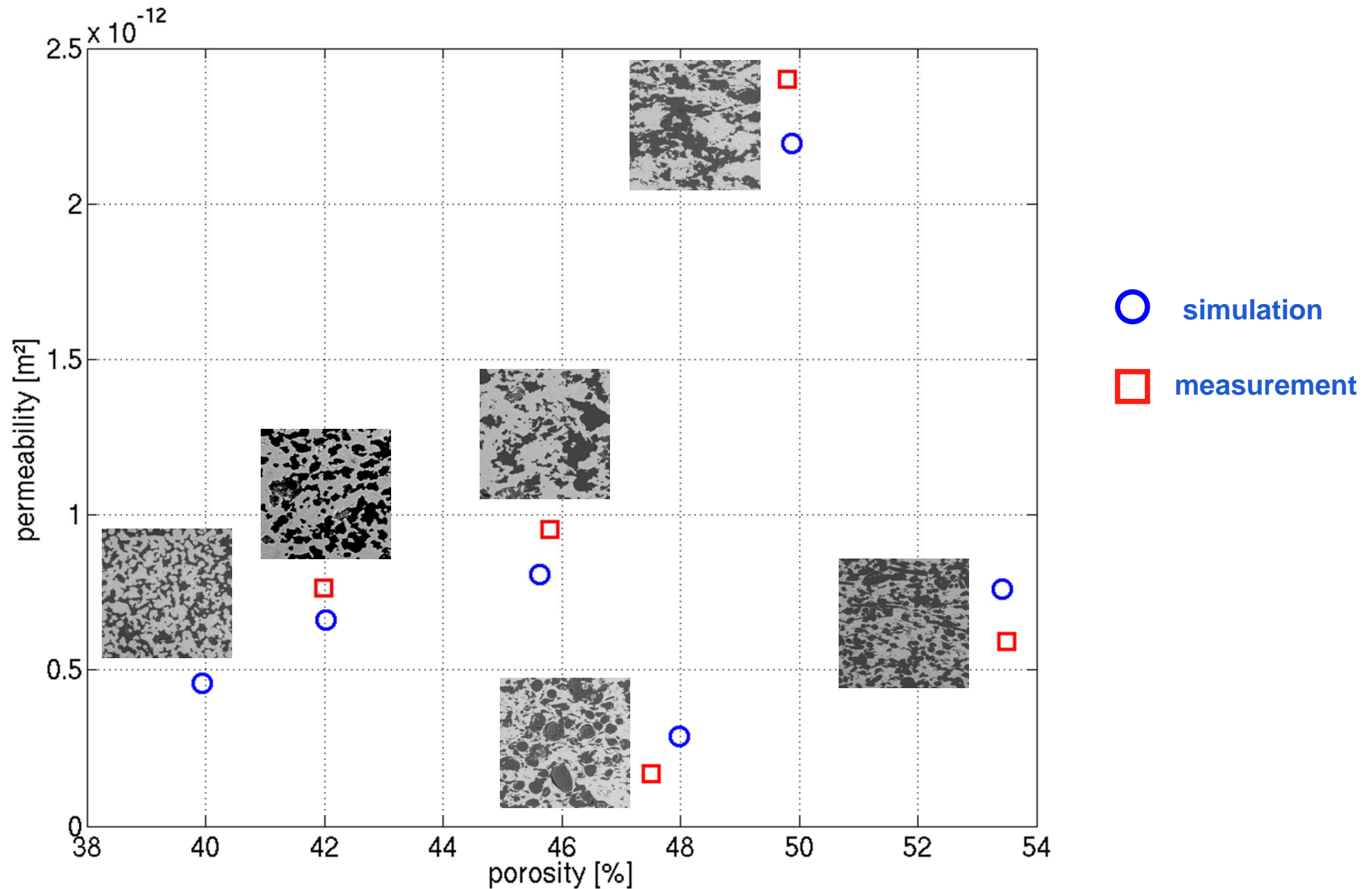
SEM (real)

(SEM courtesy of Jeff Gostick, Univ. of Waterloo)

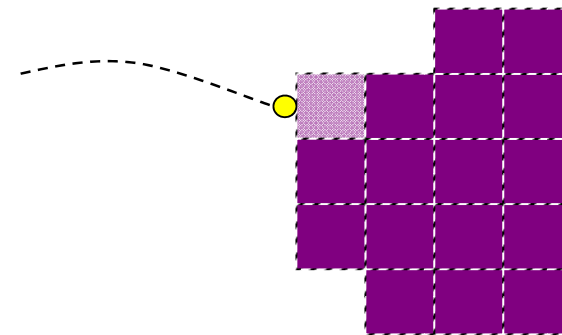
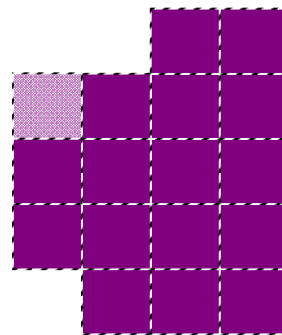
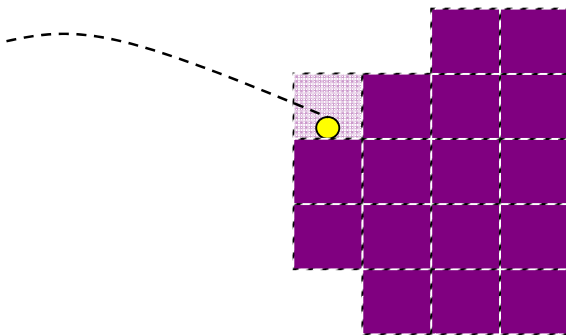
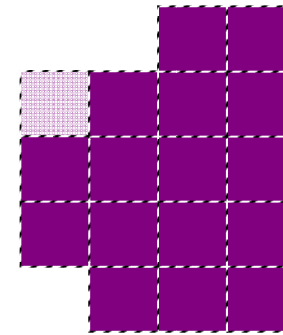
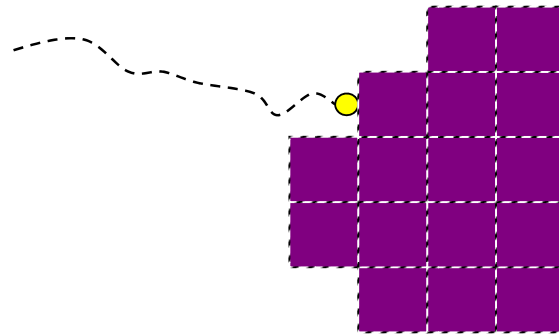
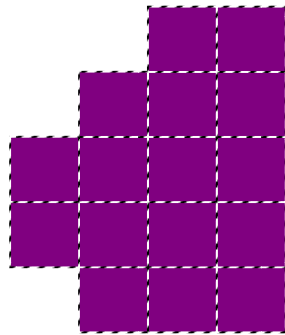
Binarized SEM (top) and virtual sintered ceramics (bottom)



Computed and measured porosities and permeabilities of real & generated structures (from polished micrograph sections)



Mikro-Modus



Stationary Flow with unresolved particles: Stokes-Brinkmann eqs

$$\begin{aligned} -\mu\Delta\vec{u} + \nabla\vec{u} \cdot \vec{u} + \nabla p + \kappa^{-1}\vec{u} &= \vec{f} \text{ (momentum balance)} \\ \nabla \cdot \vec{u} &= 0 \text{ (mass conservation)} \\ \vec{u} &= 0 \text{ on } \Gamma \text{ (no-slip on fiber surfaces)} \end{aligned}$$

$\vec{f} = (0, 0, f)$: force in flow(z)-direction,

$\kappa = \kappa_{min} \max\{1, s_{max}/s\}$: porous voxel permeability,
 s : solid volume fraction in a voxel

\vec{u} : velocity,

μ : fluid viscosity,

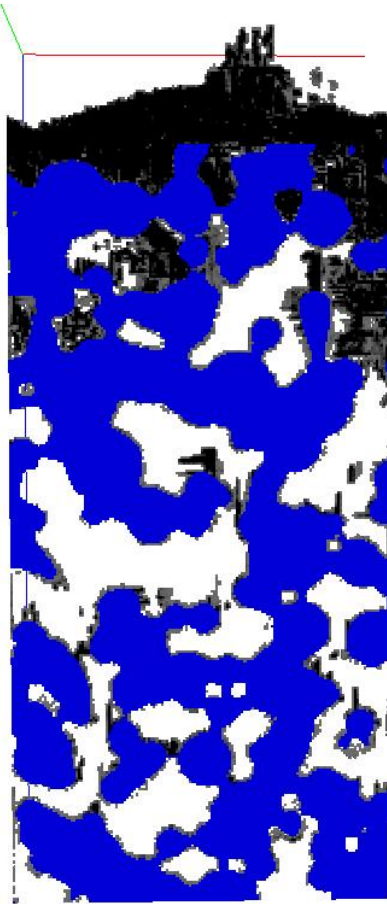
p : pressure and

Γ : fiber or deposited particle surfaces.

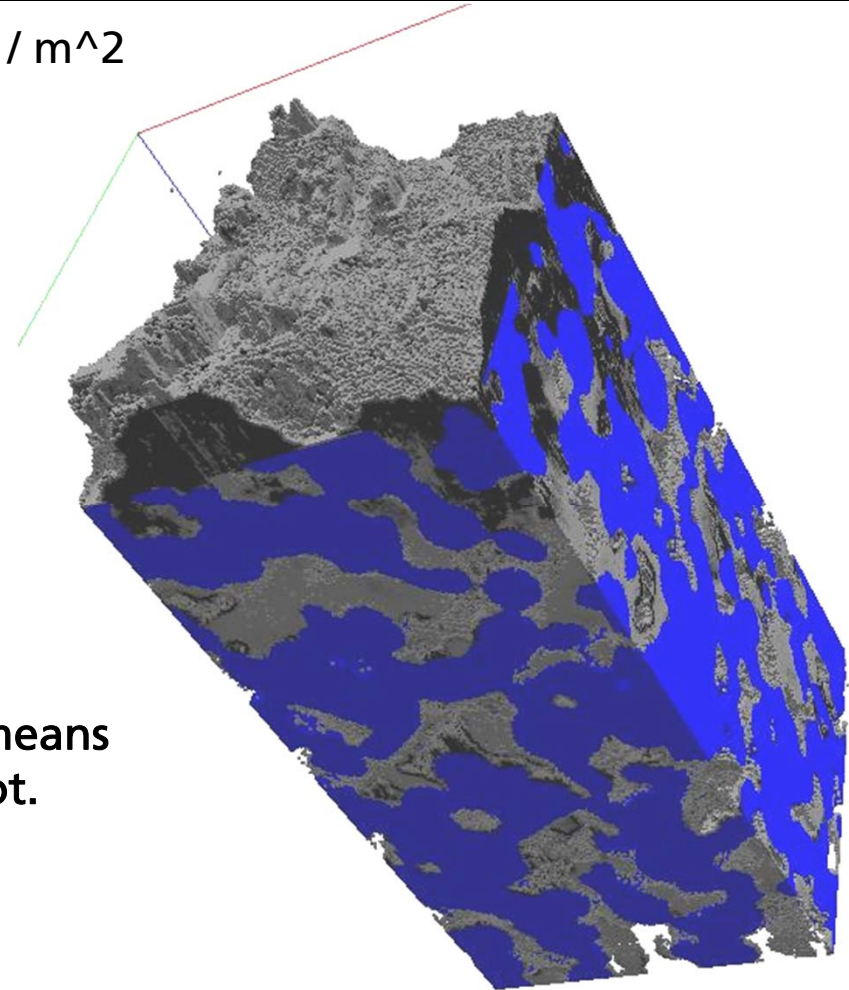
Solid volume fraction in voxel is increased until s_{max} is reached. Voxel becomes "collision-solid". Neighbor voxels svf starts increasing upon particle arrival

Micro Simulations

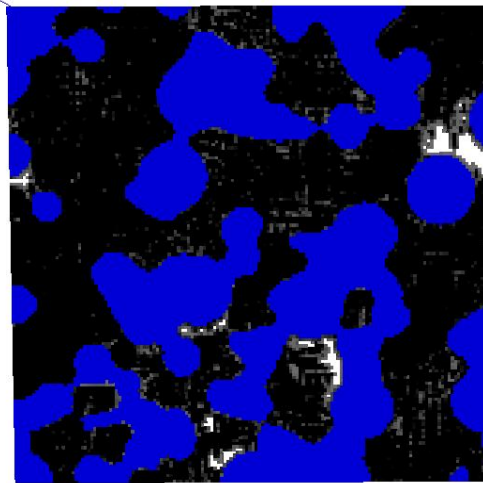
Final state at 5.1 g / m^2



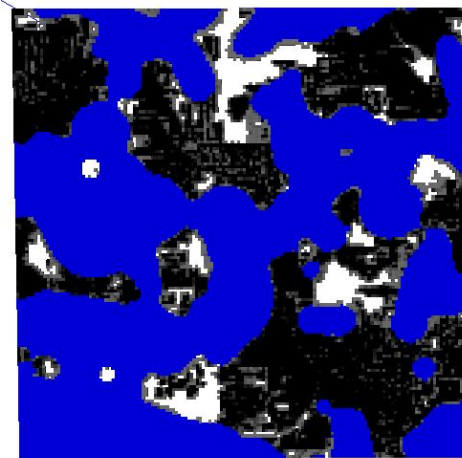
Darker gray means denser soot.



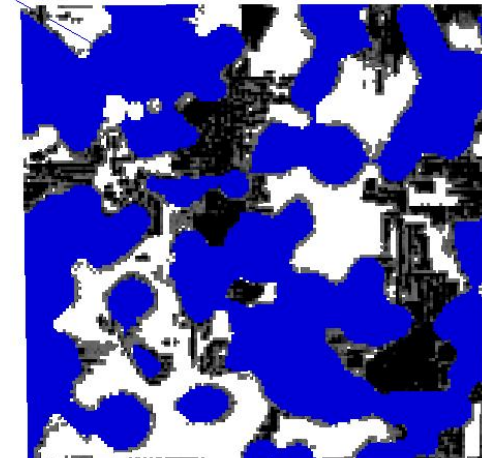
Horizontal layers



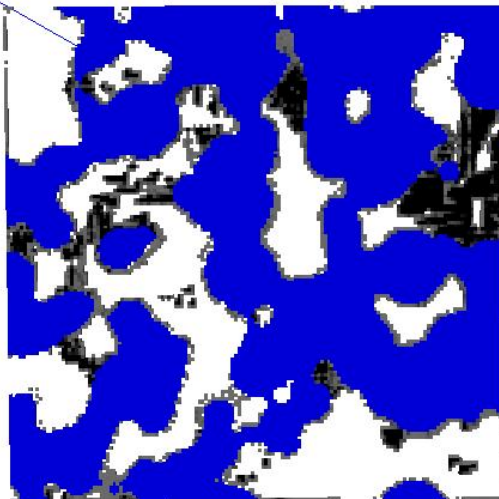
50



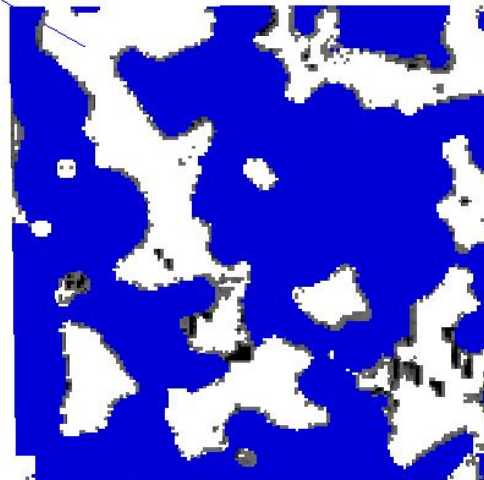
75



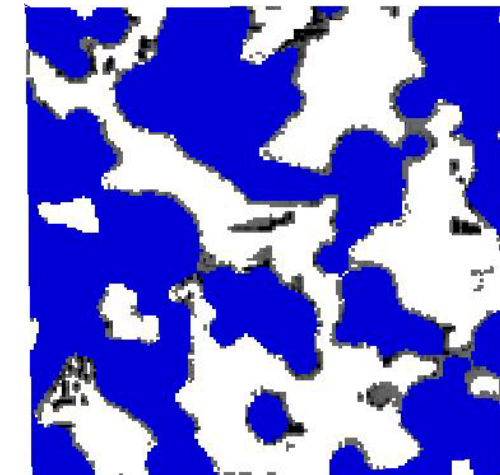
100



125



150



350



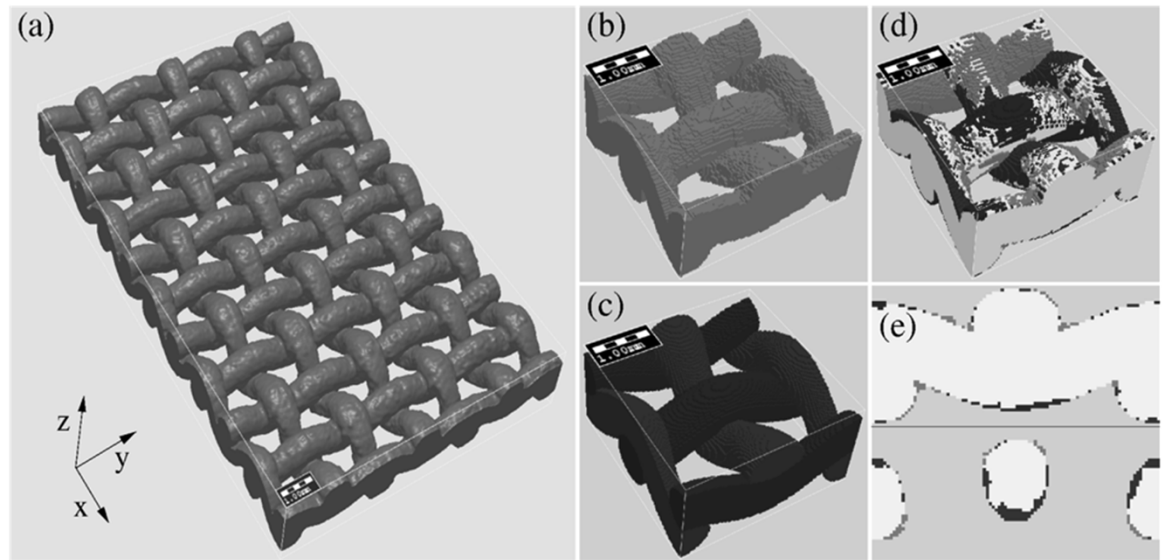
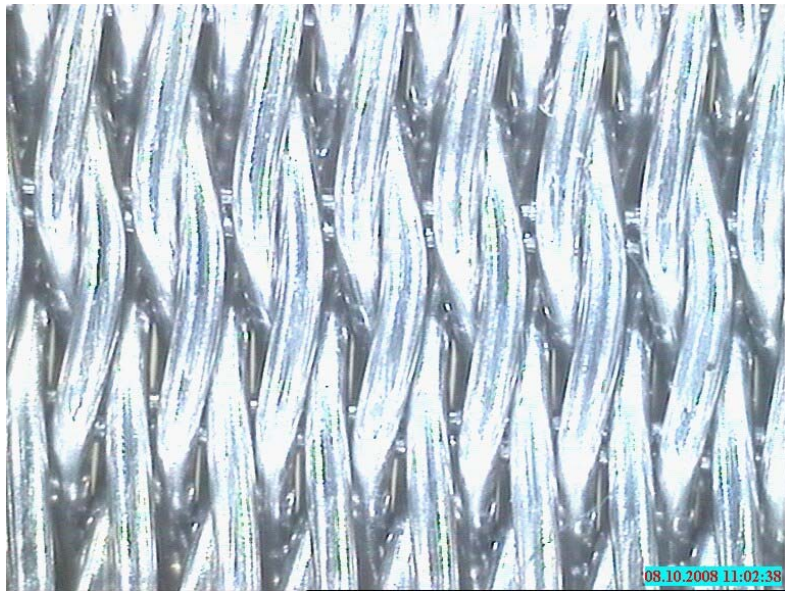
Fraunhofer
ITWM

Andreas Wiegmann

Filtech, Wiesbaden

13 October 2009

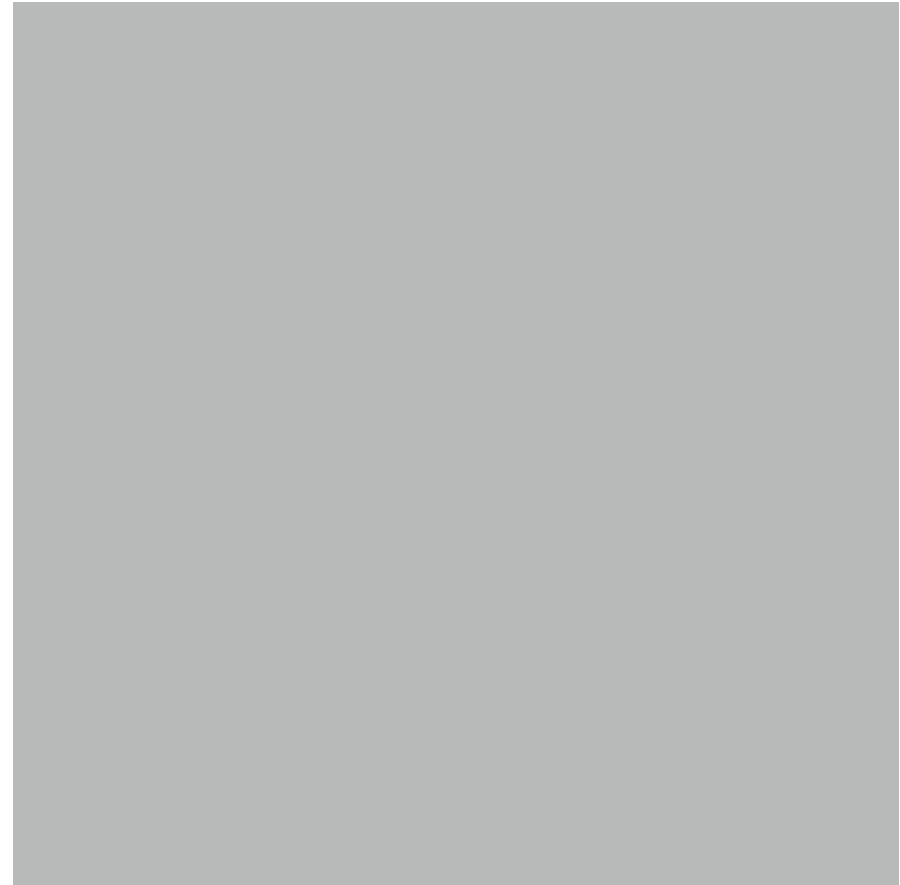
Reconstruction of Woven



More on woven simulations
in talk by Erik Glatt
L6, Wednesday at 11:50am

Surface filtration in metal wire cloth

- Filtration by “sieving”
- Recompute flow after “batch” of particles
- Cake formation in surface filtration
- Filter Cake more efficient filter than metal wire mesh
- Pressure drop increase also available

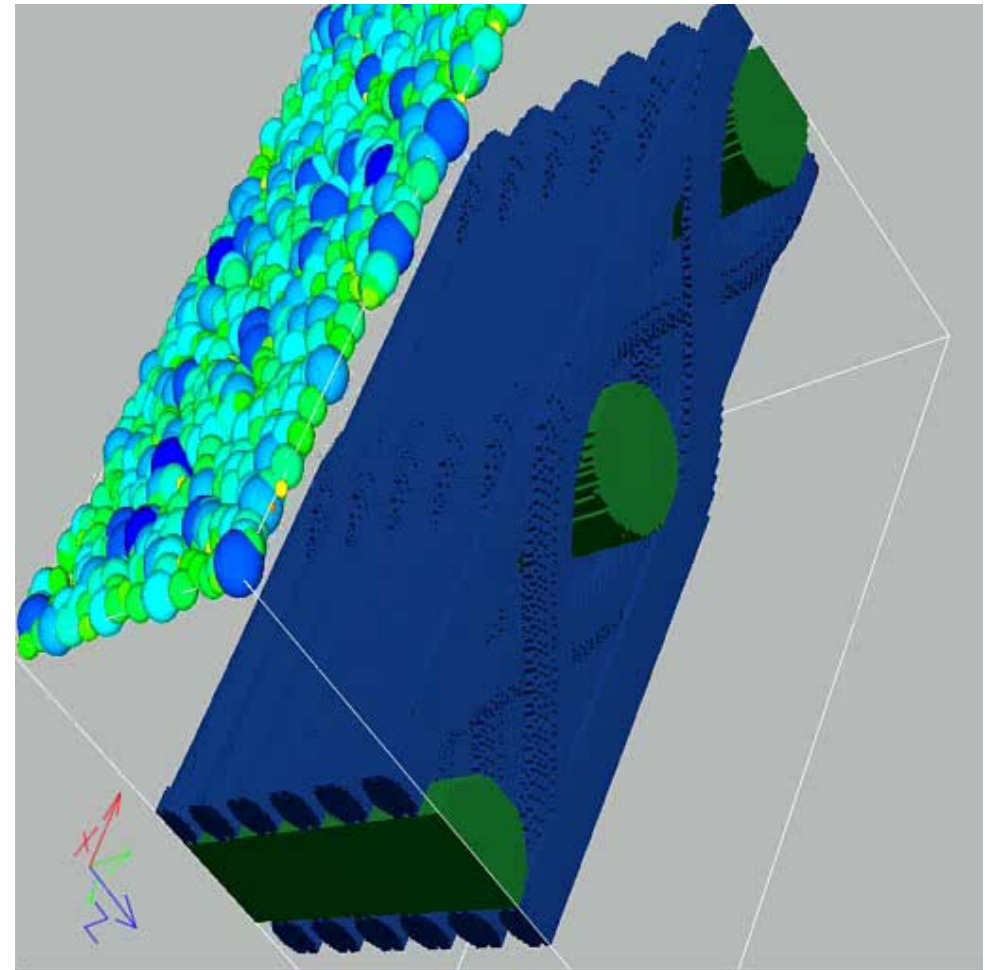


Computed & animated with **GEO DICT**

Courtesy M. Knefel, Gebr. Kufferath AG.

Surface filtration in metal wire cloth

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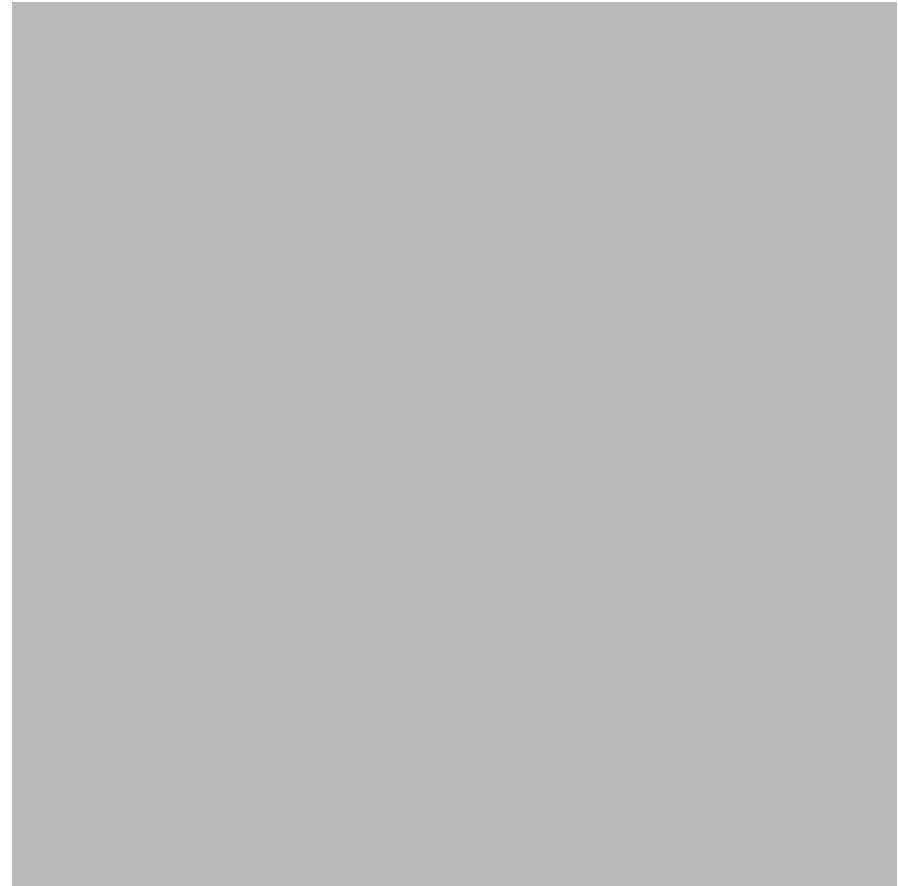


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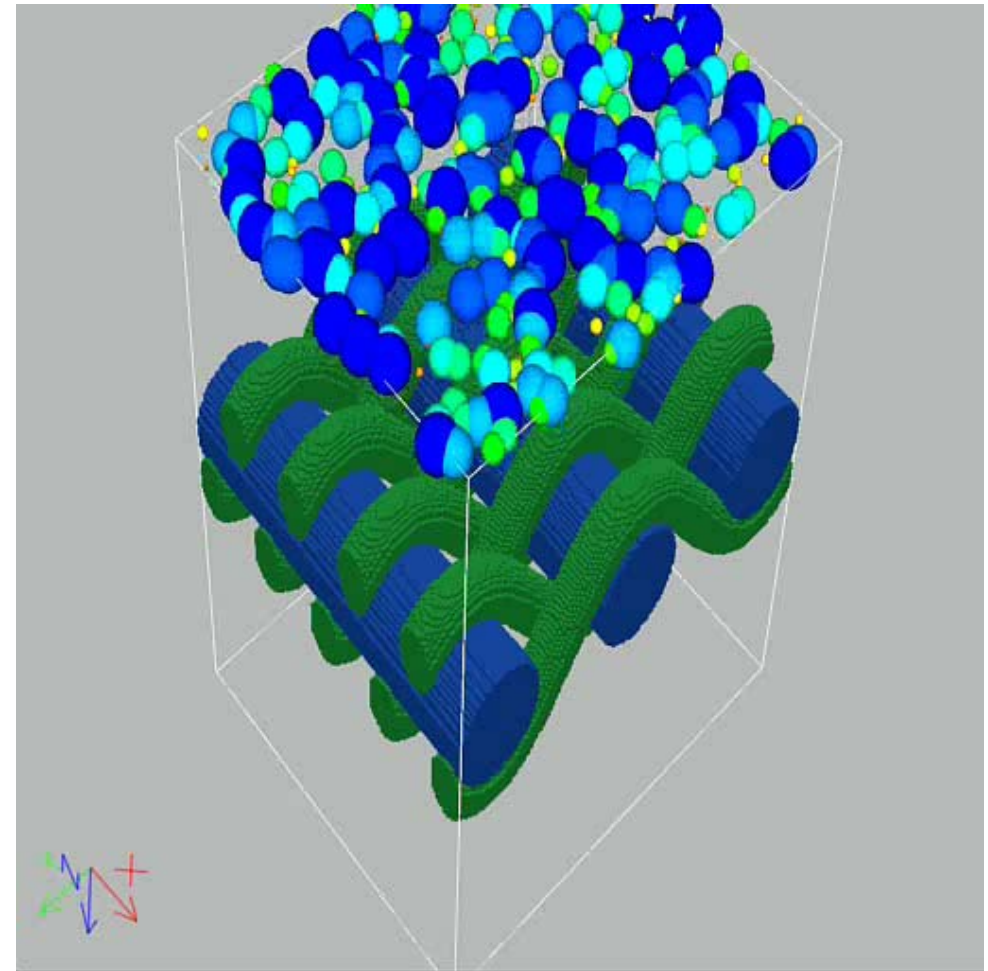


Computed & animated with **GEO DICT**

Courtesy M. Knefel, Gebr. Kufferath AG.

Surface filtration in metal wire cloth

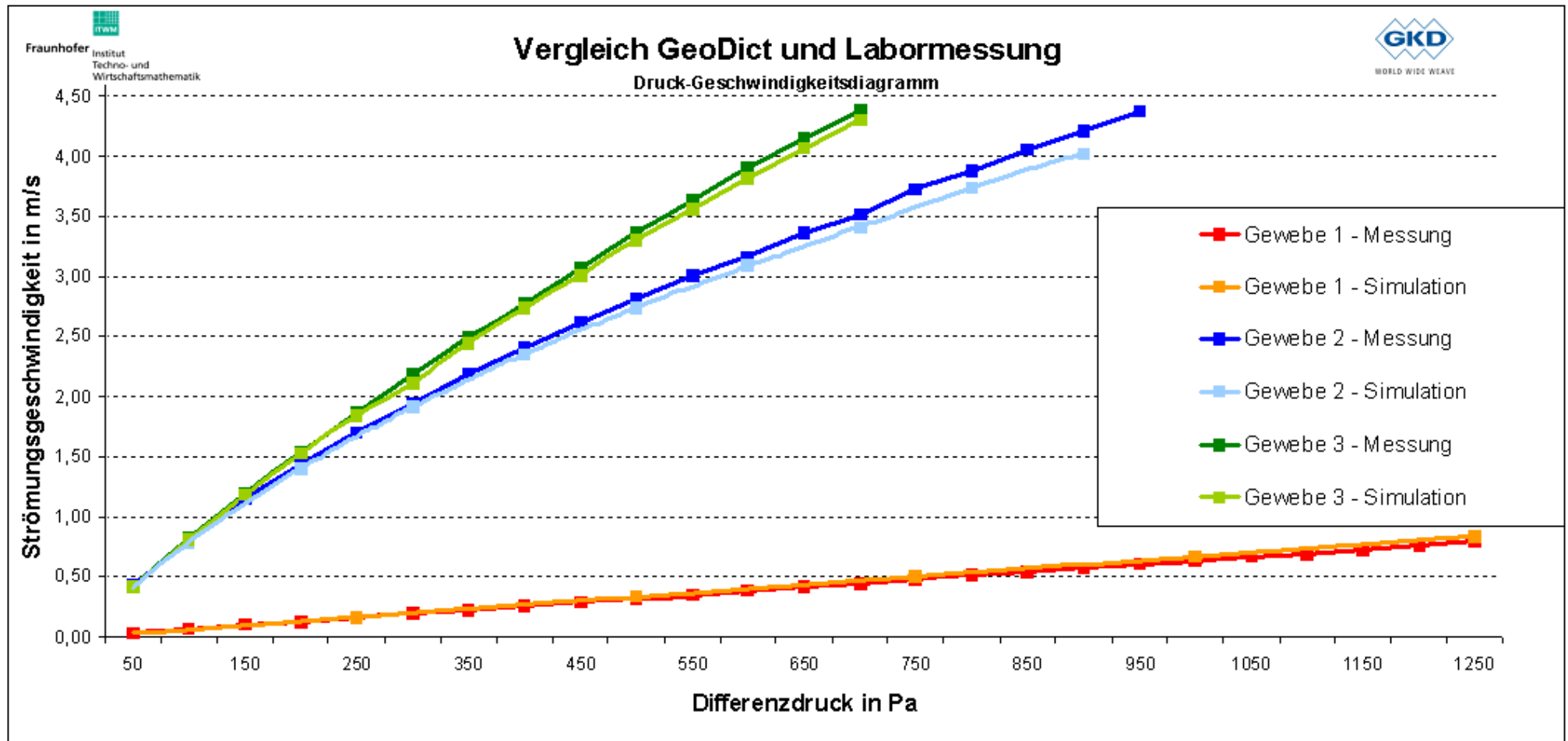
- Filtration by “sieving”
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Computed & animated with **GEO DICT**

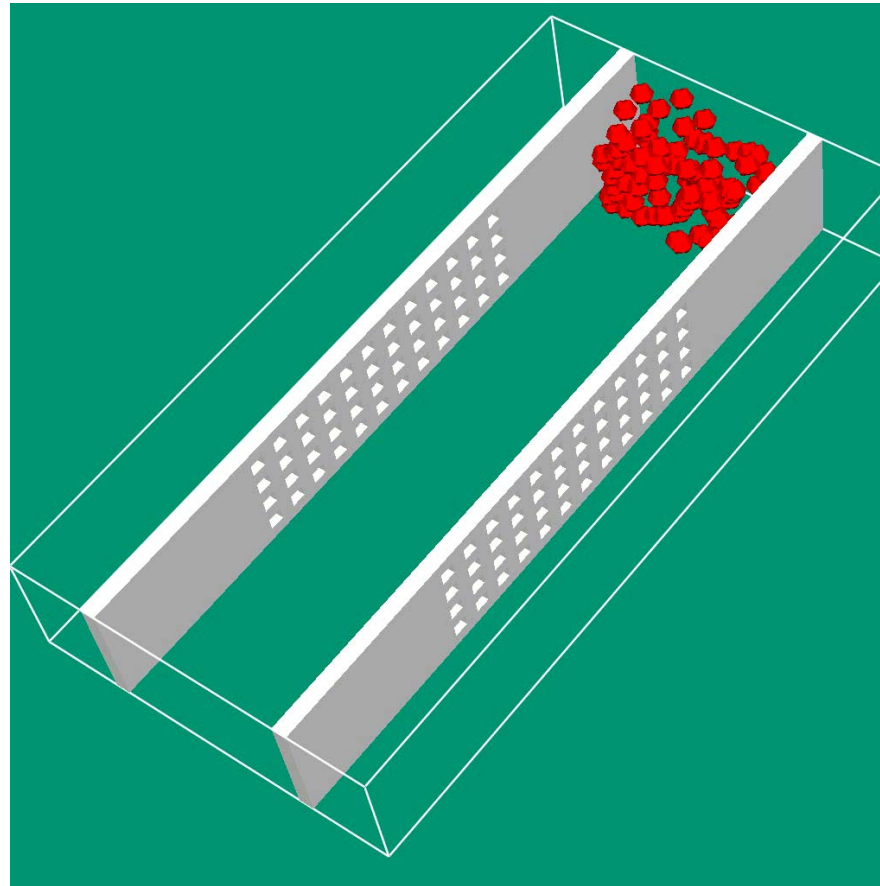
Courtesy M. Knefel, Gebr. Kufferath AG.

Measured vs Simulated pressure drop for GKD meshes



Courtesy M. Knefel & E. Wegenke, Gebr. Kufferath AG.

Cross Flow Filtration



General Pleat Options

Pleat Options [?] [X]

GEO DICT

mm ▼

General | Pleat Shape

General

Inflow Region: 1 mm

Outflow Region: 1 mm

Number of Layers of the Medium: 1

Medium Layout

1 Layer Material: 0001 0.38 mm

2 Layer Material: 0001 0.2 mm

3 Layer Material: 0101 0.1 mm

4 Layer Material: 0000 0 mm

5 Layer Material: 0000 0 mm

Medium Thickness: 0.38 mm

Discretization

Voxel Length: 0.08 mm

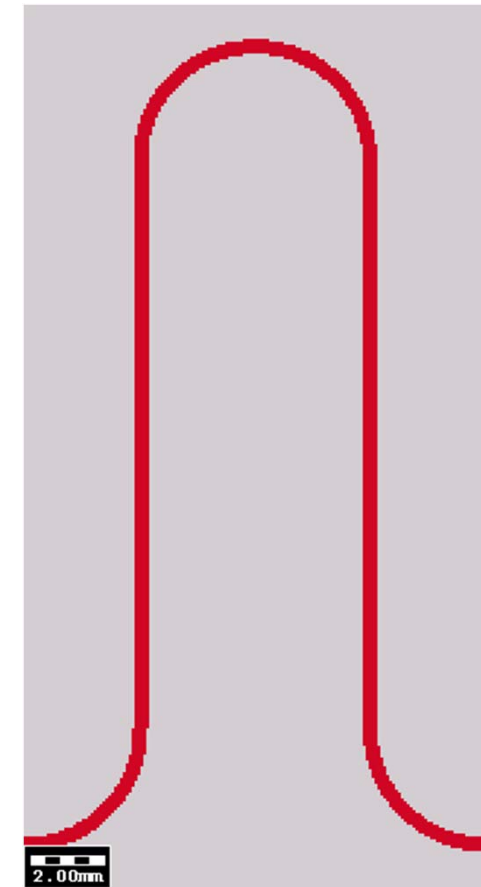
NX: 158 12.64 mm

NY: 1 0.08 mm

NZ: 306 24.48 mm

[Save] [Open] [Red Arrow] [Black Arrow] [Down Arrow]

OK Cancel

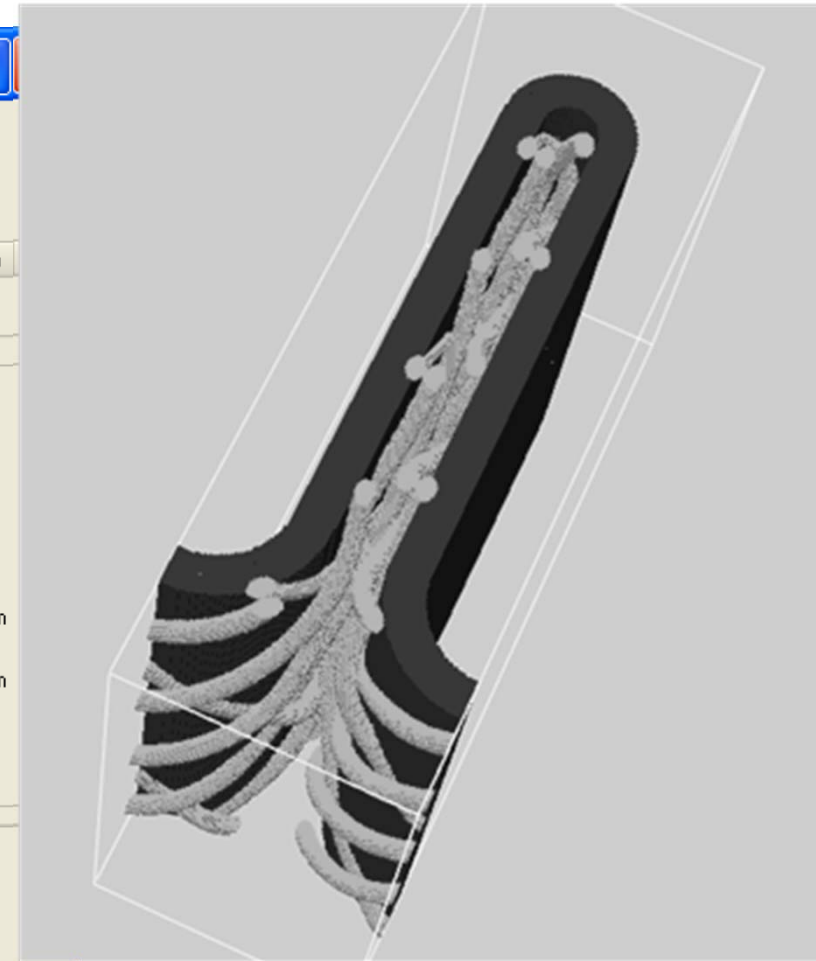
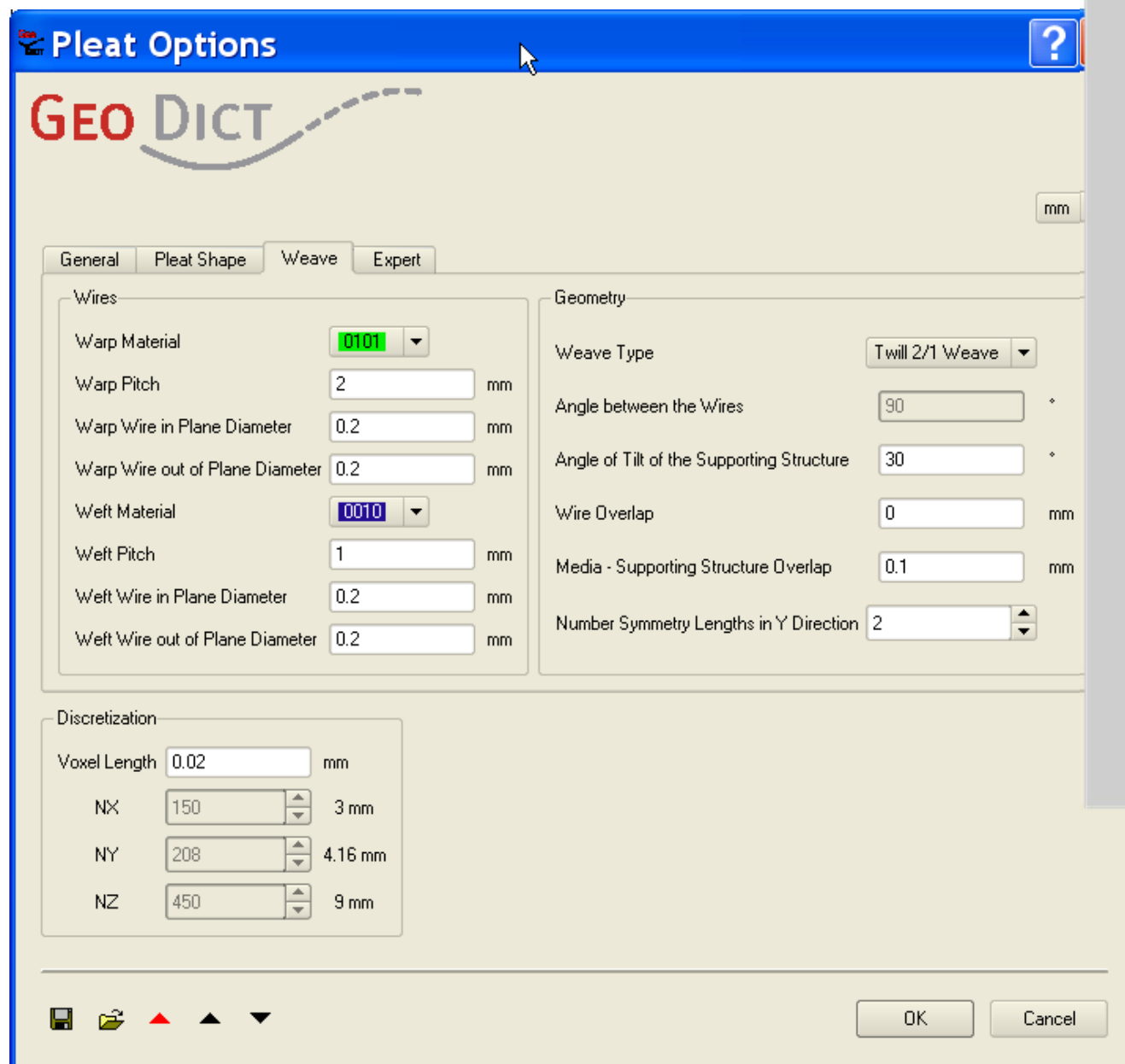


Andreas Wiegmann

Filtech, Wiesbaden

13 October 2009

Weave Pleat Options



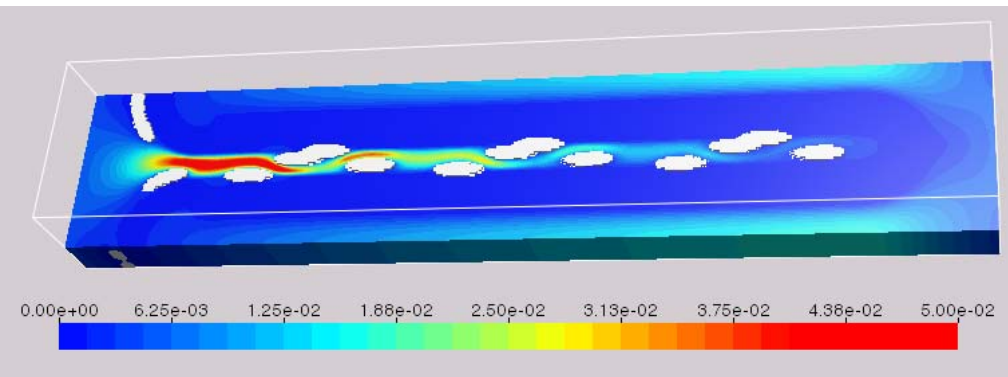
Andreas Wiegmann

Filtech, Wiesbaden

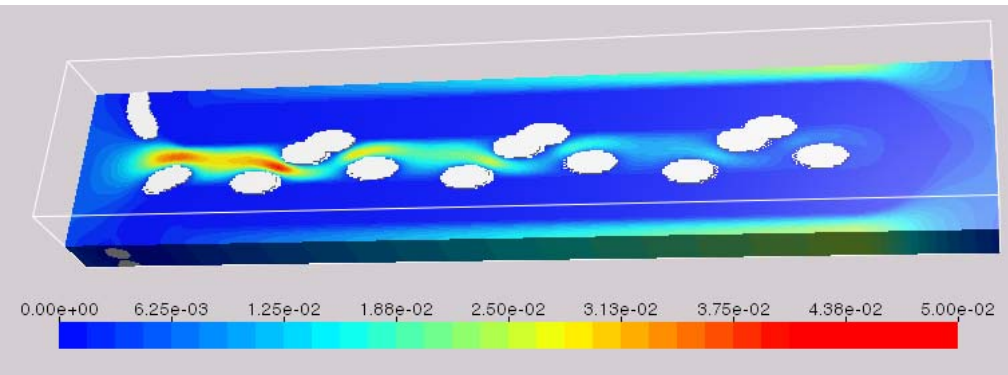
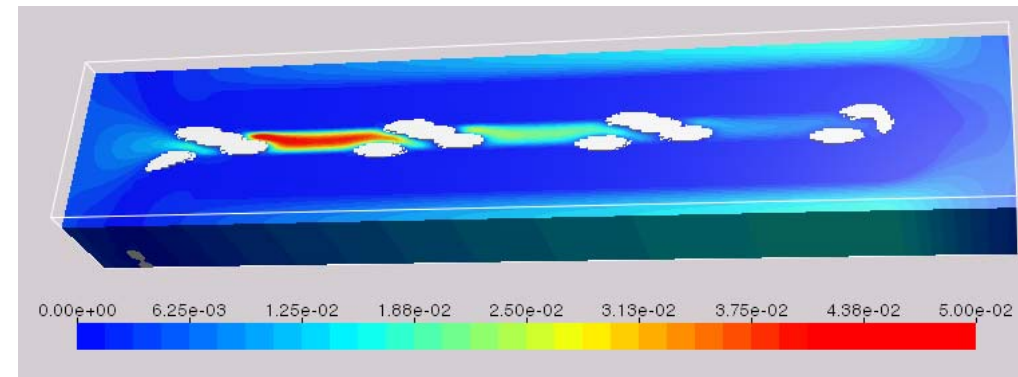
13 October 2009

Oil flow in pleats with support structure: velocity

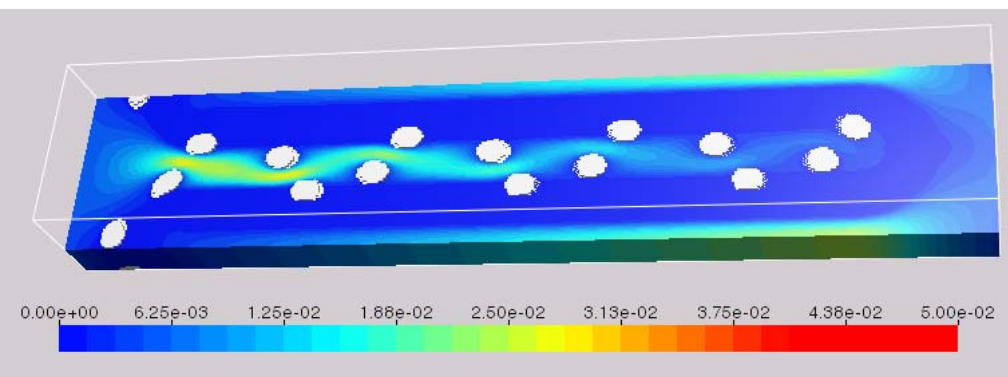
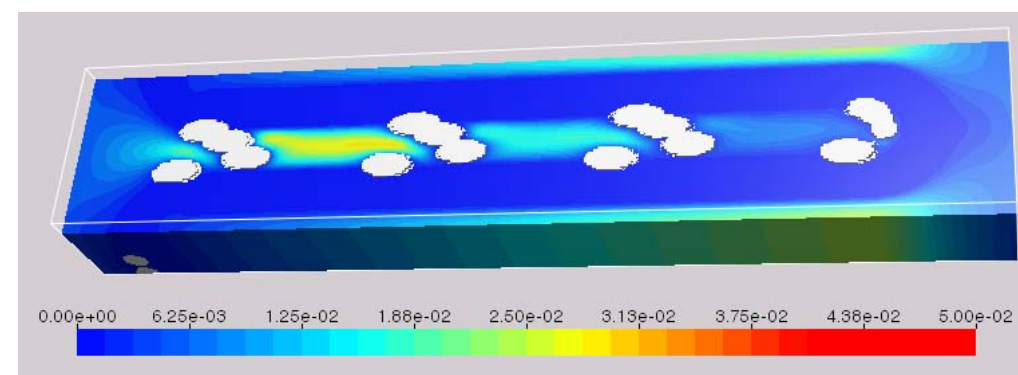
- Velocity: 0.15 m/s
- Oil: density 850 kg/m³
viscosity 0.17 m²/s
- Same pleat count
- Different in- and outflow
channel widths
- Grid resolution 40 μm
- 50 x 70 x 380 cells



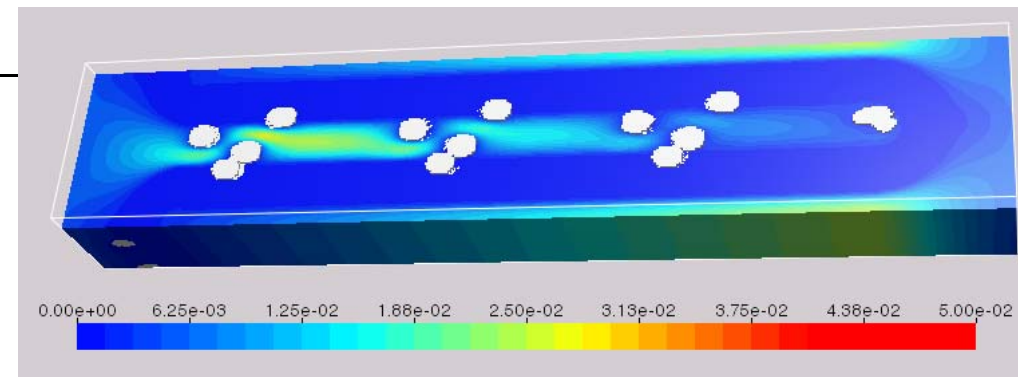
Narrow
Channel



Thick
Wire

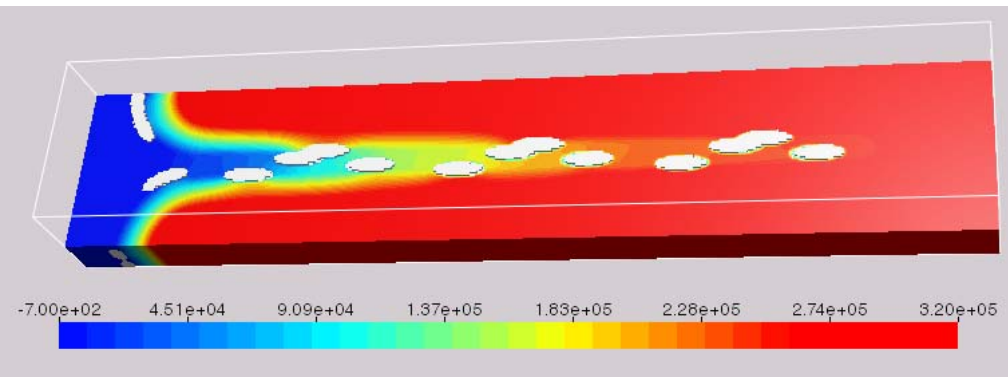


Thin
Wire

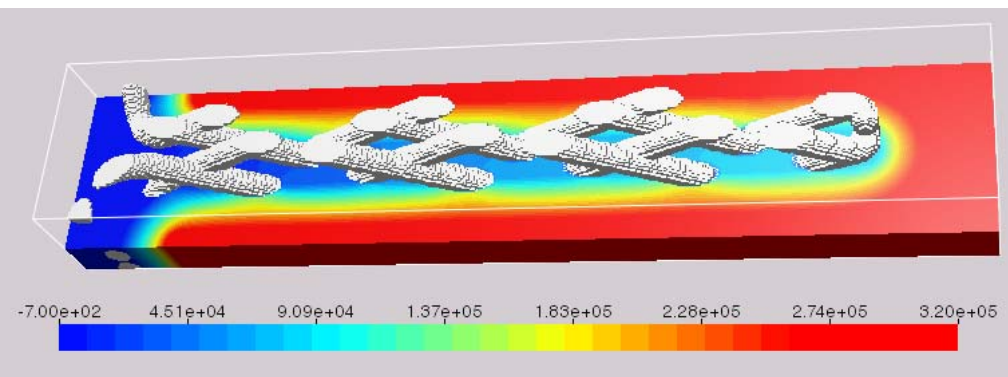
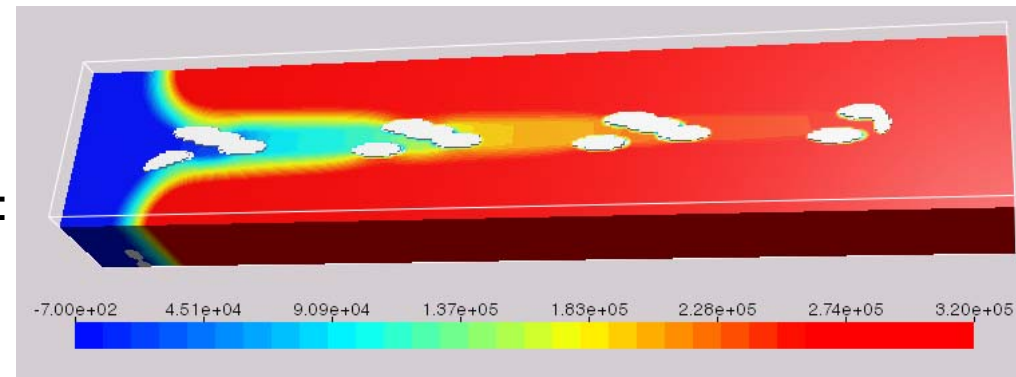


Oil flow in pleats with support structure: pressure

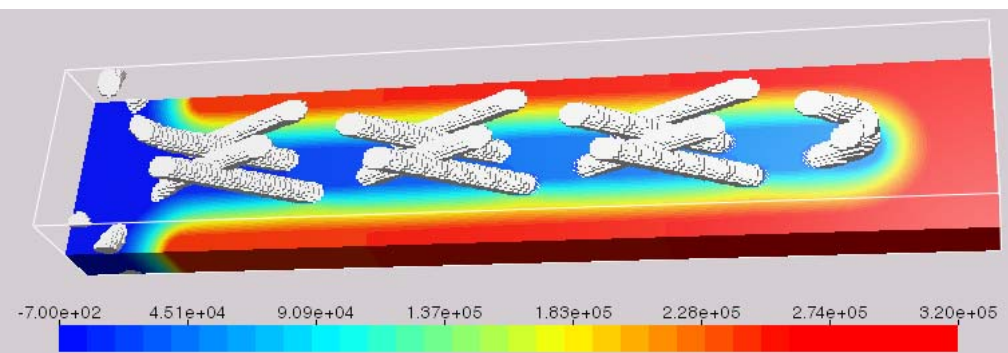
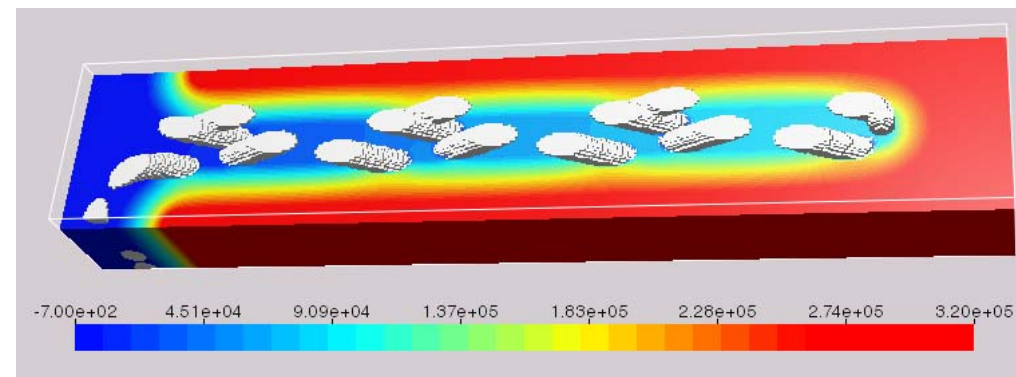
- Pressure in Pascal
- Oil: density 850 kg/m³
viscosity 0.17 m²/s
- Same pleat count
- Different in- and outflow
channel widths
- Grid resolution 40 μm
- 50 x 70 x 380 cells



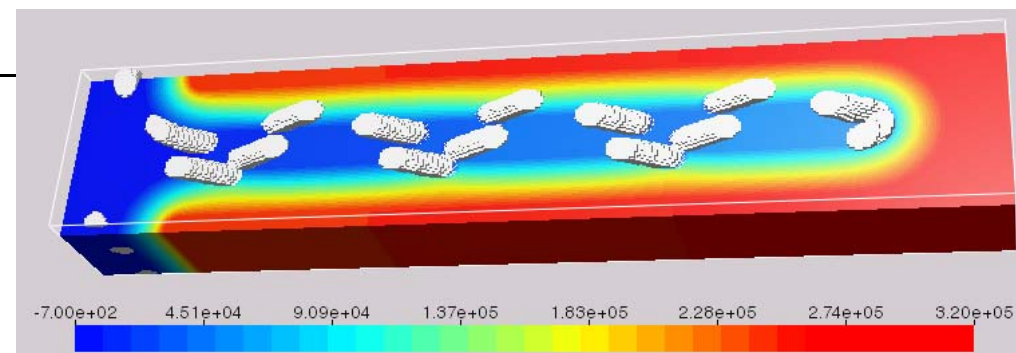
Narrow
Channel:
4 bar



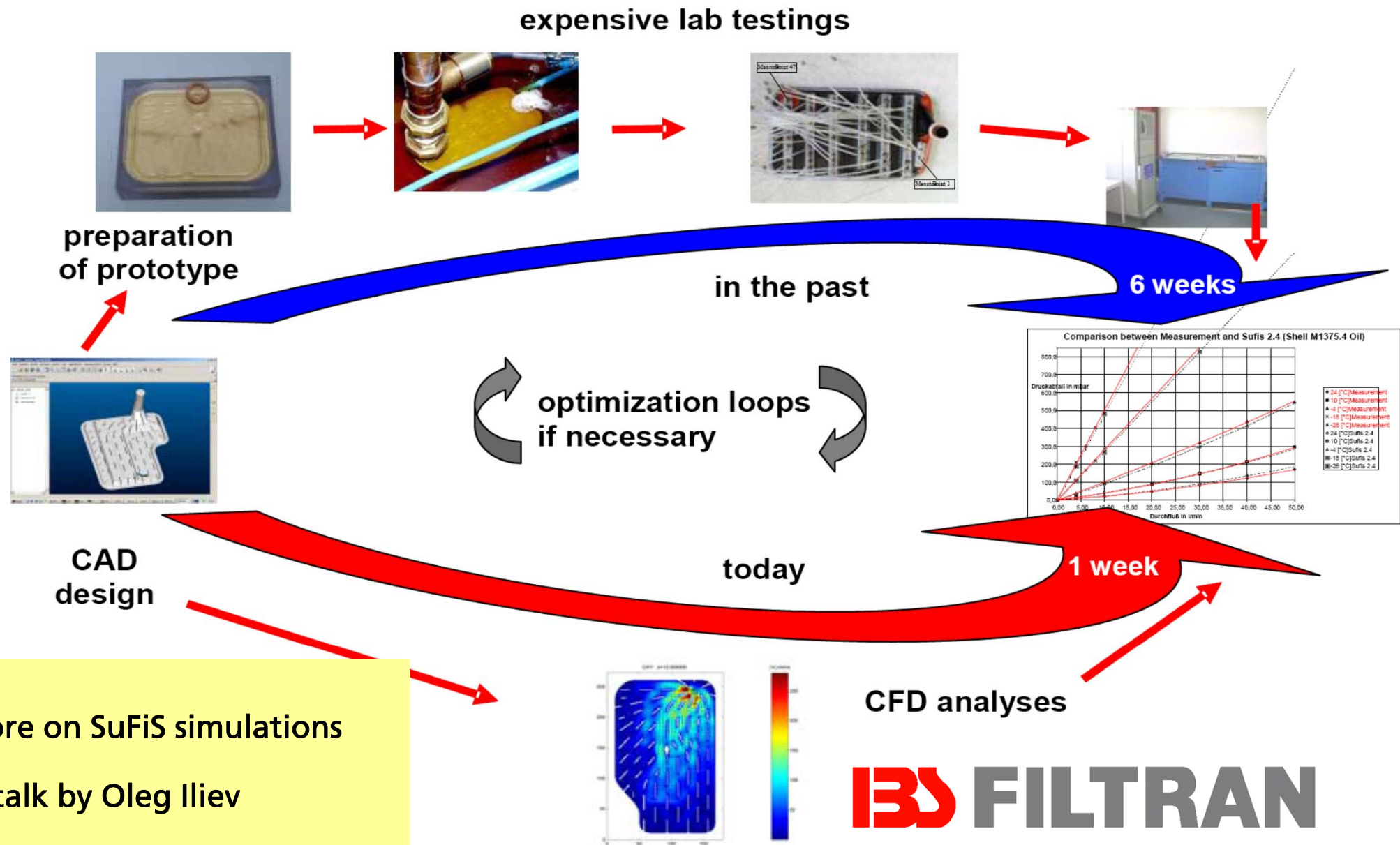
Thick
Wire:
3.1 bar



Thin
Wire:
2.7 bar



Benefits of **SUF**S simulations



More on SuFiS simulations
in talk by Oleg Iliev
L15, Thursday at 11:25am

IBS FILTRAN

Selected project partners and customers



Modules of the GeoDict Software for GAD and GAE of Materials

- **FiberGeo**, **SinterGeo**, **WeaveGeo**, **GridGeo**, **PackGeo**, **PleatGeo**, **PaperGeo**

(structure generators)

- **ProcessGeo** (3d image processing)

- **LayerGeo** (layered media)

- **ImportGeo** (e.g. tomographie, .stl)

- **ExportGeo** (e.g. Fluent, Abaqus)

- **FlowDict** (single phase flow properties)

- **PleatDict** (porous media flow)

- **ElastoDict** (effective elastic properties)

- **ThermoDict** (effective conductivity)

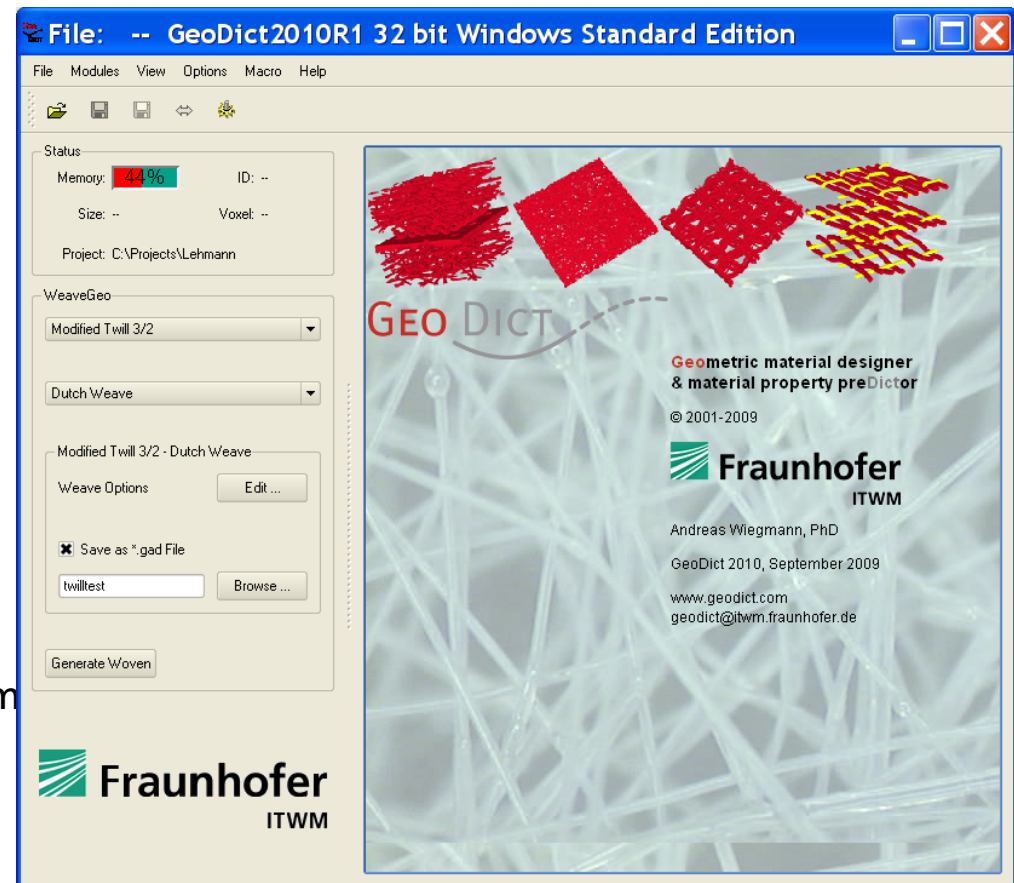
- **DiffuDict** (effective diffusivity)

- **FilterDict** (pressure drop, efficiency, life time)

- **SatuDict** (two phase flow properties)

- **PoroDict** (pore size measures)

- **AcoustoDict** (acoustic absorption)



GeoDict contributors: 2001 - 2009

GeoDict

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Conclusions

Challenges

- Measurements
- deposition location
- electric charges
- Requirements: cost, material, space, energy
- Computing power
- Geometric resolution
- Geometry uncertain
- Analytic expressions to be derived

Progress

- 3d media and element models
- Navier-Stokes-Brinkman for gas and liquid
- Fast & low memory solvers
- Prediction of pressure drop for $Re < 100$
- Low concentration particle transport
- Prediction of filter efficiency
- Cake and porous media build-up
- Prediction of clogging and life time
- **Filtration and separation simulation spread in Academic and Industrial R&D**

Exhibit and talks at Filtech 2009 also by Fraunhofer ITWM

Visit us at Booth I A 12

Simulation of **pleat deflection** in talk by Matthias Kabel,

G1, Tuesday 1:40pm

More on **ceramics and soot simulations** in poster by Kilian Schmidt,

G4, Wednesday at 8:30am

More on **woven simulations** in talk by Erik Glatt,

6, Wednesday at 11:50am

Coupled particle and filter element level in talk by Zarah Lakdawala,

L10 Wednesday at 5:30pm

More on **SuFiS simulations** in talk by Oleg Iliev,

L15, Thursday at 11:25pm

More on **nano filtration media** in talk by Liping Cheng,

G15, Thursday at 3:00pm

Thank you for your attention
