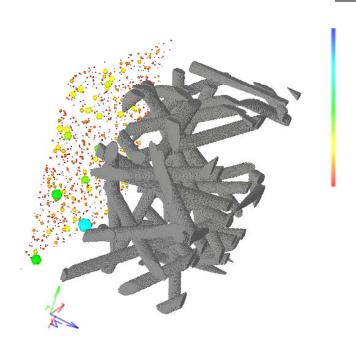
Progress & Challenges predicting Filtration and Separation



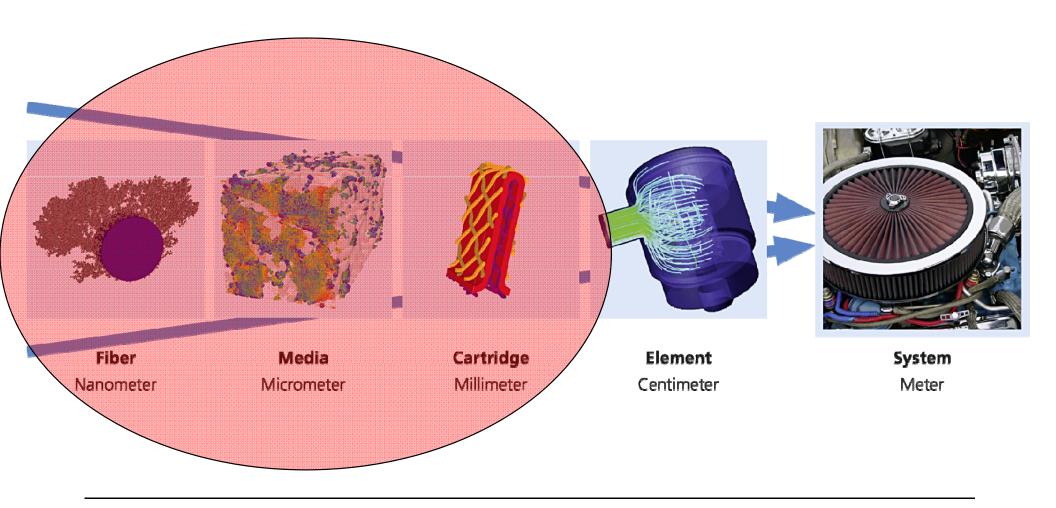
Andreas Wiegmann



Fraunhofer Institute forIndustrial Mathematics,Kaiserslautern

Louisville, KY, USA 10th May, 2011

Filtration and simulation occur on multiple scales



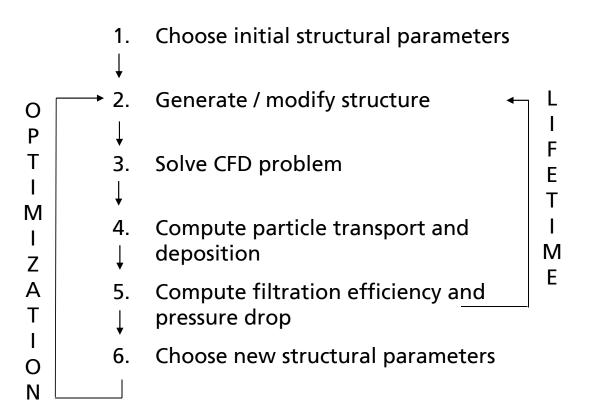




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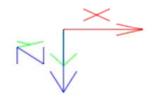
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Virtual design cycle of filter media

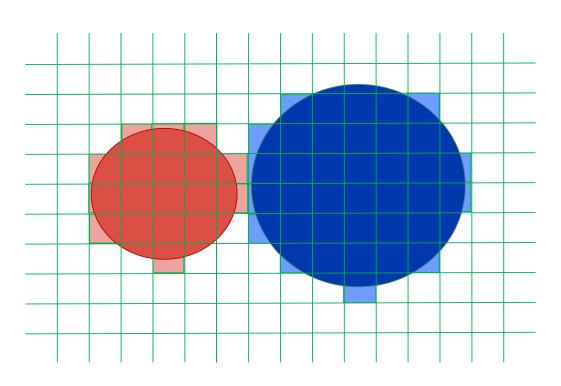








Our simulations are all based on structures of little cubes



Advantages

- Saves grid generation times
- Compatible with computer tomography
- Straight forward structure generation
- Straight forward solver implementation
- Straight forward parallel computations

Disadvantages

- Resolved features require many grid cells
- Leads to very large scale computations





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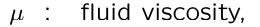
Description of fluid motion: Stationary Stokes flow w/wo slip

$$-\mu \Delta \vec{u} + \nabla \vec{u} \cdot \vec{u} + \nabla p = 0 \text{ (momentum balance)}$$

$$\nabla \cdot \vec{u} = 0 \text{ (mass conservation)}$$

$$\vec{u} = 0 \text{ on } \Gamma \text{ (no-slip on fiber surfaces)}$$

$$P_{in} = P_{out} + c \text{ (pressure drop is given)}$$



 $ec{u}$: velocity, periodic,

p: pressure, periodic up to pressure drop in flow direction.

$$-\mu\Delta\vec{u}+\nabla p=0$$
 (momentum balance)
$$\nabla\cdot\vec{u}=0 \text{ (mass conservation)}$$

$$\vec{n}\cdot\vec{u}=0 \text{ on } \Gamma \text{ (no flow into fibers)}$$

$$\vec{t}\cdot\vec{u}=-\lambda\vec{n}\cdot\nabla\left(\vec{u}\cdot\vec{t}\right) \text{ on } \Gamma \text{ (slip flow along fibers)}$$

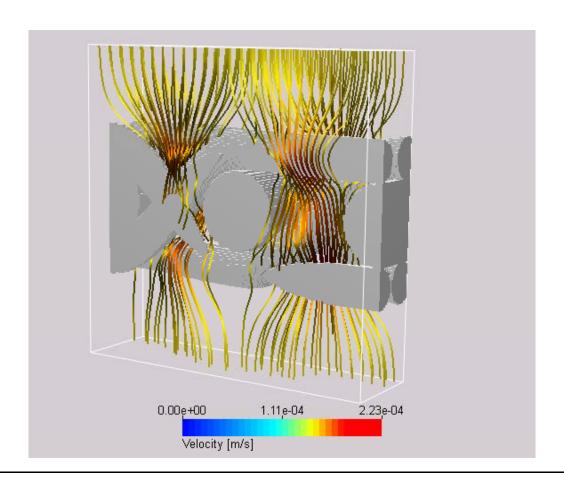
$$P_{in}=P_{out}+c \text{ (pressure drop is given)}$$

 \vec{n} : normal direction to the fiber surface,

 λ : slip length,

 \vec{t} : any tangential direction with $\vec{t} \cdot \vec{n} = 0$.

Flow Field Visualization

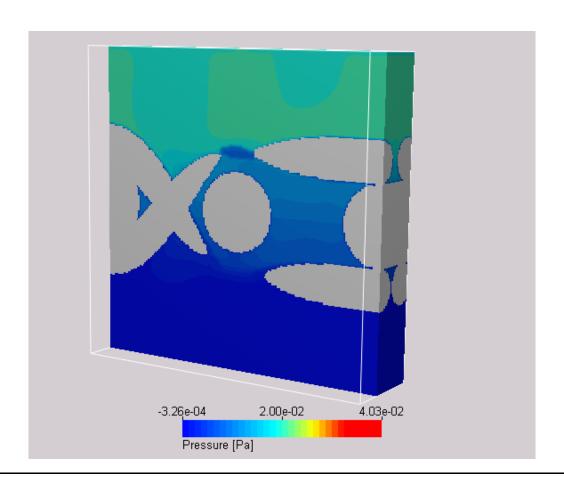






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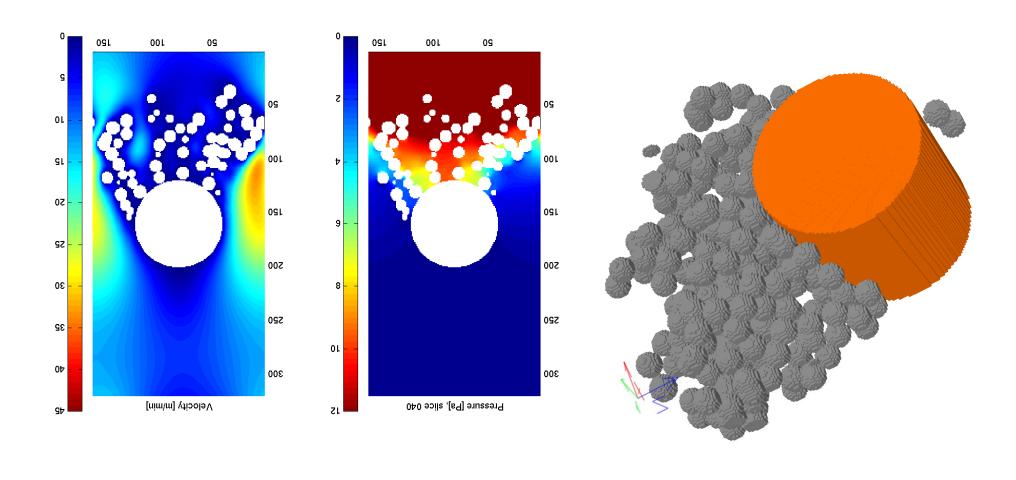
Pressure Drop Visualization







Pressure and Velocity in Clogging Simulation





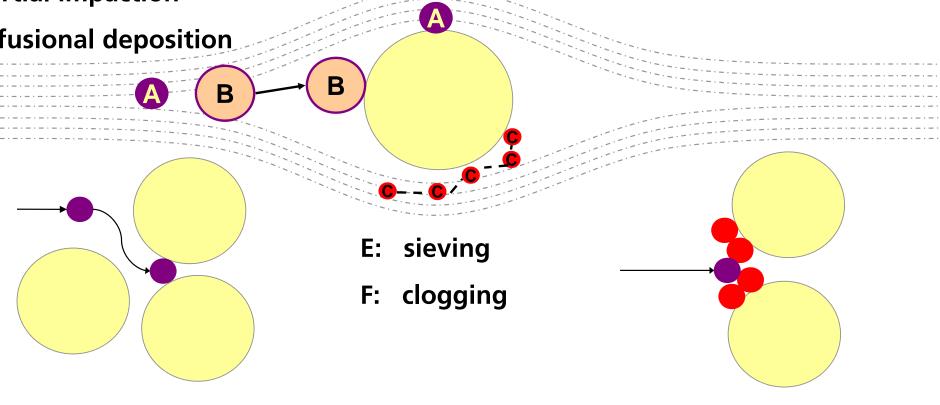


Filtration Effects I

A: direct interception

B: inertial impaction

C: diffusional deposition





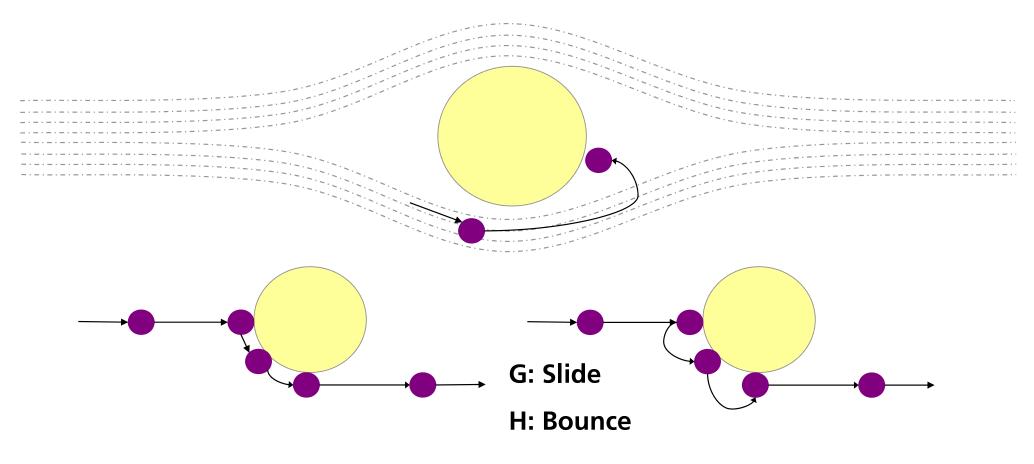


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Filtration Effects II and modes of particle motion

D: electrostatic attraction



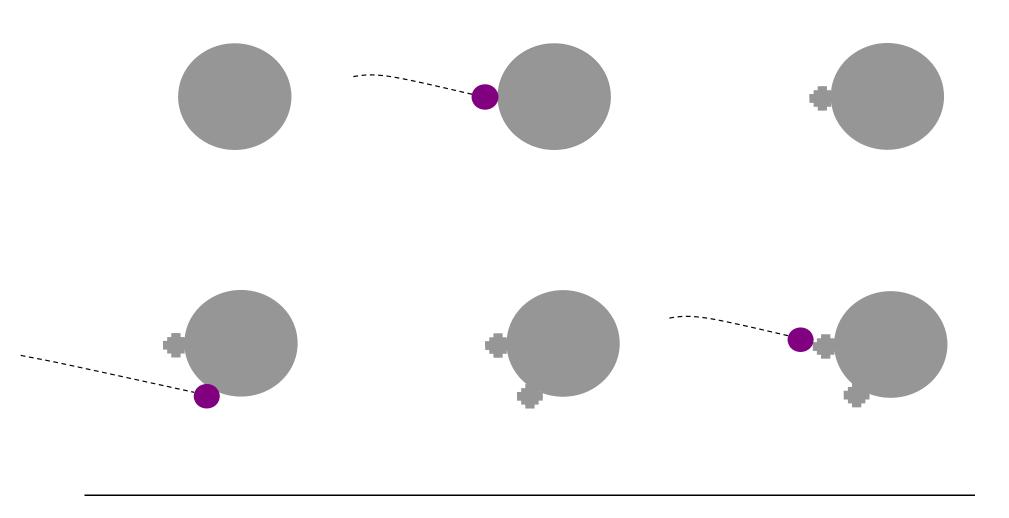




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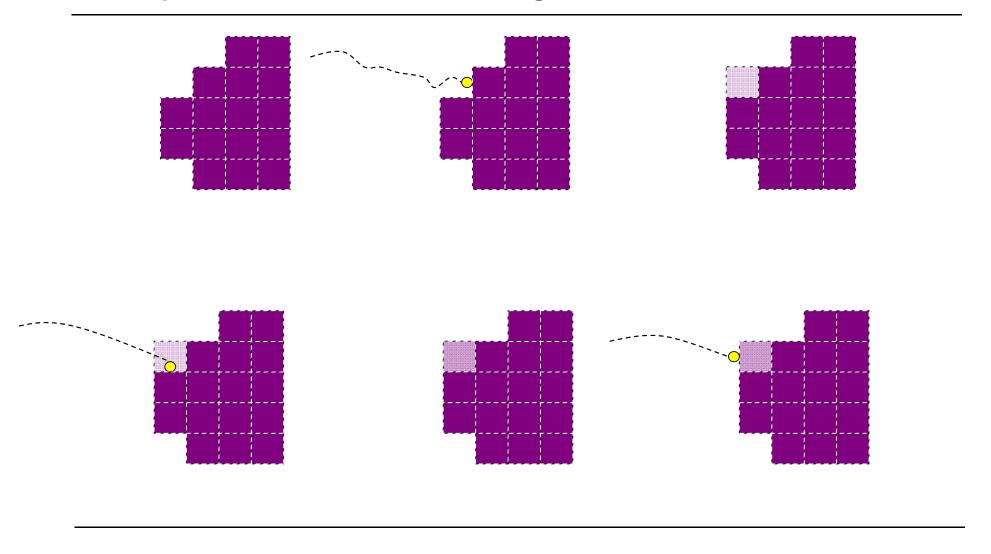
When particles are larger than the grid cells







When particles are smaller than the grid cells







Description of particle motion

$$d\vec{x} = \vec{v} \, dt, \quad \text{Friction with fluid} \qquad \text{Electric attraction Diffusive motion}$$

$$d\vec{v} = -\gamma \times (\vec{v}(\vec{x}) - \vec{v}_{\circ}(\vec{x})) \, dt + \frac{Q\vec{E}_{\circ}(\vec{x})}{m} dt + \sigma \times d\vec{W}(t),$$

$$C_c = 1 + Kn \left(1.142 + 0.558e^{-0.999/Kn} \right),$$

$$\gamma = 6\pi\rho\mu\frac{R}{C_cm}, \qquad \gamma: \quad \text{friction coefficient}$$

$$\delta^2 = \frac{2k_BT\gamma}{m}, \qquad k_B: \quad \text{Boltzmann constant}$$

$$\vec{E}_{\circ}: \quad \text{electric field}$$

$$\vec{W}_{\circ}(t), dW_{\circ}(t) = \delta_{ij}dt, \qquad t: \quad \text{time} \qquad \vec{v}_{\circ}: \quad \text{fluid velocity}$$

$$\vec{K}_{\circ} = \frac{\lambda}{R}, \qquad \vec{v}: \quad \text{particle position} \quad \rho: \quad \text{fluid density}$$

$$K_{\circ} = \frac{\lambda}{R}, \qquad \vec{v}: \quad \text{particle velocity} \quad \mu: \quad \text{fluid viscosity}$$

$$\lambda = \frac{k_BT}{\sqrt{32}\pi R^2 P} \qquad m: \quad \text{particle mass}$$

$$q: \quad \text{particle charge}$$

$$T: \quad \text{ambient temperature}$$

$$P: \quad \text{total pressure}$$

$$d\vec{W}(t): \quad \text{3d probability (Wiener) measure}$$





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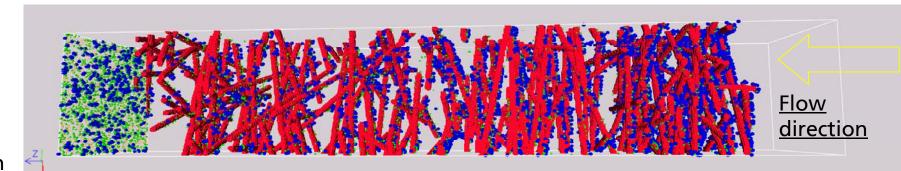
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Deposition effects

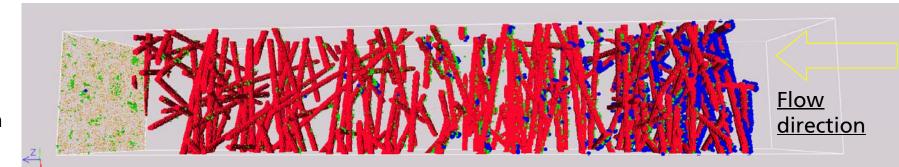
 $\alpha = 0.05$,

 $d_F = 14$,

v = 0.1m/s



Interception

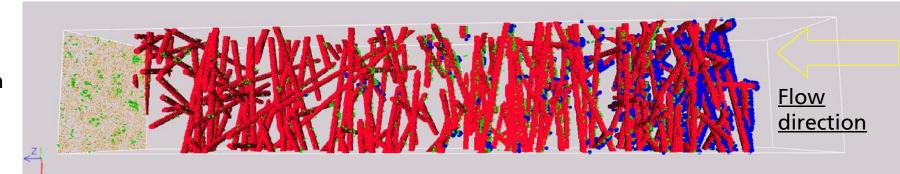


Interception

+ Impaction

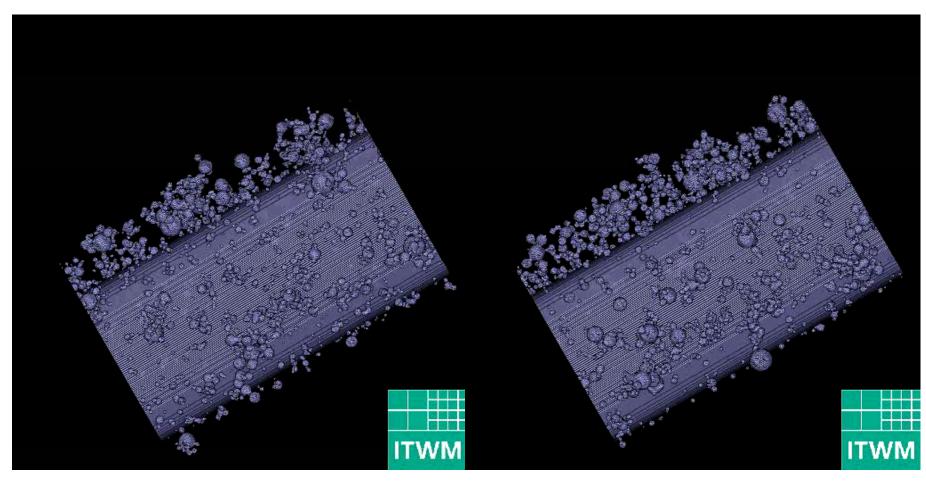
Interception

- + Impaction
- + Diffusion



Nano Simulations

1.67cm/sec 10.0cm/sec







Nano Simulations

 Deposition patterns and porosity depend on far field velocity, particle size distribution, etc.

Result:

- Find minimal porosity and permeability of the soot layers, s_{max} and κ_{min}
- Derivation by layers from single fiber highly resolved simulations

Soot Layer Cut-Out





Stationary Flow with unresolved particles: Stokes-Brinkmann eqs

$$-\mu\Delta\vec{u} + \nabla\vec{u} \cdot \vec{u} + \nabla p + \kappa^{-1}\vec{u} = \vec{\mathbf{f}} \text{ (momentum balance)}$$

$$\nabla \cdot \vec{u} = 0 \text{ (mass conservation)}$$

$$\vec{u} = 0 \text{ on } \Gamma \text{ (no-slip on fiber surfaces)}$$

 $\vec{\mathbf{f}} = (0, 0, f)$: force in flow(z)-direction,

 $\kappa = \kappa_{min} \max\{1, s_{max}/s\}$: porous voxel permeability,

s: solid volume fraction in a voxel

 \vec{u} : velocity,

 μ : fluid viscosity,

p: pressure and

 Γ : fiber or deposited particle surfaces.

Solid volume fraction in voxel is increased until s_{max} is reached. Voxel becomes "collision-solid". Neighbor voxels svf starts increasing upon particle arrival

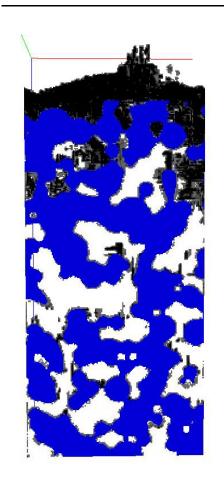


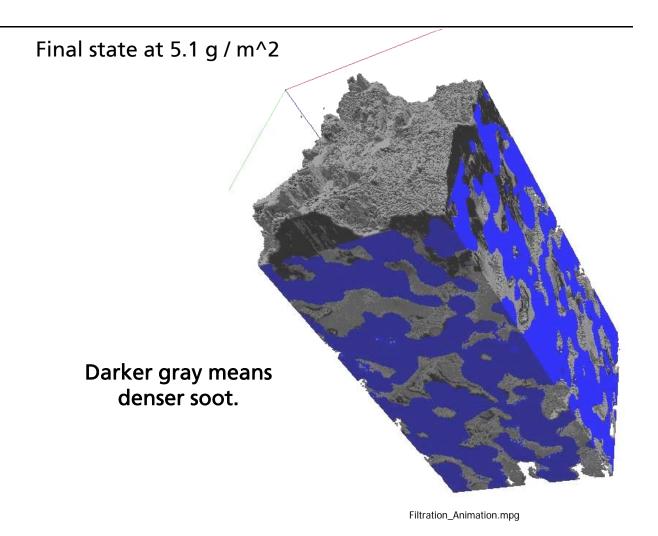


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Micro Simulations

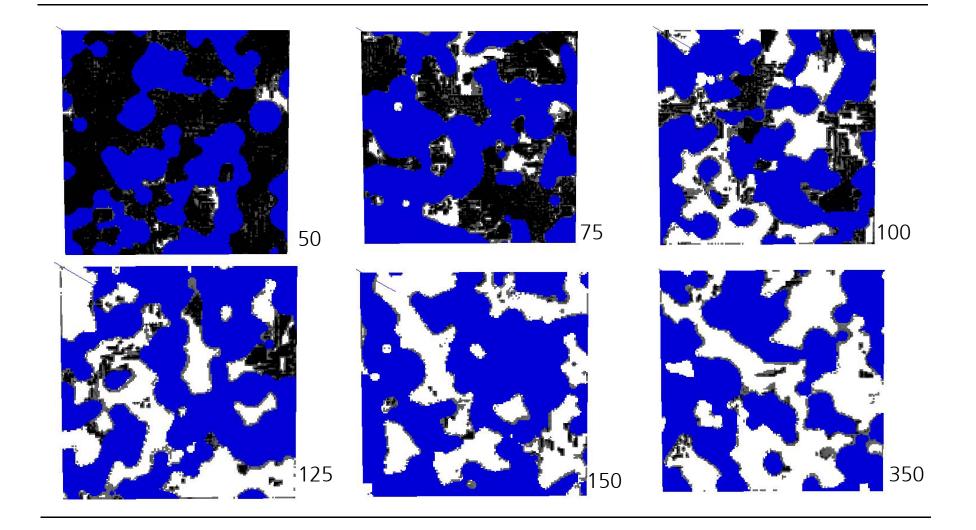








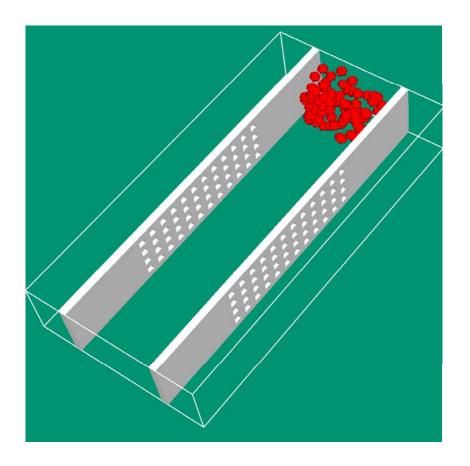
Horizonal layers







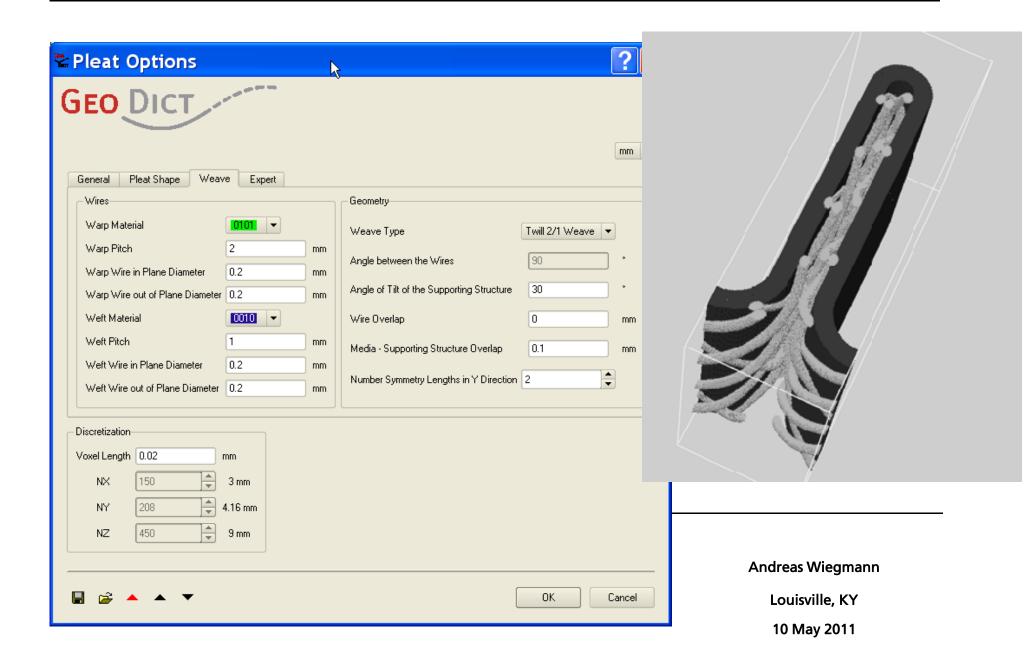
Cross Flow Filtration





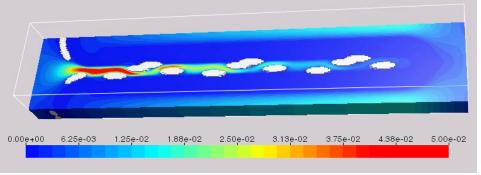


Weave Pleat Options

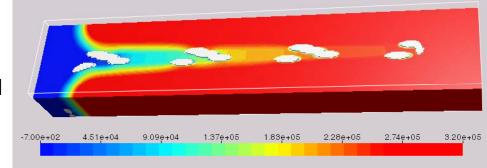


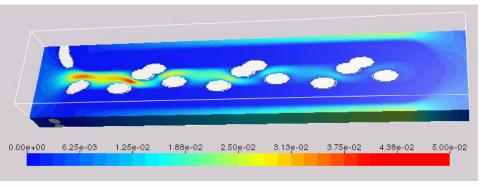
Oil flow in pleats with support structure: velocity & pressure

- Velocity: 0.15 m/s
- Oil: density 850 kg/m³ viscosity 0.17 m²/s
- Same pleat count
- Different in- and outflow channel widths
- Grid resolution 40 μm
- 50 x 70 x 380 cells

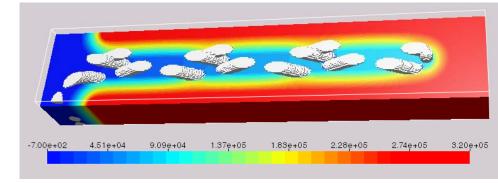


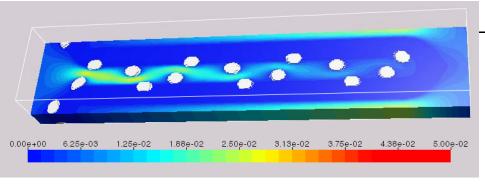
Narrow Channel



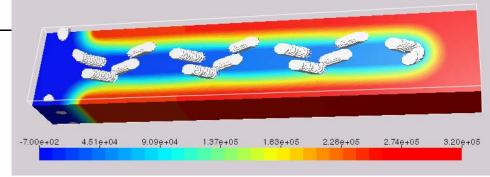


Thick Wire





Thin Wire



Conclusions

Challenges

- Measurements
- deposition location
- electric charges
- Requirements: cost, material, space, energy
- Computing power
- Geometric resolution
- Geometry uncertain
- Analytic expressions to be derived

Progress

- 3d media and element models
- Navier-Stokes-Brinkman for gas and liquid
- Fast & low memory solvers
- Prediction of pressure drop for Re < 100
- Low concentration particle transport
- Predicition of filter efficiency
- Cake and porous media build-up
- Prediction of clogging and life time
- Filtration and separation simulation spread in Academic and Industrial R&D





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Outlook

Current "Hot" Simulation Topics:

- Multipass time step control (see my talk tomorrow)
- Re-entrainment of particles, pulse cleaning
- Coalescence
- Filtration in pleats and DPF honeycomb structures
- Nanofibers
- Electric charges
- Two phase flows in filters, rocks, diapers and fuel cells



