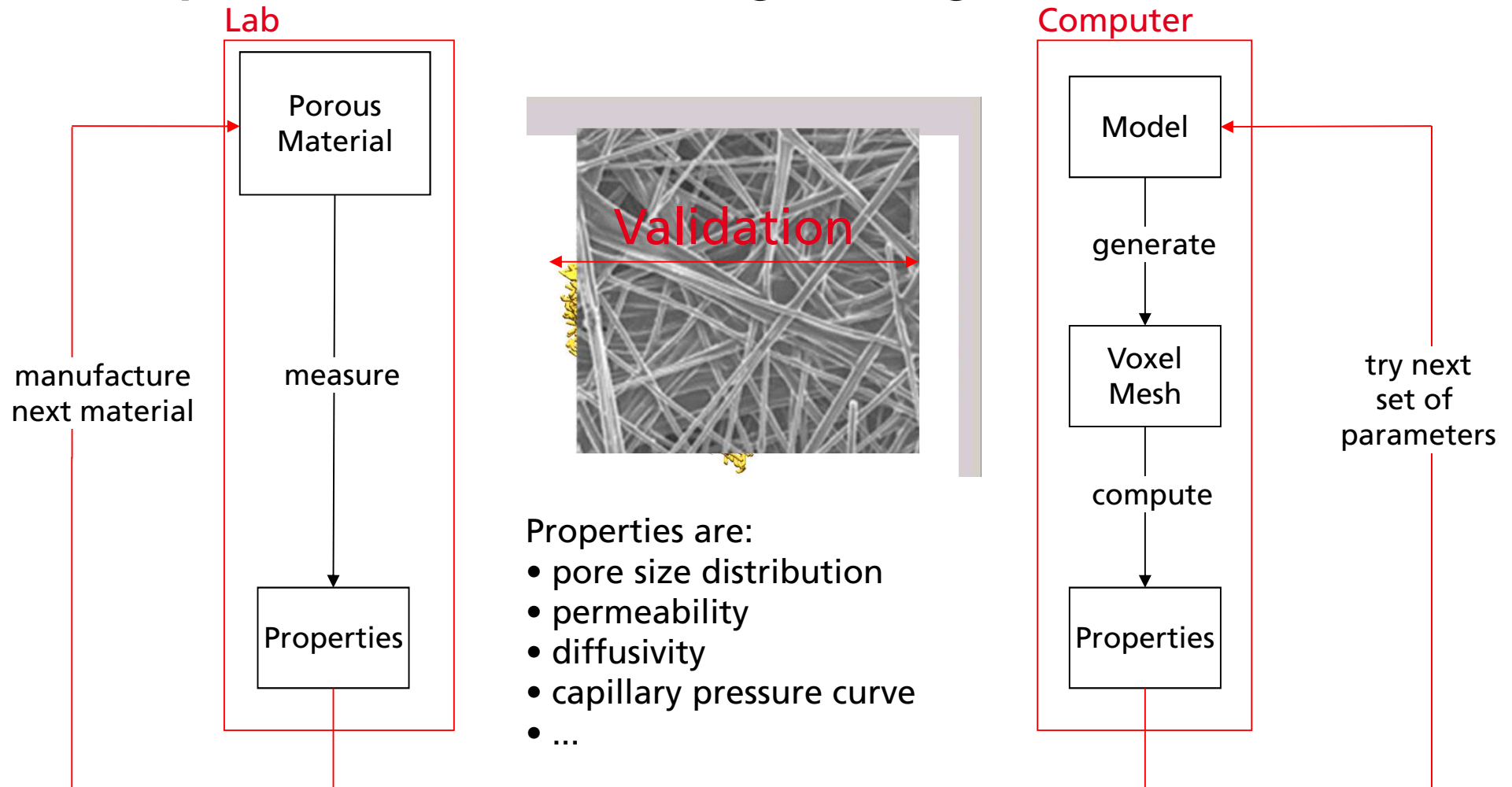

Computer Based Design Study of Porous Transport Layers of PEFC

ModVal 2012, Sursee

Jürgen Becker
Nada Zamel
Andreas Wiegmann

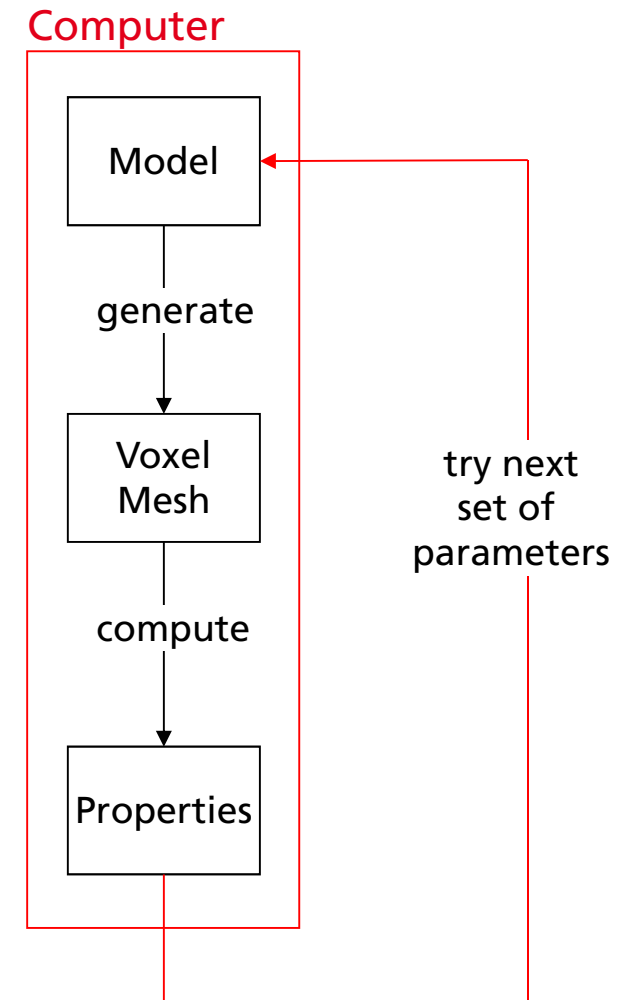
Fraunhofer ITWM, Kaiserslautern

The General Approach: Computer Aided Material Engineering



Overview

1. 3D structure model
2. Property computations
3. Parameter study
 - GDL
 - MPL



3D Models: Gas Diffusion Layer (GDL)

Nonwoven fibres

Input:

- Porosity
- Fibre diameter and type
- Anisotropy

Algorithm:

- Poisson line process
- Production process not modeled



3D Models: Gas Diffusion Layer (GDL)

Nonwoven fibres (entangled)

Input:

- Porosity
- Fibre diameter and type
- Anisotropy
- Fibre crimp

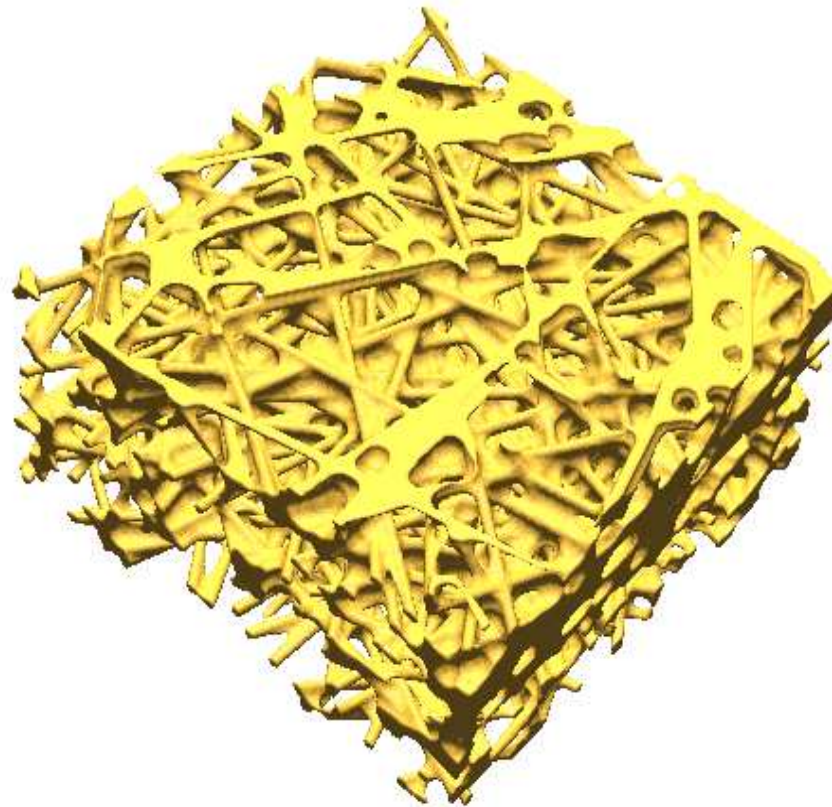


3D Models: Gas Diffusion Layer (GDL)

Nonwoven fibres plus binder

Input:

- Porosity
- Fibre diameter and type
- Anisotropy
- Weight% binder



Permeability

Macroscopic description (homogenized porous media model)

$$\text{Darcy's law : } u = -\frac{1}{\mu} \kappa \nabla p$$

u : average flow velocity

κ : permeability tensor **unknown**

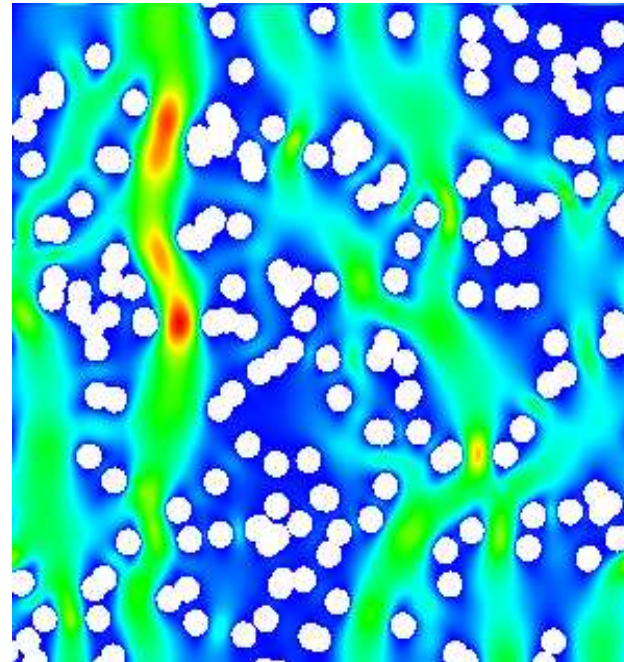
μ : viscosity

p : pressure

Microscopic description (pore structure model)

$$\text{Stokes equation: } -\mu \Delta u + \nabla p = 0$$

Boundary conditions: no-slip on fibre surface, pressure drop
 κ can be determined from the solution!



Diffusivity

Macroscopic description (homogenized porous media model)

Fick's first law: $j = -D^* \nabla c$

D^* : effective diffusivity [m^2/s] *unknown*

j : diffusion flux [$\text{mol}/\text{m}^2/\text{s}$]

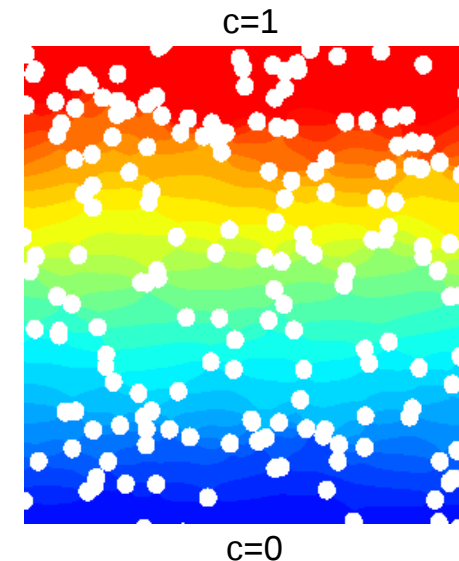
c : concentration [mol/m^3]

Microscopic description (pore structure model)

Laplace equation: $-\Delta c = 0$

Boundary conditions: no-flux on fibre surface,
concentration drop

D^* can be determined from the solution!

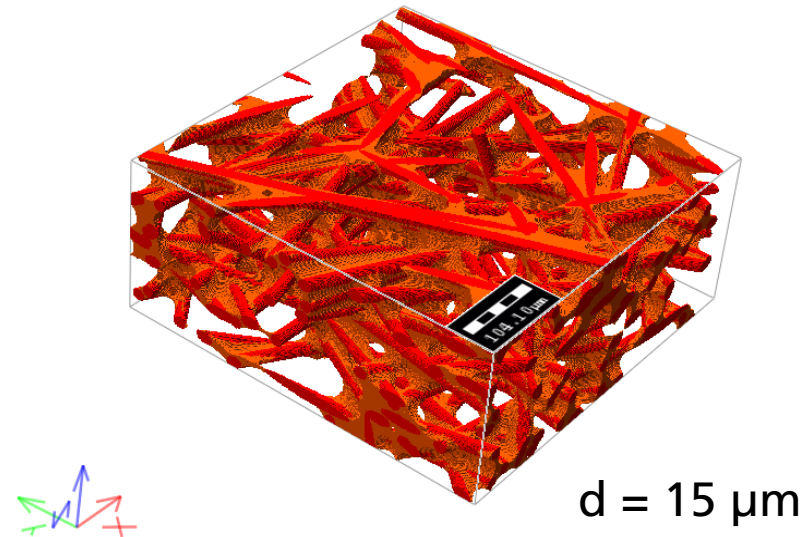
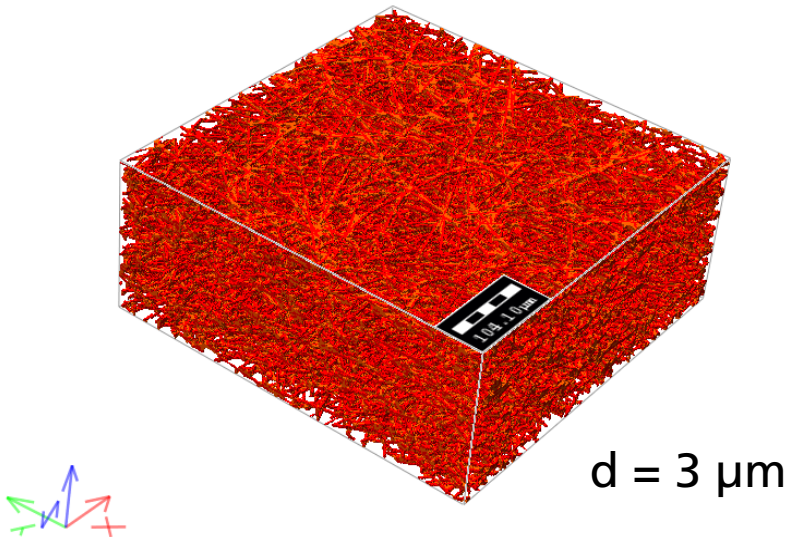


GDL Design Study

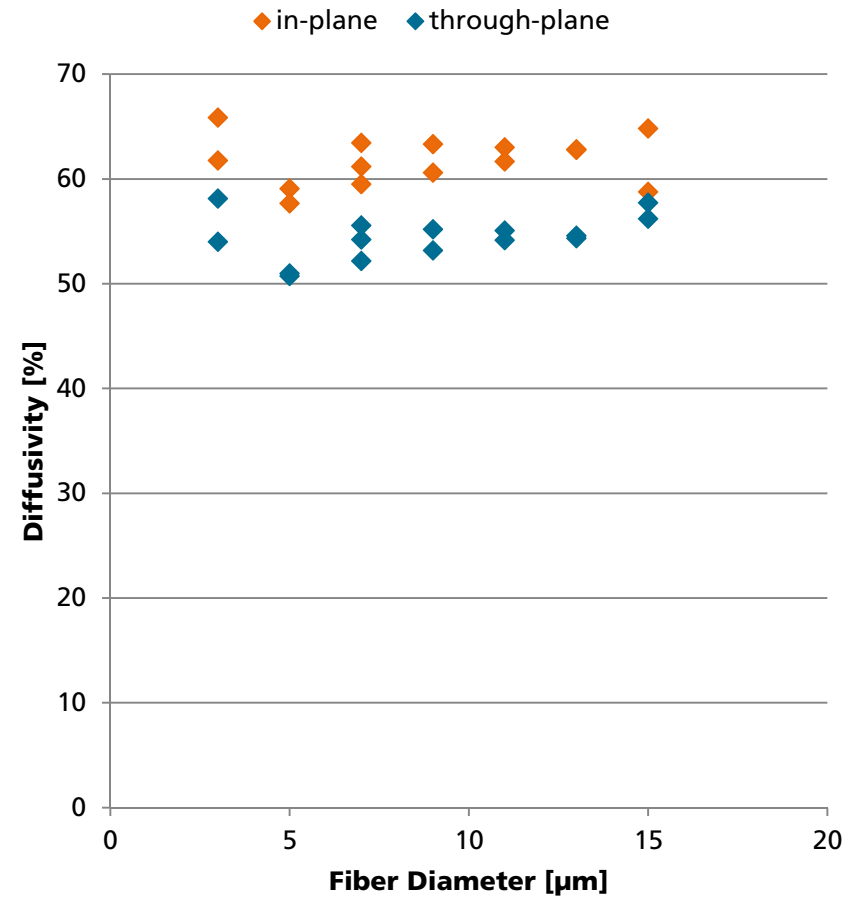
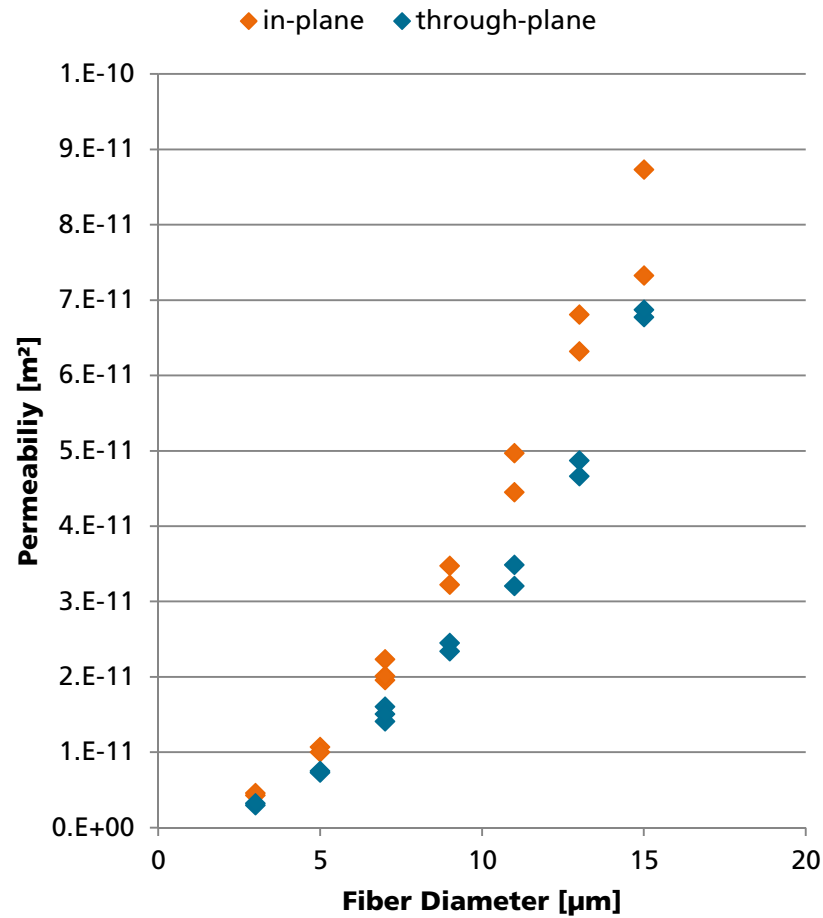
1. Create 3D structure with X vol% fibers with diameter X μm
2. Add binder until X wt% is reached
3. Determine in-plane and through-plane diffusivity and permeability

Fiber Diameter

- 12 vol% fibers
- binder content 40 wt% (leads to porosity 80%)

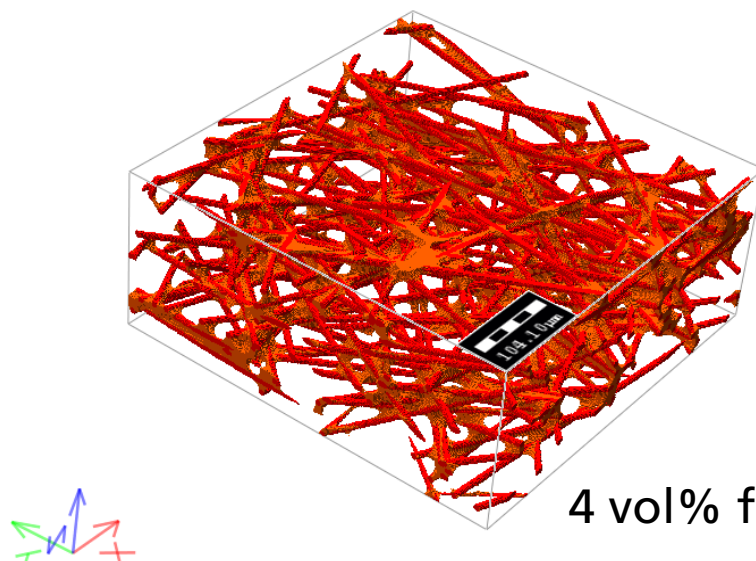


Fiber Diameter

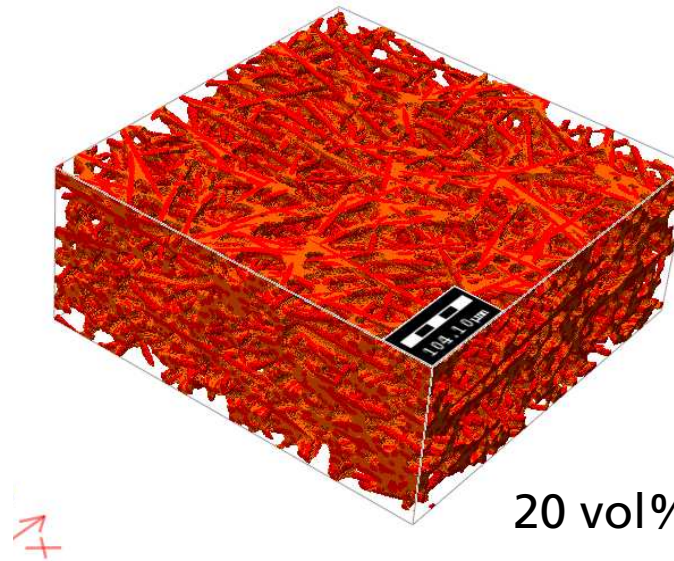


Porosity

- 7 μm fiber diameter
- 40 wt% binder content

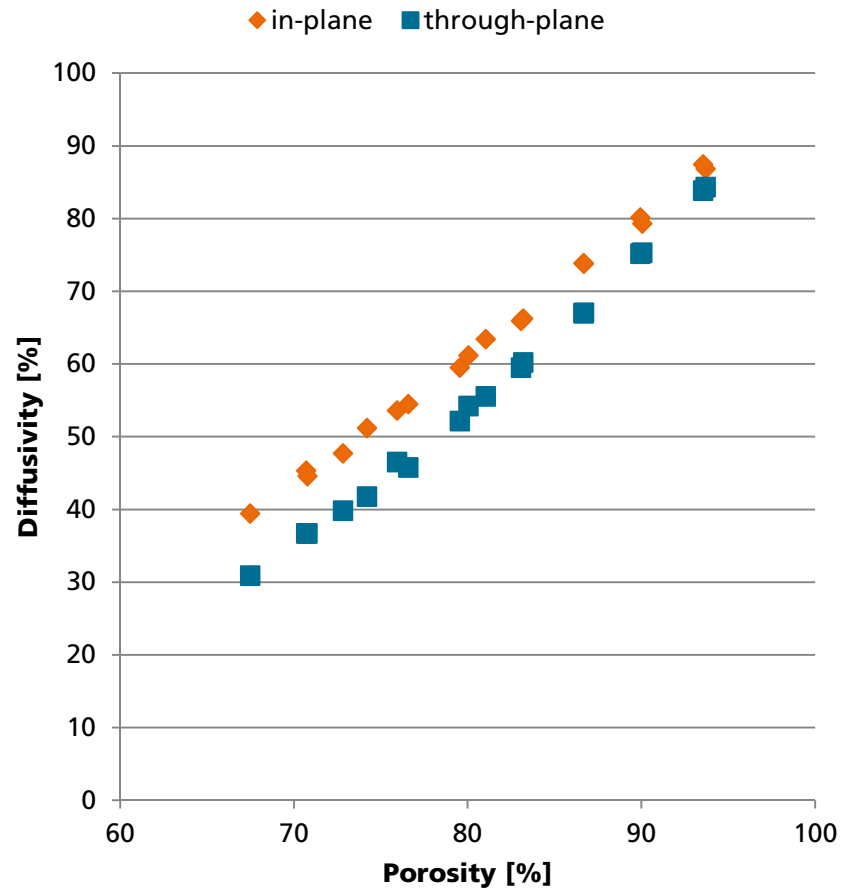
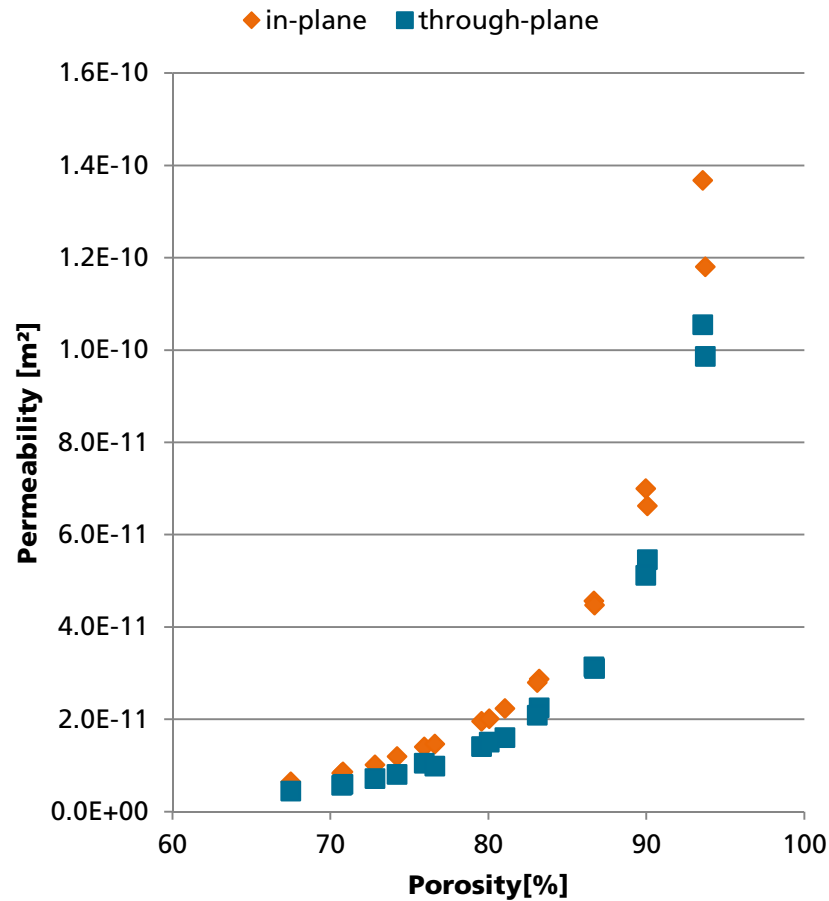


4 vol% fibers



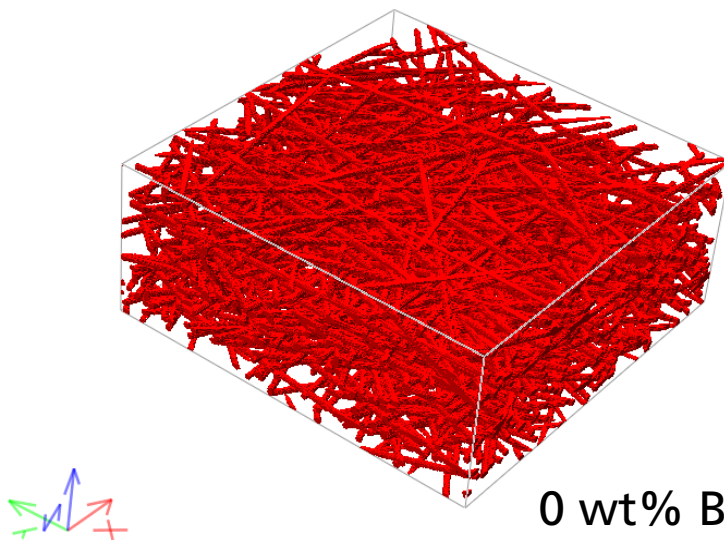
20 vol% fibers

Porosity

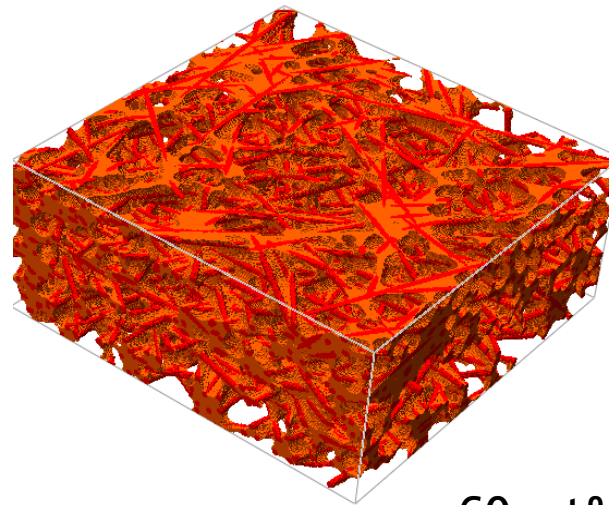


Binder content

- 7 μm fiber diameter
- 12 vol% fibers

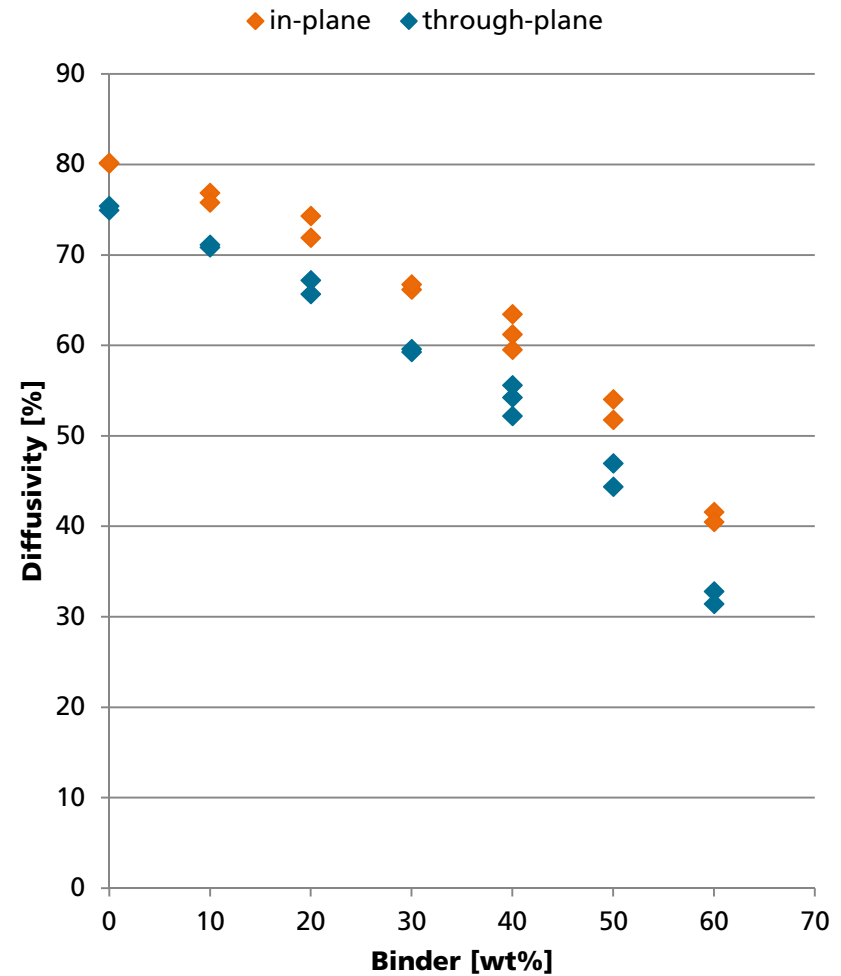
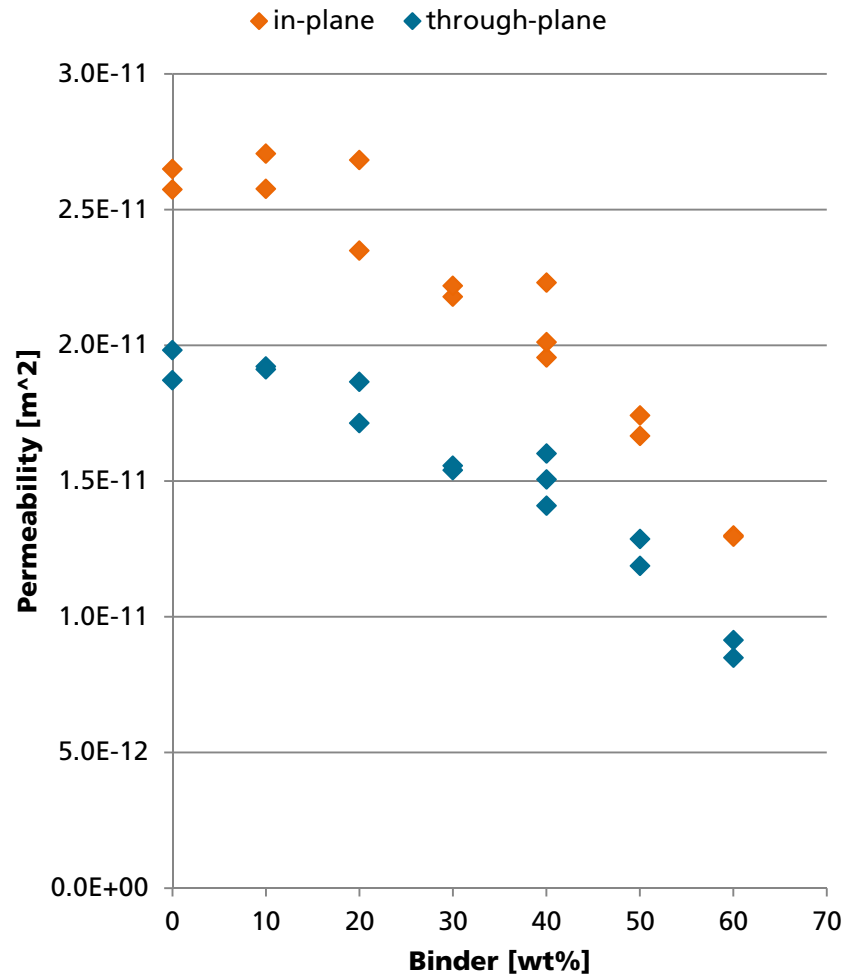


0 wt% Binder

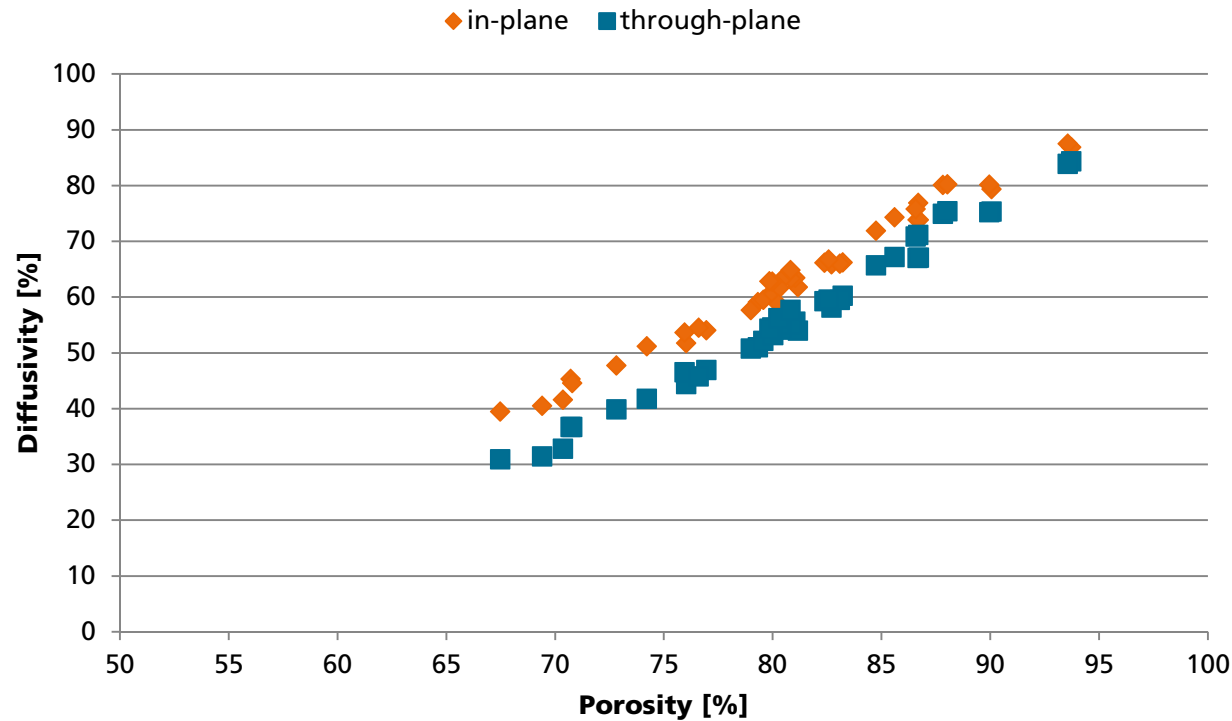


60 wt% Binder

Binder Content

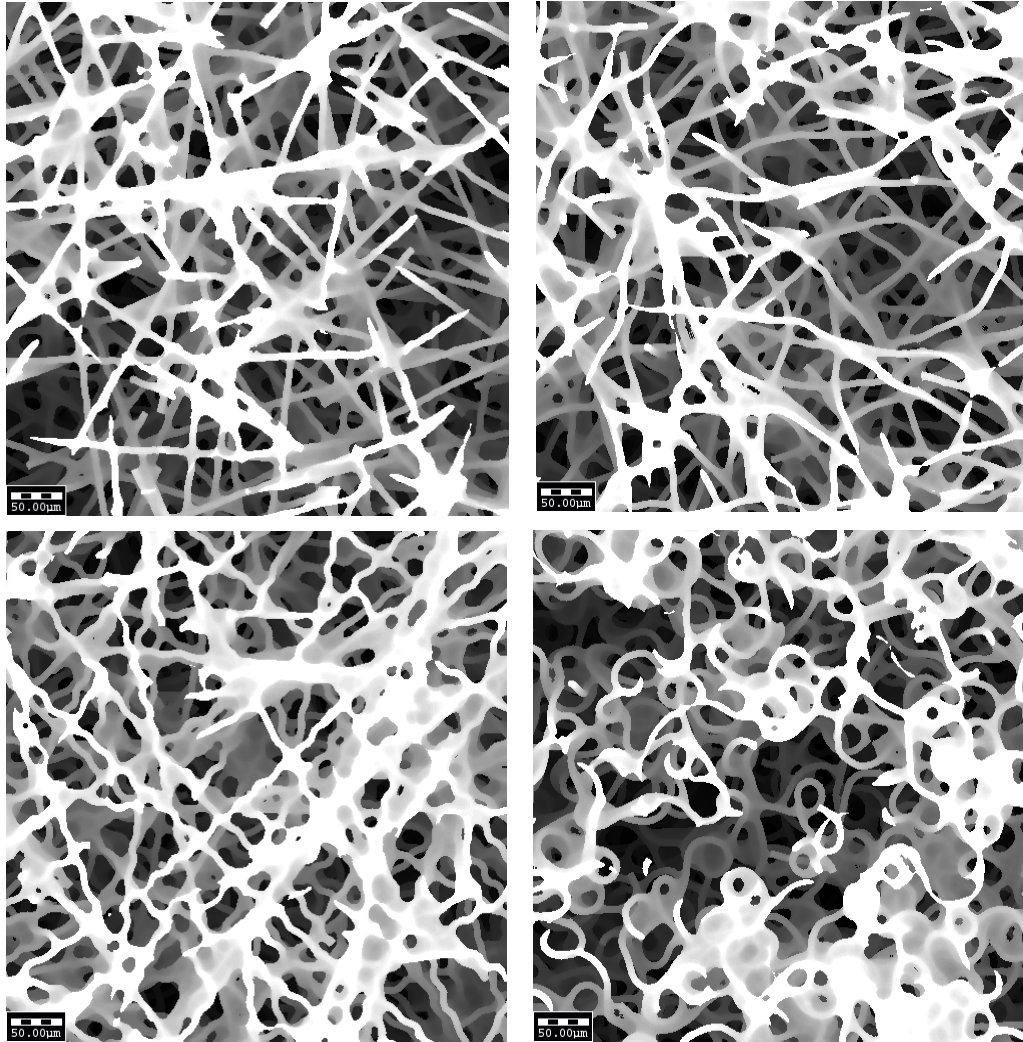


Diffusivity vs Porosity (all structure models)



Diffusivity only depends on porosity !
(all structures are similar enough)

Curl



- No direct influence on diffusivity and permeability
- Indirect influence by:
 - anisotropy
 - clustering

MPL Design Study

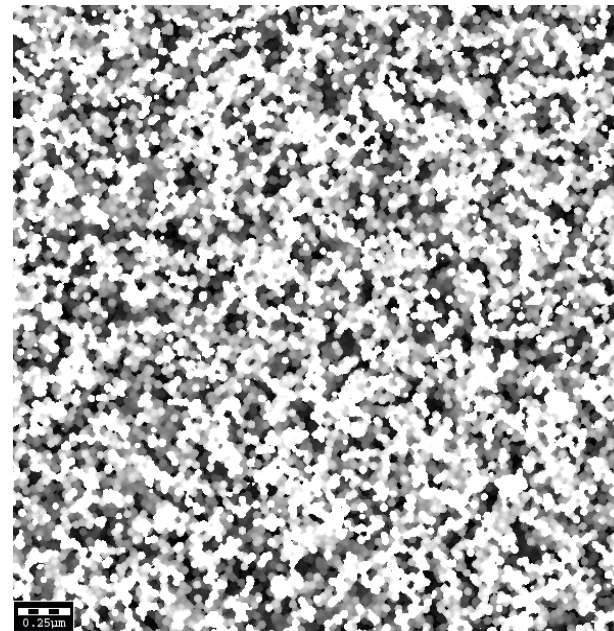
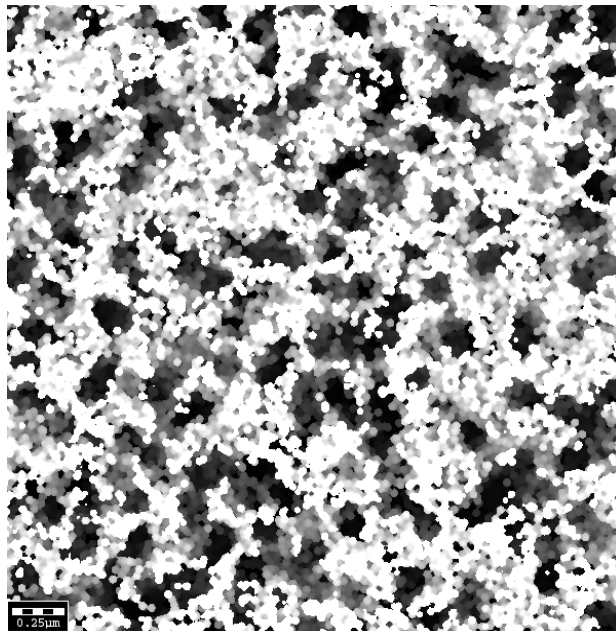
- Step 1: Create model of MPL structure, determine effective parameters for MPL alone
- Step 2: Create model for GDL+MPL, determine diffusivity and conductivity of combined layer
- Step 3: What changes when we change MPL design parameters?

Work done by N. Zamel

Comparison of Different MPL

Create MPLs with

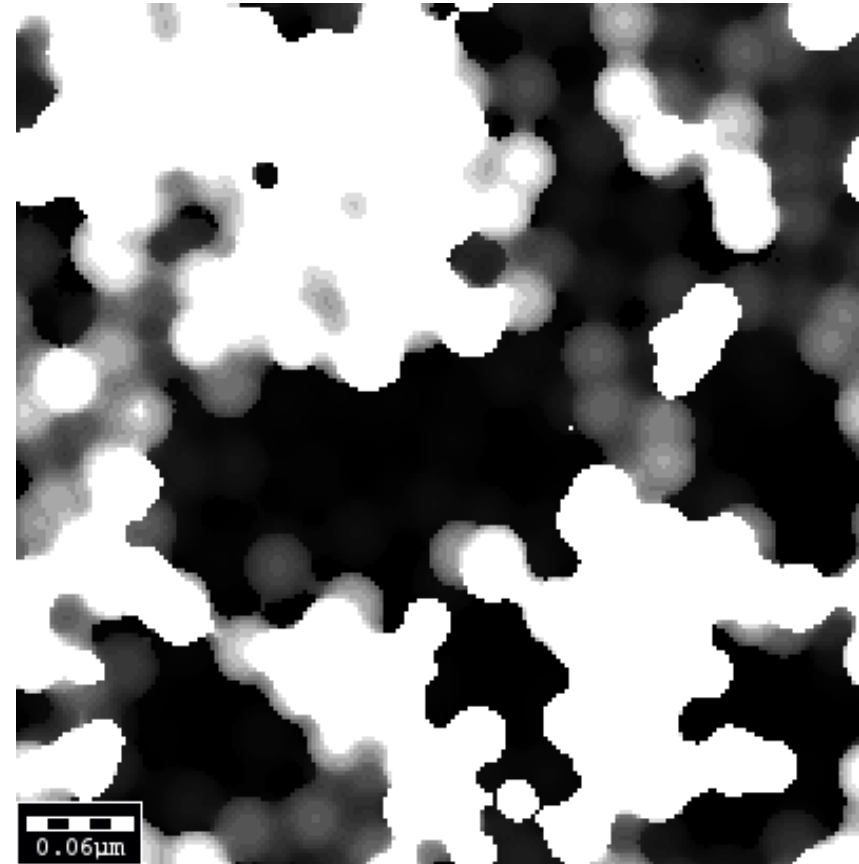
- same porosity & carbon particle sizes
- different pore size distributions



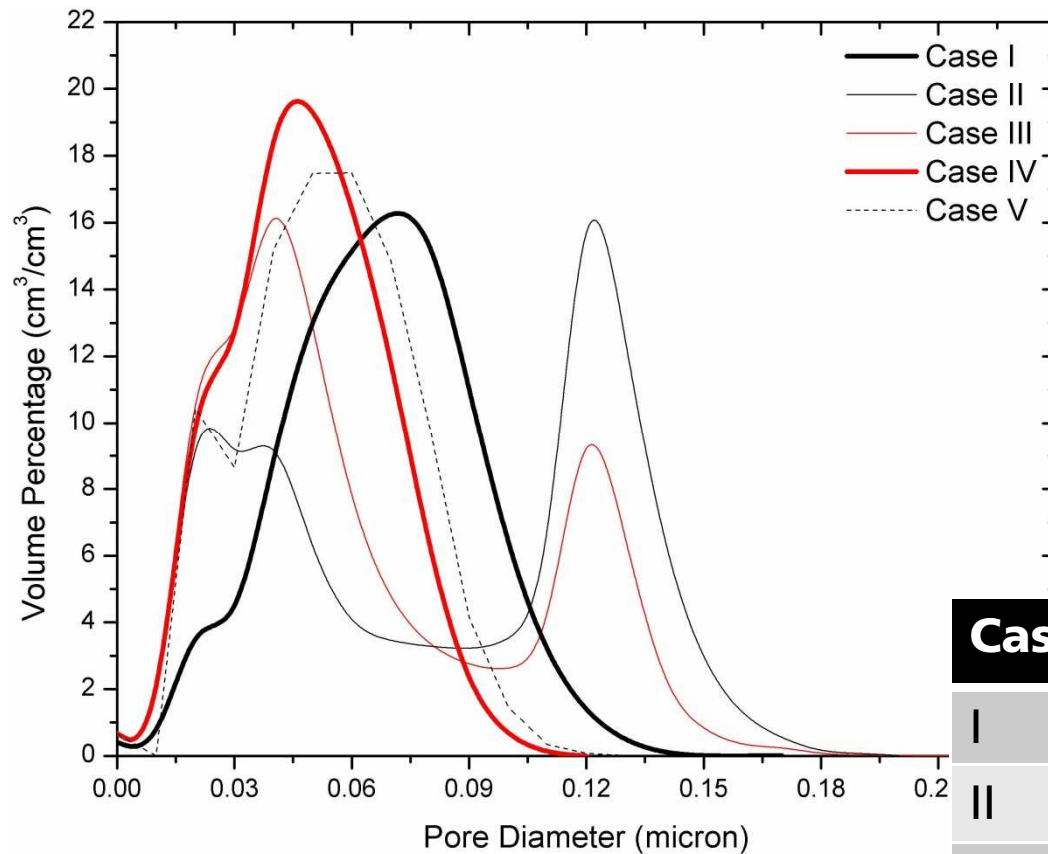
MPL Model

1. Create large pores
(distribute spheres randomly)
2. Create carbon particles
(distribute spheres in white area)
3. Glue
(fill small pores)

Parameters: radii, volume fractions



Comparison of Different MPL



Diffusivity:

Becker, Wieser, Fell, Steiner, Int. J. Heat and Mass Transfer 54, 2011.

Conductivity:

Wiegmann, Zemitis, Tech Report 94, ITWM, 2006.

Case	Conductivity	Diffusivity
I	0.094	1.92
II	0.120	1.78
III	0.104	1.65
IV	0.092	1.59
V	0.095	1.67

Knudsen Diffusivity

Macroscopic description (homogenized porous media model)

Fick's first law: $j = -D^* \nabla c$

D^* : effective diffusivity [m^2/s] **unknown**

j : diffusion flux [$\text{mol}/\text{m}^2/\text{s}$]

c : concentration [mol/m^3]

Diffusion mechanisms

1. $\text{Kn} \ll 1$ (bulk diffusion)

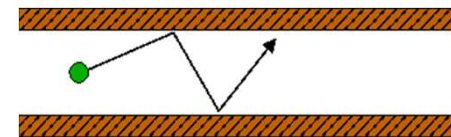
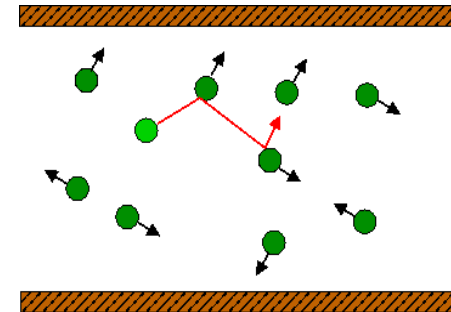
- Diffusion by particle-particle collisions
- Mathematical model: Laplace equation

2. $\text{Kn} \gg 1$ (Knudsen diffusion)

- Diffusion by particle-wall collisions
- Mathematical model: random walk methods

3. $\text{Kn} \sim 1$ (transition regime diffusion)

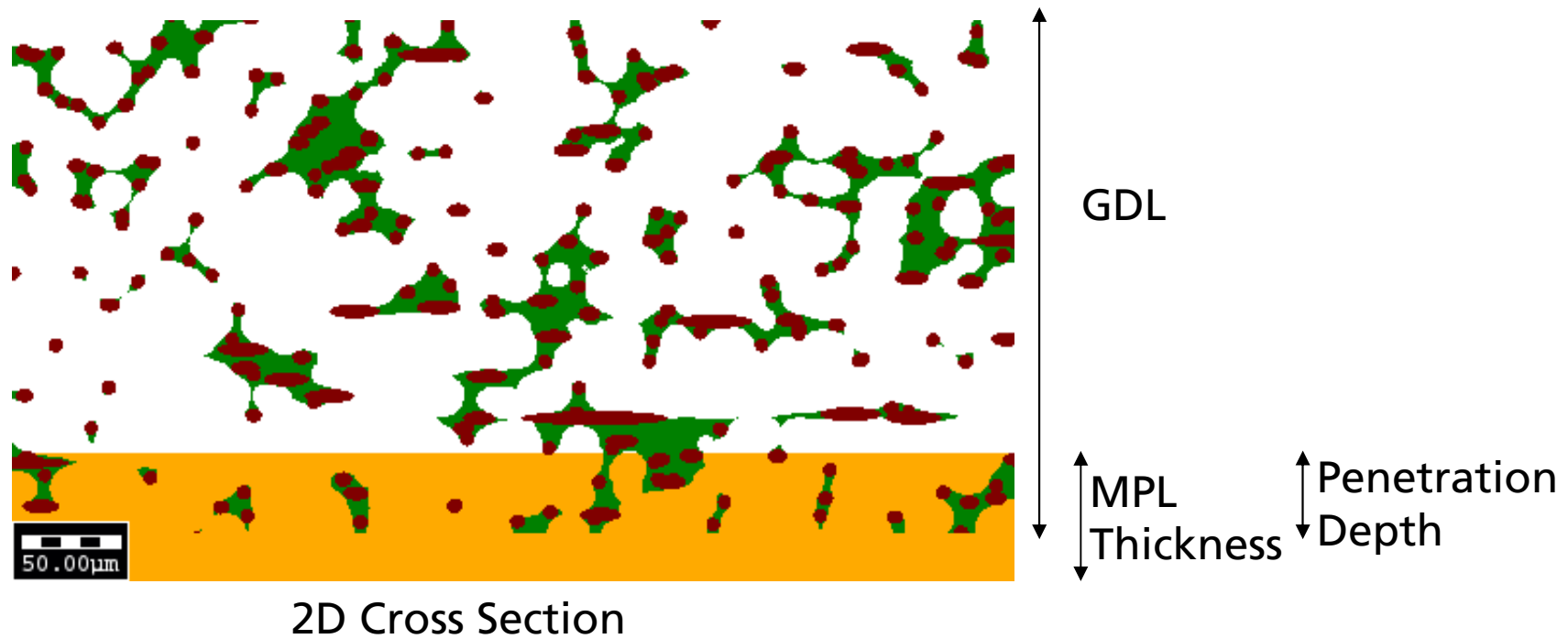
- Both mechanisms are present, Bosanquet:

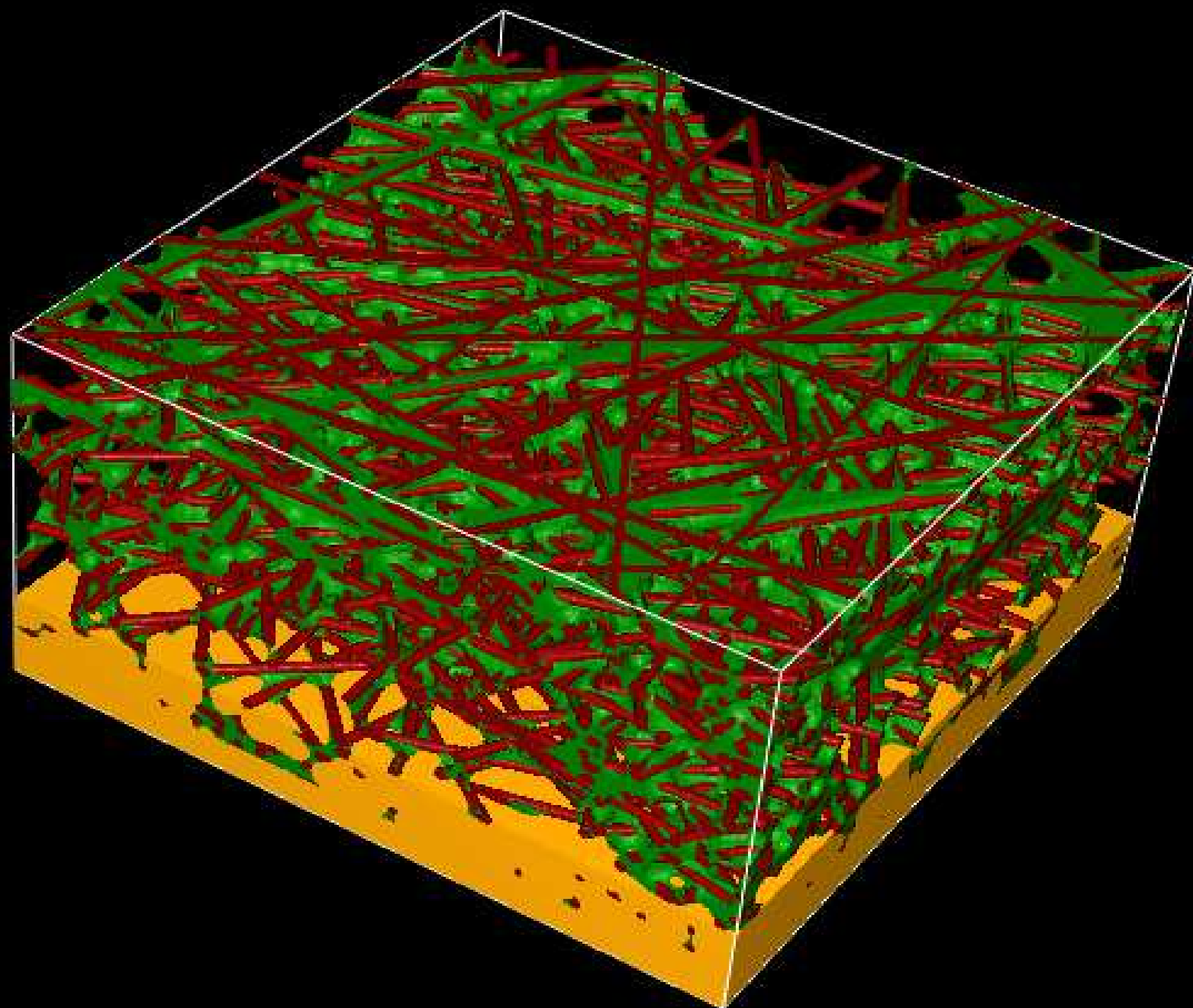


$$D_{Kn} = \frac{\varepsilon}{2t} E[(x_t - x_o)(x_t - x_o)^T]$$

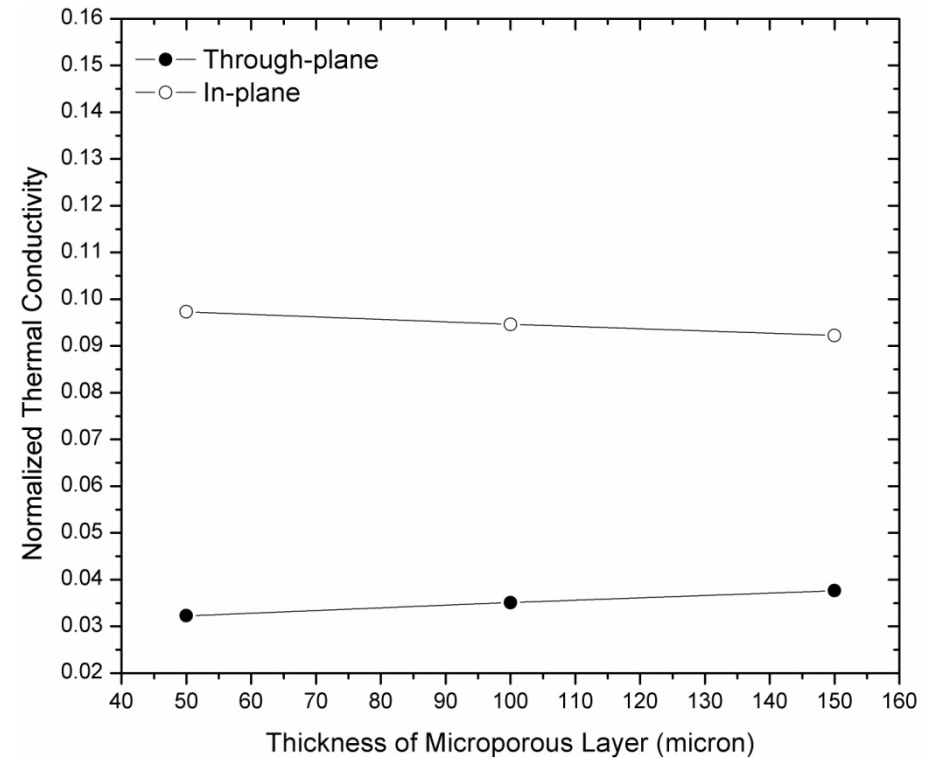
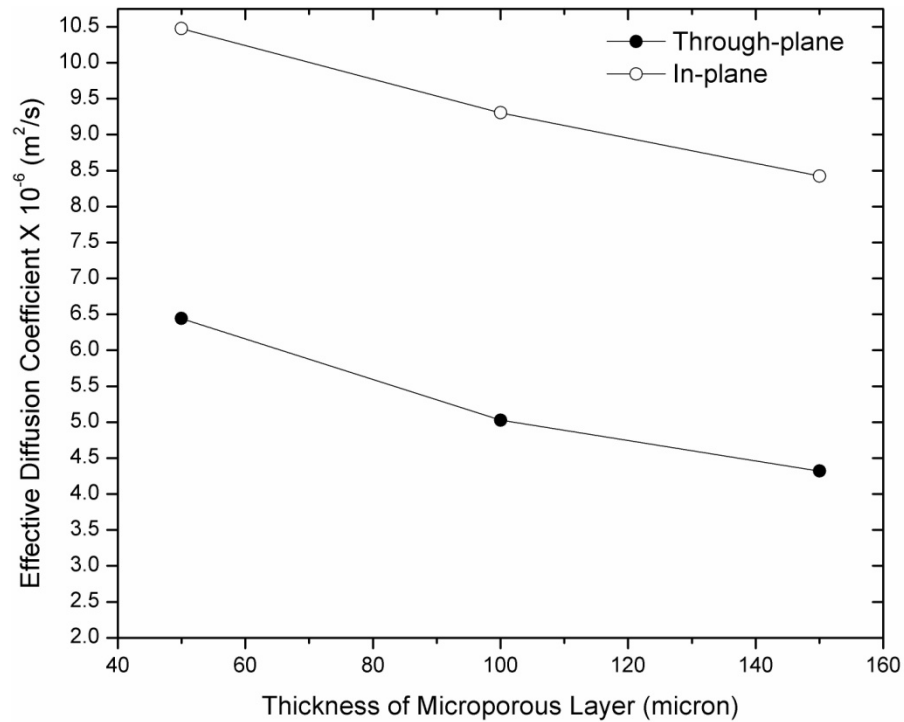
$$D = \left(D_{bulk}^{-1} + D_{Kn}^{-1} \right)^{-1}$$

GDL / MPL Assembly

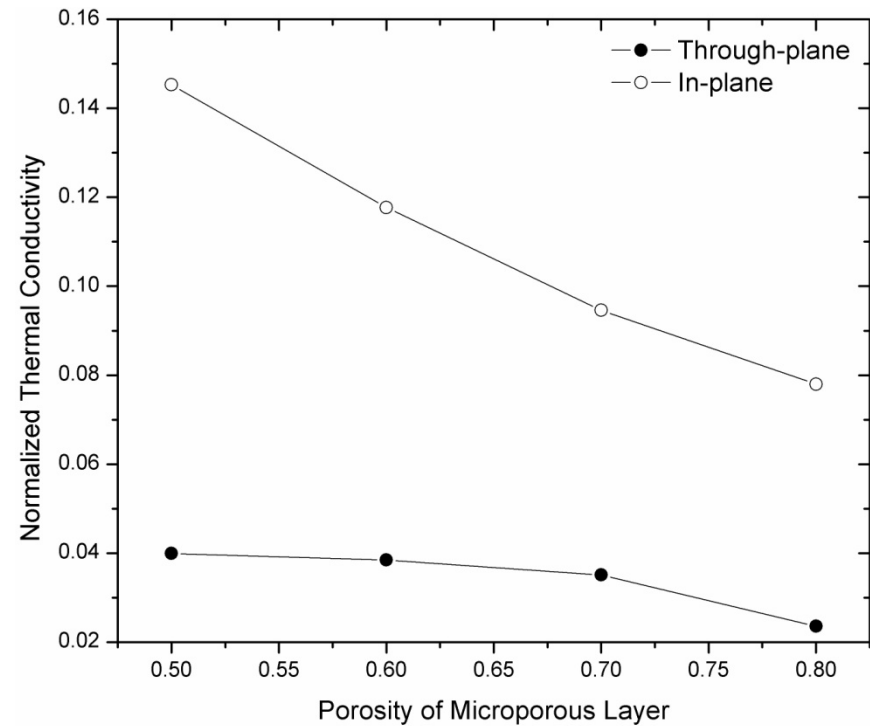
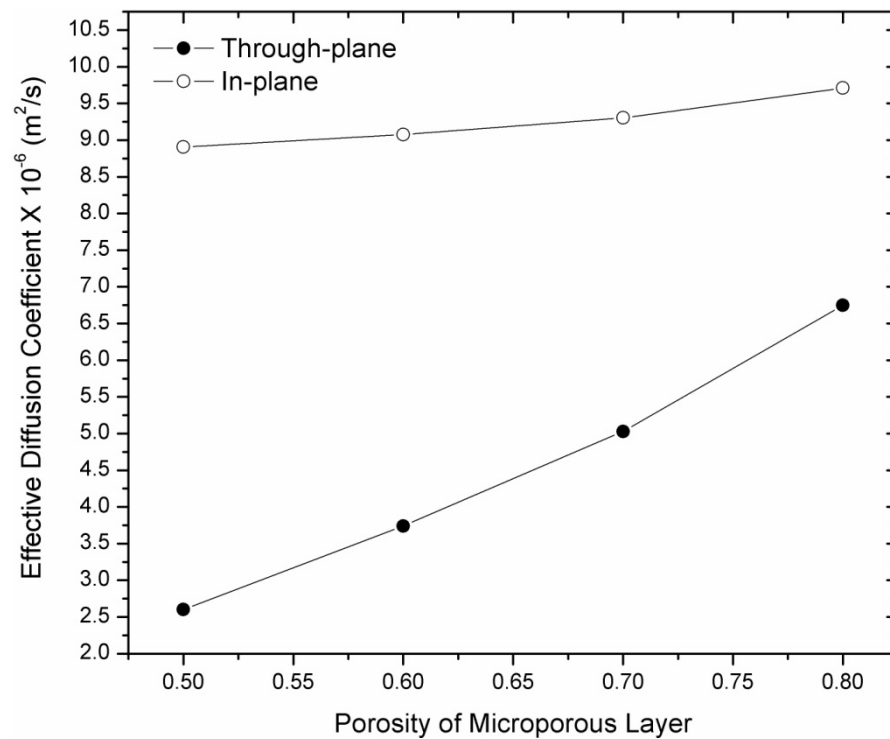




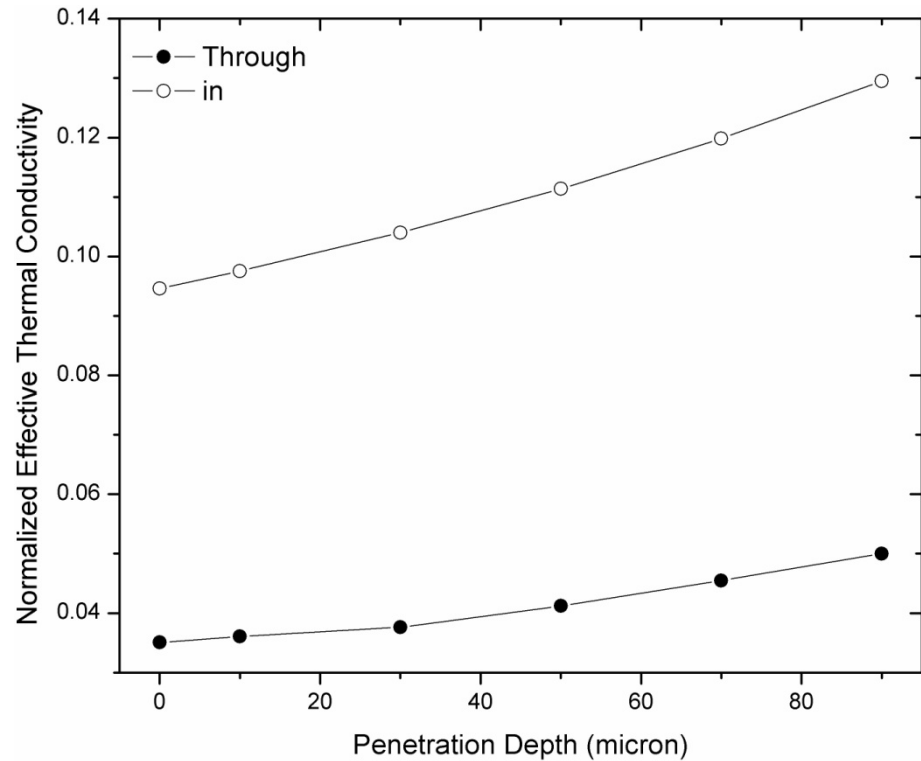
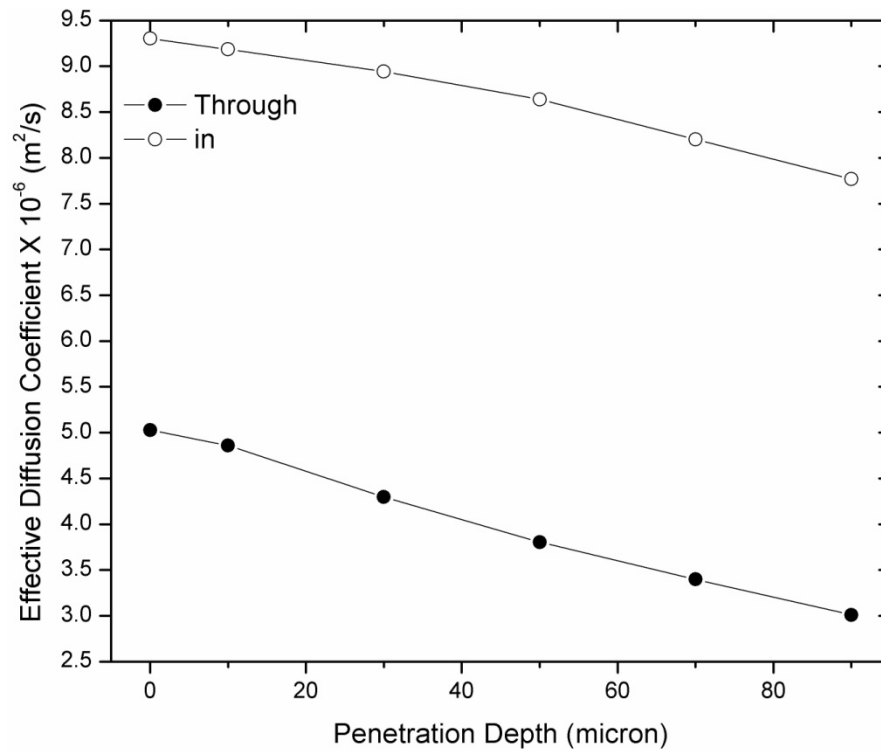
Variation of MPL Thickness



Variation of MPL Porosity



Variation of MPL Penetration Depth



Design Studies Summary

- GDL structure
 - fiber diameter, porosity, binder content, curl
- MPL micro structure
 - pore size distribution, porosity
- MPL macro structure
 - thickness, penetration depth

Thank You !



Geometry generator, property
predictor and virtual material
designer

www.geodict.com

BMBF project PemCaD

